

TEMPERATURE IMPACT OF NITROGEN TRANSFORMATION IN TECHNOLOGICAL SYSTEM: VERTICAL FLOW CONSTRUCTED WETLAND AND POLISHING POND

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Abstract

The article describes the results of the research, purpose of which was to evaluate influence of the temperature on the effectiveness of nitrification and denitrification in the sewage treatment system consisting of vertical flow constructed wetland and polishing pond. During the analysed period, the efficiency of removing total nitrogen was low and amounted to 12.7%. In the polishing pond in the summer period, content of total nitrogen in treated sewages was further decreased by nearly 50%. In the winter period, the polishing pond fulfilled mainly retention role and thus did not improve effectiveness of the whole system. Temperature coefficients, calculated on the basis of single first-order kinetics, for nitrification process in the filter bed ($N-NH_4^+$) and denitrification process in the polishing pond ($N-NO_3^-$) amounted to 1.039 and 1.089, respectively.

Keywords: constructed wetlands, temperature, nitrogen removal, first-order kinetics

1. INTRODUCTION

For many remote communities, due to economic and topographic constrains, constructed wetlands (CW) are a perfect alternative for centralized sewage systems based on septic tanks or sewerage, improving living standard. However, decentralizing of wastewater management aims not only for improvement of sanitation safety but also reduction of pollution discharge into the water bodies.

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In many areas, domestic wastewater is a primary source deteriorating quality of local water resources, with nitrogen discharge being one of the main environmental concerns. Constructed wetlands offer wide range of removal mechanisms and can be pollution targeted designed, thus are widely used to limit excessive nitrogen leaching into the environment [11, 17, 22]. Due to the design characteristic (smallest land area required) and easy operational maintenance, vertical flow constructed wetlands (VFCWs) are very popular among home owners. Unlike other types of subsurface flow constructed wetlands, VFCW are less vulnerable to clogging and engage more plant interaction [7]. Transformation of nitrogen compounds in VFCW is dependent on several factors such as temperature, redox conditions, substrate material and sewage composition [7]. Further increase in effectiveness can be obtained through applying advanced operation strategies that include baffled flow, microbial fuel cells, bioaugmentation, artificial aeration or supply of electron donors [21]. Construction characteristic that enhances air-substrate gas exchange makes VFCW well aerated systems predominantly with aerobic zones. Oxygen enters VFCW filter bed through suction effect made by downwards water flow as well as plant input. Hence, in terms of nitrogen removal, VFCWs are dominated by oxygen – based nitrogen transformation processes. Even though VFCW are most efficiently oxygen-supplied wetland systems, several attempts were made to artificially enhanced oxygen content within filter bed. Simple air pump systems [5], eventual evolved into highly efficient oxygen supply systems such as force bed aeration VFCW [1]. When supplying VFCW with wastewater rich in organic nitrogen, ammonification process is activated, occupying top, highly aerated layers of filter bed. As a result, availability of NH_4 drives nitrification process, predominantly carried out by autotrophic nitrifiers, however heterotrophic nitrifiers can also be involved [18]. High alkalinity of wastewater ($\text{pH} > 9.3$) can lead to conversion of NH_4^+ into NH_3 and thus removal of ammonia through volatilization, however this process is insignificant for VFCW [12]. Also dissimilatory nitrate reduction, has not been reported to play any major role in VFCW, unlike in HFCW [18]. Ammonium can also be effectively incorporated into biomass, with rates in some cases taking over nitrification process [16]. Cation exchange phenomenon can temporarily inactivated NH_4^+ transformation, when proper substrate media is used. Nevertheless, over the time absorbed ammonium is further utilize for nitrification process or biomass assimilation. Proper design and operational strategies, can promote anaerobic ammonium oxidation combined with vertical flow systems [3]. Ammonium transformation route may also include completely autotrophic nitrate removal over nitrate (Canon process) which can significantly improve VFCW effectiveness [15]. Even though, nitrogen-related process in VFCWs are mostly recognized for ammonium transformation routs, nitrate-based denitrification can occur as well, although advanced approach is

needed to facilitate the process otherwise it would have relatively low impact [8, 9]. Both nitrate and ammonium, are converted into organic forms to form organic cells and tissues through plant uptake and microbial assimilation. Gaseous form of nitrogen (N_2) can be converted to ammonia, however that transformation process is rather negligible in VFCWs [18].

The main objective of this paper is to show the seasonal variability of transformation of nitrogen in most popular, commercially available type of vertical flow constructed wetland in Poland. Additionally the temperature coefficient with the first-order kinetic model was determined.

2. METHODOLOGY

2.1. Research object

The research object was a constructed wetland in Lubusz Voivodeship, which was created on the basis of solution patented by Applicable Ecology Institute [The Patent Office of Republic of Poland, No. 198680]. The treatment system realised the project of building of sewage treatment systems in the borough, subsidized by the Rural Development Programme for 2007-2013. Sewage treatment system is a system consisting of interconnected elements: 2m³ polythene sedimentation tank, collector/pumping station with a submersed pump, and uplifted root filter connected by a drainage system with a polishing pond (Fig. 1). The root filter is a system of 3 filtering layers: 20cm top layer of grinded pine bark, 50cm middle layer of medium sand, 20cm bottom layer of washed river gravel of 20-50mm granulation. Common sedge (*Carex niagra*) grows on the surface of the filter. The structure of the filter is uplifted 90cm over the ground, which enables gravitational discharge of treated sewages to the polishing pond. The filter bed is isolated from the ground with a foil of 2mm width. The pond is isolated up to the height of 60cm above the bottom, enabling discharge of the treated sewages into the soil through the infiltration zone. The whole system takes up 49m², in which the filter takes up 31.5m² and the pond takes up 17.5m² (Phot. 1).

Based on water meters reading of a household, average daily surface overflow rate of the treatment system is 0.4m³/d or 12.7dm³/m²·d per 1m² of the filter bed. The filter bed is fed in the pressure system with pre-treated sewages from the sedimentation tank. Dosing of sewages is irregular and depends on the filling of the pumping station, in which the pump automatically insets itself after the tank (about 75dm³) has been filled. Thereby, the filter bed is fed from 5 to 6 times a day.

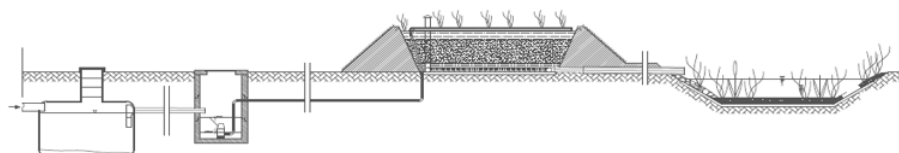


Fig. 1. Cross section of treatment system analyzed in the research
[by Ecoverde, No. 198680]



Phot. 1. View on the constructed wetland system [by Bydałek]

In the analysis of the research results, the water balance of the wetland including precipitation and evapotranspiration was not included, since:

- Average precipitation for the area in which the treatment system is located [6] amounts to about $575\text{mm}/\text{m}^2$ per year, which with the territory of treatment system taking 49m^2 gives about 29m^3 of precipitation per year;
- Evaporation from water surfaces very varied depending on the region of Poland and air temperature. The literature [2, 6] gives ranges from $500\text{mm}/\text{m}^2$ per year to even $1000\text{mm}/\text{m}^2$ per year, for Lubusz Voivodeship it is $500\text{mm}/\text{m}^2$ per year. Meanwhile, evaporation from surface covered in hydrophytes amounts to from $1000\text{mm}/\text{m}^2$ per year to even $2000\text{mm}/\text{m}^2$ per year [6]. Therefore, when considering minimal values of the evapotranspiration (500 and $1000\text{mm}/\text{m}^2$ per year), evapotranspiration of the analysed treatment plant amounts to about $33\text{m}^3/\text{year}$, thus being comparable to estimated precipitation.

2.2. Analysis of effectiveness of sewage treatment

Effectiveness of the treatment characteristic for the system was researched in a sewage quality monitoring system in three measuring points: raw sewages, sewages treated in the filter bed and sewages treated in the pond. The samples were collected in the period between August 2015 and January 2016. Before collecting samples, a pump was connected to the filter bed and to the pond, forcing

the feeding of fresh portion of sewages to the treatment system. Depending on the weather conditions, hydraulic retention time of the hydrophytic filter bed was between 10 and 15min. During sample collection, temperature of the sewages was measured at each measuring point, as well as air temperature and temperature at the depth of 30cm inside the filter bed.

During 6 months, 16 samples total were collected, in 3 series:

- 5 samples in the period between August and September - summer period;
- 8 samples in the period between October and December - autumn period;
- 3 samples in the period between January 7 and 21 - winter period.

Due to exceptionally mild winter of 2015/2016, only 3 samples were collected in the period characterised by long periods of minus ambient temperatures.

Total Kjeldahl Nitrogen (TKN), ammonium nitrogen, nitrate nitrogen were marked in the sewage samples in compliance with applicable regulations.

2.3. The first-order kinetic model of nitrogen removal applied to the VFCW

The areal removal rate constant and the temperature coefficient were calculated from the monitoring data and the following first-order model [10, 13]:

$$\ln(C_{out}/C_{in}) = -k_{(T)}/q \quad (2.1)$$

where:

- C_{in} and C_{out} are the influent and effluent concentrations, respectively, in mg/dm^3 ,
- q is the hydraulic loading rate (m/day),
- t is the temperature ($^{\circ}\text{C}$),
- $k_{(T)}$ is the constant of a first-order removal rate on temperature (m/day).

Equation (2) was used to calculate q (m/day):

$$q = Q/ A \quad (2.2)$$

where:

- Q is total wastewater inflow rate (m^3/day),
- A is the total area of the wetland (m^2).

The effect of temperature on the areal removal rate constant was modelled using the following equation:

$$k_{(T)} = k_{(20)} \cdot \Theta^{(T-20)} \quad (2.3)$$

$$\ln k_{(T)} = \ln \Theta(T-20) + \ln k_{(20)} \quad (2.4)$$

Statistically significant differences were determined at the $\alpha = 0.01$ significance level.

3. RESULTS AND DISCUSSION

3.1. Influent and effluent nitrogen concentrations

Content of total nitrogen in raw sewages was on average 122 mgN/dm^3 ($n=15$) and stayed in the range from 100 to 140 mgN/dm^3 . The lowest values were observed in the winter period. Average content of total nitrogen in treated sewages was between 90 and 130 mgN/dm^3 . Effectiveness of sewage treatment was irregular. The lowest values of concentration of total nitrogen in pond water were observed in the summer period ($55\text{-}75 \text{ mgN/dm}^3$) and they were gradually increasing in the autumn period, stabilising at the level of $80\text{-}90 \text{ mgN/dm}^3$ in the winter period. Ammonia nitrogen was the dominant (97%) form of total nitrogen in raw sewages, reaching average value of $118.8 \text{ mgN-NH}_4^+/\text{dm}^3$. Sewage treatment in the hydrophytic filter bed lowered that value by 88%. However, visible change of effectiveness of removing nitrogen was observed in comparison to the summer/autumn and winter periods. Content of N-NH_4^+ in the effluent in the summer/autumn period was $9.1 \text{ mgN-NH}_4^+/\text{dm}^3$ ($n=12$) on average, while in the winter period over triple increase up to $30.9 \text{ mgN-NH}_4^+/\text{dm}^3$ ($n=3$) was observed, which mirrors the decrease of effectiveness of mechanisms of removing ammonia nitrogen from the initial 92% ($n=12$) to 70% ($n=3$). Similar dependence was observed in the polishing pond, where content of ammonia nitrogen was highly correlated ($R^2=77.2\%$, $p<0.05$) with quality of fed sewages. Content of ammonia nitrogen in the pond was, on average, 20% lower than in treated sewages. Organic nitrogen in samples constituted from 1 to 5% of total nitrogen, which is indicator characteristic for this type of system. The lowest values were observed in treated sewages, which proves the effectiveness of ammonification process. Simultaneously, in the polishing pond could be observed increased level of nitrogen as compared to quality of sewages fed to it. Content of nitrogen in forms of nitrates in raw sewages was between 0.5 and $1.0 \text{ mgN-NO}_3^-/\text{dm}^3$. Effective nitrification process happening in the hydrophytic filter bed caused the increase of content of nitrate nitrogen in the effluent to the level from 80 to $100 \text{ mgN-NO}_3^-/\text{dm}^3$ in the summer period ($n=12$). In the winter period decrease of 25% in the content of N-NO_3^- was observed, which coincides with the observations regarding effectiveness of removing ammonia nitrogen. Nitrate nitrogen constituted the dominant part of nitrogen in the polishing pond, wherein its' content fluctuated significantly in the range from 40 to $80 \text{ mg N-NO}_3^-/\text{dm}^3$, reaching minima in the summer and winter periods, while increased values were observed in the autumn period.

3.2. Effectiveness of the nitrification and denitrification process

Effectiveness of the nitrification process in the hydrophytic filter bed during the period of the research presents Fig. 2. Between August and December, the effectiveness of oxidization of ammonia nitrogen was high: from 88 to 96%. During that period, the temperature was gradually dropping due to change of seasons from 22 to 8°C. In January, when the temperature in the filter bed dropped below 3°C, the efficiency of nitrification process gradually decreased to 65%.

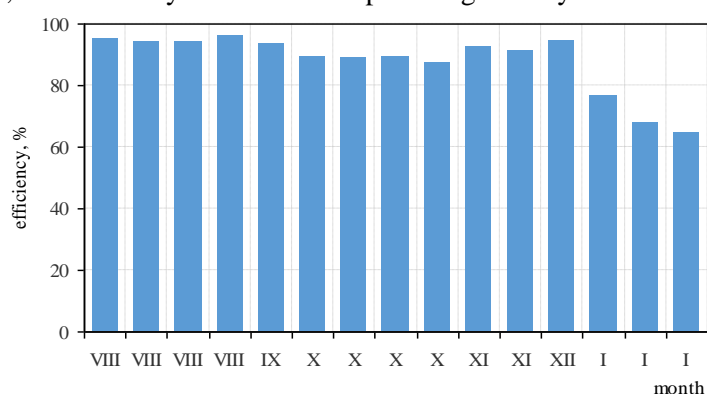


Fig. 2. Effectiveness of nitrification process

Effectiveness of denitrification process in the polishing pond during the period of the research presents Fig. 3. Between August and September, the effectiveness of reduction of nitrate nitrogen was from 40 to 65%. From Oktober to beginning of January from 10 to 20%. In January, it was found in the effluent from the pond higher concentration than in the treated wastewater.

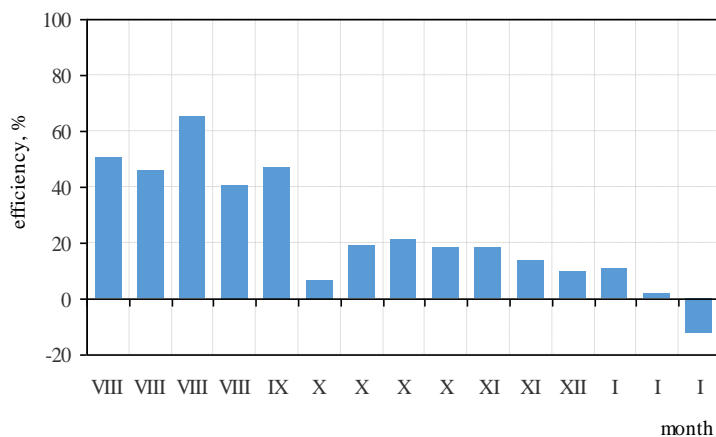


Fig. 3. Effectiveness of denitrification process



The mechanism of transformation of nitrogen compounds in the hydrophytic filter bed and polishing pond system is proved also by the changes of pH.

High significant correlation (Fig. 4) between pH of treated sewages and the effectiveness of removing ammonia ions ($R^2=0.97$, $p<0.001$) was observed. Nitrification of 1 mg of ammonia nitrogen uses up 7.14 mg of basicity expressed with calcium carbonate (CaCO_3), whereas stoichiometrically, during the nitrification process of 1 mole of ammonia nitrogen, 1.98 mole of hydrogen ion H^+ is released, which leads to decrease of the pH [7]. The observed correlation proves, then, that nitrification process is the dominant mechanism of transformation of nitrogen compounds in the researched system, leading to acidification of the filter bed environment as a result. Observed decrease in effectiveness of nitrification in the winter period resulted in increase in pH of treated sewages amounting to nearly one degree.

Similar dependency, although not as much correlated ($R^2=0.785$, $p<0.001$), was observed in the case of the polishing pond, where effectiveness of removing nitrogen compounds directly influenced pH of water (Fig. 5). This phenomenon shows influence of denitrification as a mechanism of removing nitrate nitrogen in the pond. Stoichiometric equation of denitrification shows that 1mg of oxidized nitrate nitrogen creates about 3mg of calcium carbonate, which results directly in the increase of pH [7]. Clearly, the decreased effectiveness of nitrification process in the winter period caused the decrease of water pH in the pond to the level close to the pH of treated sewages.

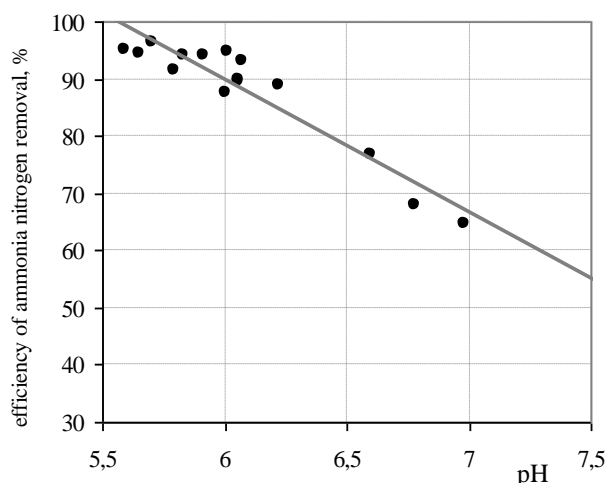


Fig.4 The impact of ammonium removal on pH of effluent

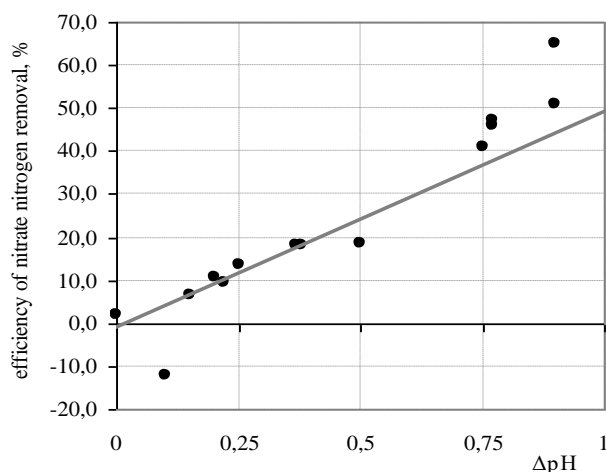


Fig. 5. pH neutralization effect based on removal effectiveness of nitrate in polishing pond

3.3. Estimation of the temperature coefficients

Using Equation (2.1) and the measured values of C_{in} and C_{out} , were calculated constants ($k_{(T)}$) for $N-NH_4^+$ and $N-NO_3^-$ (Table 1). The corrected values of $k_{(T)}$ for a temperature of 20°C and temperature coefficient were obtained from Equation (2.3).

Table 1. Calculated constants ($k_{(T)}$ and $k_{(20)}$) and temperature coefficient (Θ) for nitrification and denitrification process

constants	$k_{(T)}$ [m/day]	$k_{(20)}$ [m/day]	Θ [-]
Nitrification (VFCW)	0.030	0.038	1.039
Denitrification (polishing pond)	0.007	0.012	1.089

Corrected to 20°C, the $k_{(20)}$ values of both $N-NH_4^+$ and $N-NO_3^-$ were slightly greater, indicating the influence of temperature on nitrogen removal. The $k_{(20)}$ of $N-NH_4^+$ and $N-NO_3^-$ were lower respectively, than those reported by the values obtained by Dzakpasu et al. [4]. The temperature coefficient Θ values estimated for $N-NH_4^+$ and $N-NO_3^-$ were 1.039 ($R^2=0.72$) and 1.089 ($R^2=0.92$) for VFCW and for polishing pond, respectively, and were higher than those reported by Dzakpasu et al. [4].

4. CONCLUSIONS

Among a few mechanisms of removing nitrogen in VFCW sewage treatment systems, nitrification is the dominant process [19]. Meanwhile in vertical flow



systems, nitrification process is often replaced by highly effective mineralisation of organic matter, which uses up majority of the available oxygen [14]. Practically, an effective nitrification happens only at depth below 40 cm [23], since in the higher part of the profile dominate processes of organic compounds oxidizing. VFCW systems are characterised by high level of aeration, however, in case of filling them with sewages containing high amount of organic matter or in case of clogging the filter, a considerable reduction of supplied oxygen happens. Literary data shows that effectiveness of nitrification in typical hydrophytic sewage treatment systems decreases rapidly in conditions below 10°C [7]. However, there are hydrophytic systems specifically adjusted to low temperatures that maintain high (over 70%) effectiveness of removing nitrogen [24], which proves the possibility of maintaining biological mechanisms of removing nitrogen compounds in low temperatures. Thus, it can't be unequivocally determined that decrease in air temperature largely influenced the decrease in effectiveness of removing ammonia ions.

Based on the results, it was found that:

1. The mechanism of transformation of nitrogen compounds in the hydrophytic filter bed and polishing pond system was proved by the changes of pH.
2. Temperature has an impact on the effectiveness of the processes of nitrification and denitrification in hydrophytic systems.
3. Greater influence of temperature on the transformation of nitrogen compounds was observed in the polishing pond than in the hydrophytic filter bed.
4. The temperature coefficient Θ values estimated for N-NH_4^+ and N-NO_3^- were 1.039 and 1.089 for VFCW, and for polishing pond, respectively.

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WPŁYW TEMPERATURY NA PRZEMIANY AZOTU W UKŁADZIE
TECHNOLOGICZNYM: ZŁOŻE HYDROFITOWE O PRZEPLYWIE PIONOWYM
I STAW DOCZYSZCZAJĄCY

Streszczenie

W artykule opisano wyniki badań, których celem była ocena wpływu temperatury na efektywność procesów nityfikacji i denityfikacji w przydomowej oczyszczalni ścieków pracującej w układzie: złożo hydrofitowe o przepływie pionowym i staw doczyszczający. W analizowanym okresie sprawność usuwania azotu ogólnego była niska i osiągała wartość 12,7%. W stawie doczyszczającym w okresie letnim zawartość azotu ogólnego w ściekach oczyszczonych uległa dalszemu obniżeniu o blisko 50%. W okresie zimowym, staw pełnił głównie rolę retencyjną, nie przyczyniając się do zwiększenia efektywności pracy całego układu. Wyznaczony współczynnik temperaturowy (Θ) na podstawie założeń kinetyki pierwszego rzędu dla procesu nityfikacji w złożu ($N-NH_4^+$) oraz denityfikacji w stawie doczyszczającym ($N-NO_3^-$) wynosił odpowiednio 1.039 i 1.089

Słowa kluczowe: oczyszczalnie hydrofitowe, temperatura, usuwanie azotu, kinetyka pierwszego rzędu

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