

Article

Electromagnetic Control and Dynamics of Generalized Burgers' Nanoliquid Flow Containing Motile Microorganisms with Cattaneo–Christov Relations: Galerkin Finite Element Mechanism

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Abstract: In our research work, we have developed a model describing the characteristics of the bio-convection and moving microorganisms in the flows of a magnetized generalized Burgers' nanoliquid with Fourier's and Fick's laws in a stretchable sheet. Considerations have been made to Cattaneo–Christov mass and heat diffusion theory. According to the Cattaneo–Christov relation, the Buongiorno phenomenon for the motion of a nanoliquid in the generalized Burgers' fluid has also been applied. Similarity transformations have been used to convert the control system of the regulating partial differential equations (PDEs) into ordinary differential equations (ODEs). The COMSOL software has been applied to obtain mathematical results of non-linear equations via the Galerkin finite element method (G-FEM). Logical and graphical measurements for temperature, velocity, and microorganisms analysis have also been examined. Moreover, nanoparticle concentrations have been achieved by examining different approximations of obvious physical parameters. Computations of this model show that there is a direct relationship among the temperature field and thermal Biot number and parameter of the generalized Burgers' fluid. The temperature field is increased to grow the approximations of the thermal Biot number and parameter of generalized Burgers' fluid. It is reasonable to deduce that raising the chemical reaction parameter and concentricity relaxation parameter or decreasing the Prandtl number, concentricity Biot quantity, and active energy parameter can significantly increase the nanoparticles concentration dispersion.

Keywords: generalized Burgers' nanofluid; Cattaneo–Christov heat flux theory; motile microorganisms; Galerkin finite element method

1. Introduction

Heat transference is a heat planning subject that contains the collecting, use, extrade, and exchange of depth power amongst useful structures. Heat transference is separated into diverse phases, as heat-conducting, heat convective, heat radiative, and power circulate via degree changes. Strategies additionally consider transferring a huge quantity of

engineered combinations (extrade in climate styles mass trade), both bloodless and heat, to acquire warmth circulation. However, these strategies have specific characteristics, and they normally appear in a comparative structure. Heat trade takes place whilst the motion of an incredible amount of liquid (fueloline or liquid) carries its heat in a liquid. All convective cycles additionally communicate fractional heat to the dissemination [1]. Heat transfer is perhaps the main modern cycle. Heat must be added, subtracted, or removed from the adaptation of one interaction to another throughout the modern field. Because of the lack of regular heat, the heat diffused by a heat flow is never equal to the warmth acquired by a cool fluid [2]. The goal of heat transfer is that the majority of modern conception uses a specific interaction to move heat. Drying processes are examples of large-scale heat transference. The contemporary applications of heat transfer liquids range from simple, dry plans to cutting-edge guesstimated structures that play multiple roles in the manufacturing cycle. Because there are different varieties within the connection and use of phases within the usage of depth pass liquids, the number of expeditions that use this strategy is similarly huge [3]. Downsizing vastly affects the improvement of depth exchangers and modifications of heat exchangers, resulting in greater disadvantages and greater benefits. The functionality of the depth exchanger basically affects the general viability and adequacy of the atomic strength structure. Smaller than normal channel heat sinks are one important device in heat change improvement. The capacity benefits of an enormous depth pass district and the excessive cohesiveness of a bit channel heat sink make it a very beneficial heat exchanger for microelectronic cooling [4].

Nanofluids are fluids that contain nano-sized molecules, identified as nanomolecules. These liquid particulate suspensions contain nanostructures in critical liquid. Most of the NPs used in nanofluids are made of metals, oxides, carbides, or carbon nanotubes. Various standard liquids have been used as operating liquids to transfer heat to various cycles. Water is commonly used as a working fluid due to its high availability, but it is not regarded as an effective heat transporter due to its lack of thermal conducting. Semi fluids, for example, fuel oil and propylene glycol, are also used in a variety of applications, but their platforms are designed, and a poisonous climate limits their use in heat transference processes [5]. The development of nanoparticles enhances the engine cooling rate when ethylene glycol and H₂O are used as vehicle coolants. Electronic cooling of integrated circuits and chip circuits has expanded recently, with outstanding implementation PCs utilizing a maximum force of 100–300 w/cm² [6]. The heat transference of Newton nanoliquid convection on the outer surface of the laminar limit is studied precisely. It has been noted that the convective heat transfer of standard convective is not only characterized by the dynamic nanoliquid of thermal conductance, and that abhorrence to the thickener model used appears obvious and plays an important role in heat transference conduct [7]. Since the turn of the century, the supposition of a layer beyond what many would conceive has proven extremely important and has provided a staggering capacity for the assessment of fluid hardware. Minor hypothesis occupations include an assessment of trying to pull bodies on the flow, such as a pull level surface in a zero point, an all-over, airfoil, aircraft body, or a generator edge [8]. The heat transference and flowing of pseudoplastic non-Newtonian nanoliquid over the entering surface were resolved in the continuing overall view where there was imbuelement and intake. Non-Newtonian nanoliquids demonstrate better heat transfer execution compared to Newtonian nanoliquids by imbuelement and non-combination plate. Furthermore, changing the type of nanomolecules has a general effect on the heat transference process throughout assistance [9]. Many additional studies, such as [10–14], have looked at the heat transmission problem with various types of surface and physical impacts.

The Buongiorno scheme is employed to inspect the impressions of Brownian diffusion enhancement and thermophoretic movement on electricity, heat, and mass transactions from plates having a long temperature history. The development of the problem is done using two-speed slide features, the Buongiorno model, which combines brown scattering and thermophoretic diffusion. We have measured the reliable movement of the

Buongiorno prototype via an extendable open tube. The mathematical prototype works by conjecturing the twisted tubes. Directly following applying the cutoff layer appraisals to Navier–Stokes calculations, we have arranged partial blunders. These calculations were changed over into a course of action of different standard non-layered assessments with a comparable quantifiable change [15]. The Buongiorno prototype is applied to analyze the influences of Brownian headway and thermophoretic diffusion on flowing, heat, and mass transfer from a stage surface with actual temperature progress. Assessment connects for dynamical thickness, heat conductance, and dependability of nanofluid are associated with the management assessments. Detaching proper attributes are modified into many general estimations using the equal change. These value determinations are decided computationally using the Runge–Kutta–Fehlberg methodology, which passes a careful five-returned directly to the returned design. The influences of perfect rapidity, temperature, and shearing weight at the dividing wall and Nusselt and Sherwood quantities, which are added to, managed, and veered from H₂O, primarily depend on nanofluids including ethylene-glycol [16]. For the heat circulation factor, due to the scale of the nanomolecules, the scattering sway is completely insignificant. Along those lines, Buongiorno suggested a greater version of painting the convective depth circulation manner that is extraordinary for nanoliquids and washes out the deficiencies of homogeneity and dispersing prototypes. Moreover, Buongiorno deduced that political agitation is not always affected by nanoparticles. With those disclosures as an explanation, he offered a two-component non-homogenous computational version of a varying automobile in nanofluids. Changed versions were applied by the study [17] to zero in on the impact of nanomolecules past what many could consider a feasible run-of-the-mill floor throughout an immediate platter, by study [18] to discover the nanoliquid Bernard convective, and by the study [19] for the appraisal of forced laminar convective. Then, an expansive evaluation of the convective automobile of nanoliquid change was facilitated by the studies [20,21], Khan and Pop [22], Malvandi et al. [23–25], Aziz and Khan [26], Sheikholeslami et al. [27–30] Gupta et al. [31], Haddad et al. [32], Sheikhzadeh et al. [33], and James et al. [34]. Beyond question, the most modern reviews have been presented in Refs. [35,36].

Evaluation of non-Newtonian liquids has been a continuing area of exploration for the past few years. Numerous contemporary fluids, which include unique oils, shampoos, paints, restorative items, polymers, colliding liquids, suspension liquids, and frozen yogurt, are described as non-Newtonian liquids. The assorted rheological categories of the effects of the non-Newtonian liquid are the price type (including the Maxwell version, Jeffery version, Oldroyd version, the Burgers version, and so on), the differential kind (including the following grade version, third-grade version, and so on), and the critical sort (including the Sisko version and so on). The Burgers' liquid version has been proposed to foresee the residences of unwinding and problem influences on the equal time. Because of the intricacies in numerically showing the Burgers' liquid version, little or no information has been reported for the Burgers' version. The work [37] registered several solutions for turning streams of a summed-up Burgers' liquid in spherical and hole regions. The researchers took into consideration the liquid circulation among co-pivotal chambers and applied the Laplace and Hankel modifications for the preparation's strategy. Awareness of the longitudinal motions of a summed-up Burgers' liquid in barrel-fashioned regions was brought with the aid of Ref. [38]. The researchers brought the influences of longitudinal motions and laid out the Fourier–Bessel collection. The particular association of beginning circulation for a reactive summed-up Burgers' liquid in a permeable half of the area was brought with the aid of study [39]. They employed and adapted Darcy's formula for computational representation in a permeability material and the Fourier sine and fragmentary Laplace alternate to systematize the specialist provision of the velocity conveyance. Khan et al. [40] discovered novel solutions for various swinging movements of a portion of Burgers' liquid. The authors merged the partial math approach into the constitutive courting model. They brought articulations for the velocity region and the succeeding shear stress. As a special state, equivalent answers for summed up

Oldroyd-B, Maxwell, and 2nd-grade liquids may be recorded. Liu et al. [41] examined the hydromagnetic circulation and depth circulation of a summed-up Burgers' liquid caused by a rapidly rushing-up surface with radioactivity impacts. The authors brought the circulation over a dramatically rushing-up divider. Definite explanations for the rapidity and temperature area are brought in a vital and collection shape as some distance because of the GG capacities. The study [42] brought the peristaltic circulation of a Burgers' liquid with criticism dividers and depth circulation. The authors employed a hypothetical test to discover the peristaltic circulation and depth circulation traits of a Burgers' liquid in a channel administered with the use of sinusoid rays. Different plots were used to approximately discuss the concept of rheology. The study [43] researched the depth circulation in the development of a Burgers' liquid at some stage in the liquefying system. The layered circulation situations were verified and, after some time, streamlined by making use of restriction layer investigation. The solution for the rising nonlinear difficulty was registered and expertise of various springing up barriers was given through diagrams.

This study centered on some elements that could affect the extent of motile microorganisms in an instance from the tongue determined utilizing a degree comparison magnifying instrument. It was found that the possibility of passing between inspection and research is basically significant. In each easy saline and dwindled delivery liquid (RTF), a lower extent of motile microorganisms could be observed inside 15–30 min in the wake of each individual attempt. To have the choice to postpone the time between examination and research, it was observed that placing an instance in a tuberculin needle with RTF more suitable with Fildes separately blanketed the motility of the microorganisms and gave no important reduction within the stage of the motile interior 48 h. As a result, the interaction of bioconvection with nanoliquid will be crucial in the future for microfluidic devices. Bees [44] mentioned "bioconvection", which depicts the effective power of fluids and blood hemoglobin living designs. The investigation [45] studied the convection restriction layer circulation of an Oldroyd-B nanoliquid created via an extended enclosure. Tlili et al. [46] looked at second-request slippage. The conjecture is a true notion for bioconvective nanofluids. The study [47] probed a dynamical nanoliquid on a circling surface with sliding microbes. The study [48] tried bioconvection of second-generation altered nanoliquids holding motile bacteria. The study [49] investigated the bioconvective flowing of nanoliquids using Wu's slippage rheology. The study [50] investigated the suitability of an expanded nanoliquid attractive substance with motile microbes introduced by the Prandtl bioconvective level. Waqas et al. [51] inspected the depth flowing of a non-permanent Williamson MHD nanofluid in comparison to non-equivalent motile gyrostatic microbes. Khan et al. [52] demonstrated the use of nanoliquid bioconvective flowing across an oscillating extended surface. More investigations of the bioconvection phenomenon have been completed [53].

G-FEM is a planned procedure for converting the capacities in a boundless layered painting area to first capacities in a restricted layered painting area while at ultimate regular vectors (in a vector area) which are conceivable with mathematical strategies. The FEM is a typical mathematical method for settling incomplete differential situations in some area factors (i.e., a few restricted esteem problems). To deal with a problem, the FEM walls a sizeable framework into much fewer tough components which are known as restricted additives. This is executed with the aid of a selected area discretization within the area components, which is executed using the improvement of a passing phase of the item; the mathematical place on behalf of an association has a restricted but wide variety of focuses. G-FEM defines a restricted esteem issue at ultimate effects in an association of mathematical situations. The method approximates the difficult-to-understand capability over the place [54]. The genuine scenarios that model those constrained additions are again gathered into a wider collection of situations that design the full issue. G-FEM then emulates a solution by constraining an associated blunder work using the analytics of variations. While a precise date for the invention of G-FEM is tough to pinpoint, the strategy arose from the wish to resolve complicated adaptability and major examination

challenges in odd locations and aerospace creation. Its evolution may be traced back to the works of Hrennikoff [55] and Courant [56] in the mid-1940s. Ioannis Argyris was another pathfinder. A presentation of the affordable usage of a process is normally related to the work of Leonard Oganessian [57]. Moreover, it was freely rediscovered in China with the aid Feng Kang in the late 1950s and mid-1960s, given the calculations of dam developments, in which it became referred to as the restricted evaluation method in a mild range standard. Although the methodologies used by these trailblazers are unique, they share one essential trademark: community discretizing of a consistent place keen on a group of separate sub-spaces, normally known as additives. FEM received its initial impetus in the 1960s and 1970s, thanks to the contributions of Argyris and group at the University of Stuttgart, R. W. Clough and collaborators at Berkeley, Zienkiewicz and colleagues Ernest Hinton, Bruce Irons [58], and others at Swansea University, Philippe G. Ciarlet and group at the University of Paris, and Richard Gallagher and group at Cornell University. More catalyst was delivered during those years by utilizing open supply restricted element schemes. NASA funded the initial version of NASTRAN, and UC Berkeley widely distributed the restricted element program SAP IV [59]. In Norway, the boat grouping humanity Det Norske Veritas (currently DNV GL) created SESAM in 1969 to be used in the research of boats [60]. A thorough numerical premise to FEM was given in 1973 through a study [61]. The method has been summed up for the mathematical demonstration of real frameworks in a huge collection of design disciplines, e.g., electromagnetism, warmness moves, and liquid elements. References [62–68] provide further information.

Because of the preceding literature, it was discovered that no consideration has previously been given to researching the characteristics of bioconvection and moving microorganisms in the flows of magnetized generalized Burgers' nanoliquids with Fourier's and Fick's laws and convective border constraints. To fill this void, the Burgers' nanofluid was incorporated into the interpretation, along with the Cattaneo–Christov mass and heat diffusion theory in the presence of Brownian and thermophoretic diffusion. The primary goal of this extensive research was to optimize heat transfer utilizing nanofluids. The expanded fluid model was chosen as a result of the abovementioned uses of non-Newtonian fluids and nanofluids in the literature. A similarity transformation was used to reduce the problem to ODE dimensions. The physical situation (Figure 1) was modeled in the current investigation as a stretchable sheet. This work is extremely beneficial in a variety of technical and industrial domains. The higher-order nonlinear ODEs that resulted were solved using COMSOL software to obtain mathematical results of non-linear equations via G-FEM. The effect of diverse flowing factors on the rapidity, energy, and concentricity of a Burgers' nanoliquid was graphically examined. In addition, the Nusselt, Sherwood, and consistency quantities of the Burgers' nanofluid were tabulated and studied.

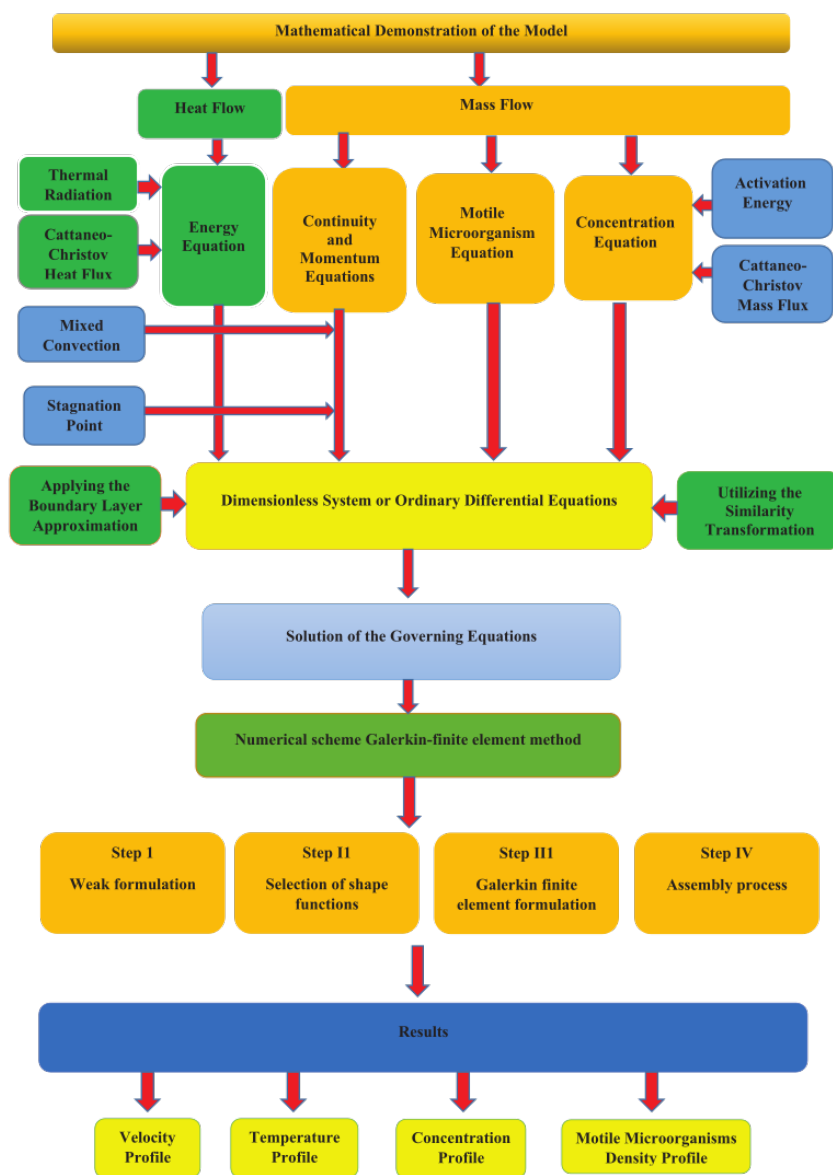


Figure 1. Flow chart of the proposed mathematical model.

2. Governing Equations and Material

Consider the 2D steady flowing of a magnetized generalized Burgers’ nanoliquid over a stretchable surface examining the characteristics of bioconvection and moving micro-organisms across the fluid flow in the x -path. The xy -coordinate system is taken where the x -axis is along the path of the flowing, and the y -axis is normal to the flowing with a stretching rapidity $u = U_w = cx$, as depicted in Figure 2. The magnetic field with potent B_0 is applied. The Burgers’ nanoliquid is anticipated to be a diluted suspension through a homogenous gyrotactic microbes distribution. It is to be noted that gyrotactic microbes’ swimming velocity and swimming direction are not influenced owing to the presence of nanoparticles when suspended the nanoparticles’ concentration is lower than 1%. Further assume that the bio convection impact is impelled when the suspended nanoparticles’ concentration is low. The wall is preserved at a fixed temperature (T_w) and concentricity (C_w). A cooled stretched surface scenario $T_w < T_\infty$ and $C_w < C_\infty$ is taken into consideration. The concentration of species in this research is supposed to be on the high side; thus, the impacts of activation energy and bilateral reaction are considerable.

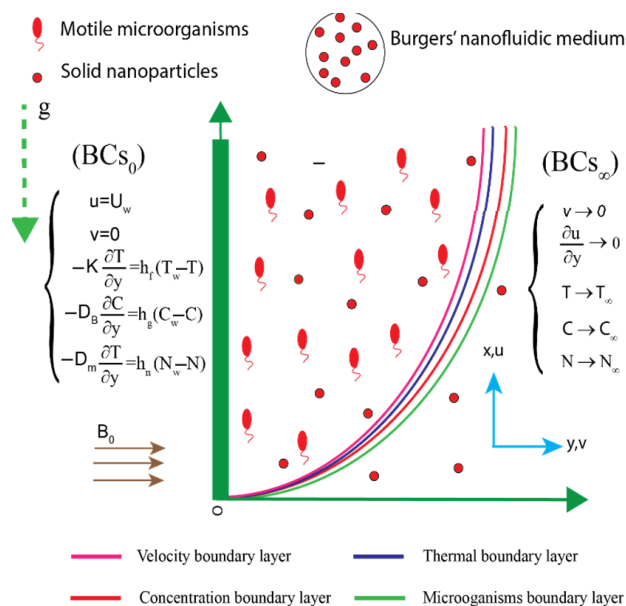


Figure 2. Flow chart for a current problem.

Taking into account the hypotheses proposed, the regulating formulas and appropriate boundary constraints for the Burgers' nanofluid flowing are as follows [69,70]:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0. \tag{1}$$

$$\begin{aligned}
 & u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + \lambda_1 \left(u^2 \frac{\partial^2 u}{\partial x^2} + v^2 \frac{\partial^2 u}{\partial y^2} + 2uv \frac{\partial^2 u}{\partial x \partial y} \right) \\
 & + \lambda_2 \left[u^3 \frac{\partial^3 u}{\partial x^3} + v^3 \frac{\partial^3 u}{\partial y^3} + u^2 \left(\frac{\partial v}{\partial x} \frac{\partial^2 u}{\partial x \partial y} - \frac{\partial u}{\partial x} \frac{\partial^2 v}{\partial x^2} + \frac{\partial u}{\partial x} \frac{\partial^2 u}{\partial x^2} \right) \right. \\
 & + 3v^2 \left(\frac{\partial v}{\partial y} \frac{\partial^2 u}{\partial y^2} + \frac{\partial v}{\partial y} \frac{\partial^2 u}{\partial x \partial y} \right) + 3uv \left(u \frac{\partial^3 u}{\partial x^2 \partial y} + v \frac{\partial^3 u}{\partial x \partial y^2} \right) \\
 & \left. + 2uv \left(\frac{\partial v}{\partial y} \frac{\partial^2 u}{\partial x \partial y} + \frac{\partial v}{\partial x} \frac{\partial^2 u}{\partial y^2} - \frac{\partial u}{\partial y} \frac{\partial^2 v}{\partial x \partial y} + \frac{\partial u}{\partial y} \frac{\partial^2 u}{\partial x^2} \right) \right] \\
 & = v \lambda_3 \left(v \frac{\partial^3 u}{\partial y^3} + u \frac{\partial^3 u}{\partial x \partial y^2} - \frac{\partial u}{\partial x} \frac{\partial^2 u}{\partial y^2} - \frac{\partial u}{\partial y} \frac{\partial^2 v}{\partial y^2} \right) + v \frac{\partial^2 u}{\partial y^2} \\
 & + v \lambda_4 \left[u^2 \frac{\partial^4 u}{\partial x^2 \partial y^2} + 2uv \frac{\partial^4 u}{\partial x \partial y^3} + v \frac{\partial u}{\partial y} \frac{\partial^3 u}{\partial x \partial y^2} - u \frac{\partial u}{\partial y} \frac{\partial^4 u}{\partial x^2 \partial y^2} \right. \\
 & - 2u \frac{\partial u}{\partial y} \frac{\partial^3 v}{\partial x \partial y^2} + u \frac{\partial v}{\partial x} \frac{\partial^3 u}{\partial y^3} + v^2 \frac{\partial^4 u}{\partial y^4} + 3v \frac{\partial v}{\partial y} \frac{\partial^3 u}{\partial y^3} - v \frac{\partial u}{\partial y} \frac{\partial^3 v}{\partial y^3} \\
 & \left. - u \frac{\partial^2 u}{\partial x^2} \frac{\partial^2 u}{\partial y^2} + \left(\frac{\partial u}{\partial x} \right)^2 \frac{\partial^2 u}{\partial y^2} - u \frac{\partial^2 u}{\partial x \partial y} \frac{\partial^2 v}{\partial y^2} \right] + \frac{dU_e}{dx} \\
 & - \frac{\sigma B_0^2}{\rho_f} \left[u - U_e + v \lambda_1 \frac{\partial u}{\partial y} \right. \\
 & \left. + \lambda_2 \left(u \frac{\partial v}{\partial x} \frac{\partial^2 u}{\partial y^2} - v \frac{\partial u}{\partial x} \frac{\partial^2 u}{\partial y^2} v^2 \frac{\partial^2 u}{\partial y^2} + uv \frac{\partial^2 u}{\partial y^2} \right) \right] \\
 & + \frac{1}{\rho_f} \left[(1 - C_\infty) \rho_f \beta^{**} g^* (T - T_\infty) - (\rho_p - \rho_f) g^* (C - C_\infty) - (N - N_\infty) g^* \gamma (\rho_m - \rho_f) \right]. \tag{2}
 \end{aligned}$$

$$\begin{aligned}
 u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = & \alpha \frac{\partial^2 T}{\partial y^2} + \frac{\partial}{\partial y} \left(\frac{16\alpha\sigma^*T_\infty^3}{3k^*} \frac{\partial T}{\partial y} \right) + \frac{Q_o}{\rho C_p} (T - T_\infty) \\
 & + \lambda_t^* \frac{Q_o}{\rho C_p} \left(v \frac{\partial T}{\partial y} + u \frac{\partial T}{\partial x} \right) \\
 & + \lambda_t^* \tau D_B \left(u \frac{\partial^2 C}{\partial x \partial y} \frac{\partial T}{\partial y} + u \frac{\partial C}{\partial y} \frac{\partial^2 T}{\partial x \partial y} + v \frac{\partial^2 C}{\partial y^2} \frac{\partial T}{\partial y} + v \frac{\partial C}{\partial y} \frac{\partial^2 T}{\partial y^2} \right) \\
 & + \lambda_t^* \tau \frac{D_T}{T_\infty} \left(\frac{\partial T}{\partial y} \right)^2 + 2\lambda_t^* \tau \frac{D_T}{T_\infty} \left(u \frac{\partial T}{\partial y} \frac{\partial^2 T}{\partial y^2} + v \frac{\partial^2 T}{\partial y^2} \frac{\partial T}{\partial y} \right) \\
 & - \lambda_t \left[u^2 \frac{\partial^2 T}{\partial x^2} + v^2 \frac{\partial^2 T}{\partial y^2} + 2uv \frac{\partial^2 T}{\partial x \partial y} + \frac{\partial T}{\partial x} \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) \right. \\
 & \left. + \frac{\partial T}{\partial y} \left(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) \right]. \tag{3}
 \end{aligned}$$

$$\begin{aligned}
 u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = & D_B \frac{\partial^2 C}{\partial y^2} + \lambda_c^* \left(\frac{D_T}{T_\infty} \right) \left(\frac{\partial^2 T}{\partial y^2} + \frac{\partial v}{\partial y} \frac{\partial^2 T}{\partial y^2} + \frac{\partial u}{\partial y} \frac{\partial^3 T}{\partial x \partial y} \right) \\
 & - Kr^2 (C - C_\infty) \left(\frac{T}{T_\infty} \right)^n \exp \left(\frac{-E_a}{k T} \right) - \lambda_c^* k_c \left(v \frac{\partial C}{\partial y} + u \frac{\partial C}{\partial x} \right) \\
 & - \lambda_c^* \left[u^2 \frac{\partial^2 C}{\partial x^2} + v^2 \frac{\partial^2 C}{\partial y^2} + 2uv \frac{\partial^2 C}{\partial x \partial y} + \frac{\partial C}{\partial x} \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) \right. \\
 & \left. + \frac{\partial C}{\partial y} \left(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) \right]. \tag{4}
 \end{aligned}$$

$$u \frac{\partial N}{\partial x} + v \frac{\partial N}{\partial y} + \frac{b W_c}{(C_w - C_\infty)} \left[\frac{\partial}{\partial y} \left(N \frac{\partial C}{\partial y} \right) \right] = D_m \frac{\partial^2 N}{\partial y^2} \tag{5}$$

having boundary conditions

$$\left. \begin{aligned}
 u = U_w = cx, v = 0, -k \frac{\partial T}{\partial y} = h_f (T_w - T), \\
 -D_B \frac{\partial C}{\partial y} = h_g (C_w - C), \quad -D_m \frac{\partial N}{\partial y} = h_n (N_w - N) \text{ at } y = 0 \\
 v \rightarrow 0, \frac{\partial u}{\partial y} \rightarrow 0, T \rightarrow T_w, C \rightarrow C_w, N \rightarrow N_w \text{ as } y \rightarrow \infty.
 \end{aligned} \right\} \tag{6}$$

The above governing equations are solved by following suitable transformations:

$$\xi = y \sqrt{\frac{c}{v}}, u = cxf', v = -\sqrt{cv} f, \theta = \frac{T - T_\infty}{T_w - T_\infty}, \phi = \frac{C - C_\infty}{C_w - C_\infty}, \chi = \frac{N - N_\infty}{N_w - N_\infty}. \tag{7}$$

where $f, \theta, \phi,$ and χ are functions of ξ . The following equations are obtained:

$$\begin{aligned}
 f''' - (f')^2 + ff'' + \alpha_1 [f^2 f''' - 2ff'f''] - \alpha_2 [3f^2 (f'')^2 - f^3 f^{iv} + \\
 2f(f')^2 f'''] + \alpha_3 [(f'')^2 - ff^{iv}] + f'''' + \alpha_4 [ff'f^{iv} - 2ff''f'''] + \\
 f^2 f^v + (f')^2 f''' + f'(f'')^2 - M^2 [f' - \alpha_1 ff'' + \alpha_2 f^2 f'''] + M^2 K + \\
 K^2 + \delta [\theta - Nr\phi - Nc\chi] = 0, \tag{8}
 \end{aligned}$$

$$\left(1 + \frac{4}{3} Rd \right) \theta'' + Pr(\delta\theta + f\theta') + Pr\lambda_T [\delta f\theta' + Nt(\theta')^2 - Nb(f\theta'\phi'' - f\theta''\phi')] + 2Ntf'\theta'' - (f^2\theta'' - ff'\theta') = 0, \tag{9}$$

$$\begin{aligned}
 \phi'' + LePr \left[-f\phi' - \sigma^* (1 + \mu\theta)^n \exp \left(\frac{-E}{1 + \mu\theta} \right) \phi - \lambda_c K_c f\phi' \right] + \\
 LePr\lambda_c \left[-f^2\phi'' - ff'\phi - LePr \frac{Nt}{Nb} (\theta'' + f'\theta'') \right] = 0, \tag{10}
 \end{aligned}$$

$$\chi'' + Lbf\chi' - Pe[(\chi + \omega)\phi'' + \chi'\phi'] = 0. \tag{11}$$

with boundary conditions

$$\left. \begin{aligned} f = 0, f' = 1, \theta' = -\gamma_1(1 - \theta(\xi)), \phi' = -\gamma_2(1 - \phi(\xi)), \\ \phi' = -\gamma_2(1 - \phi(\xi)), \chi' = -\gamma_3(1 - \chi(\xi)) \text{ at } \xi = 0, \\ f' \rightarrow K, f'' \rightarrow 0, \theta \rightarrow 0, \phi \rightarrow 0, \chi \rightarrow 0 \text{ as } \xi \rightarrow \infty. \end{aligned} \right\} \quad (12)$$

Diverse non-dimensional factors occurring in (8)–(12) are provided below:

$$\left. \begin{aligned} \alpha_1 = c\lambda_1, \quad \alpha_2 = c^2\lambda_2, \quad \alpha_3 = c\lambda_3, \quad \alpha_4 = c^2\lambda_4, M = \sqrt{\frac{\sigma B_0^2}{\rho_f}}, \\ \lambda = \frac{(1 - C_\infty)\beta^{**}g^*(T_w - T_\infty)}{c^2x}, Nr = \frac{(\rho_p - \rho_f)g^*(C_w - C_\infty)}{(1 - C_\infty)\beta^{**}\rho_f(T_w - T_\infty)}, \\ \delta = \frac{Q_0}{c\rho C_p}, \lambda_T = c\lambda_t^*, Pr = \frac{\nu}{\alpha}, Nc = \frac{(\rho_m - \rho_f)\gamma(N_w - N_\infty)}{(1 - C_\infty)\beta^{**}\rho_f(T_w - T_\infty)}, \\ Nb = \frac{\tau D_B(C_w - C_\infty)}{\nu}, Rd = \frac{4\sigma^*T_\infty^3}{k^*}, Nt = \frac{\tau D_T(T_w - T_\infty)}{\nu T_\infty}, \\ \lambda_c = c\lambda_c^*, Le = \frac{\alpha}{D_B}, E = \frac{-E_a}{\kappa T_\infty}, \mu = \frac{(T_w - T_\infty)}{T_\infty}, \sigma^* = \frac{Kr^2}{c}, \\ \frac{Nt}{Nb} = \frac{D_T(T_w - T_\infty)}{D_B T_\infty(C_w - C_\infty)}, Lb = \frac{\nu}{D_m}, Pe = \frac{bW_c}{D_m}. \end{aligned} \right\} \quad (13)$$

where $\alpha_1, \alpha_3, \alpha_4$ are Deborah’s numbers, while α_2 is a parameter of the Burgers’ fluid. $M, Nr,$ and Nc signify the magnetic field parameter, buoyancy ratio number, and Rayleigh number of bioconvection, respectively. Pr is the Prandtl number while Nb is utilized as a parameter for Brownian motion. δ is used for a different number of microorganisms whereas Rd is a parameter for thermal radiation. Le and E represent the Lewis number and activation energy. μ is the temperature difference parameter while σ^* is a chemical reaction factor. Lb is the Lewis parameter of bio-convection and Pe is used as the Peclet parameter. Moreover, $\gamma_1, \gamma_2, \gamma_3, Nt, \lambda_T,$ and λ signify the Biot number of heat, Biot number of solution, Biot number of microorganisms, thermophoresis parameter, relaxation parameter of heat, and parameter of mixed convection, respectively.

3. Galerkin Finite Element Technique

The corresponding boundary constraints of the present system were computationally simulated using FEM. FEM is based on the partitioning of the desired region into components (finite). FEM [71] is covered in this section. Figure 3 depicts the flowing chart of the finite element technique. This procedure has been employed in numerous computational fluid dynamics (CFD) matters; the benefits of employing this strategy are discussed further below.

Step I: The weak form is derived from the strong form (stated ODEs), and residuals are computed.

Step II: To achieve the weak form, shape functions are taken linearly, and FEM is used.

Step III: The assembly method is used to build stiffness components, and a global stiffness matrix is created.

Step-IV: Using the Picard linearizing technique, an algebraic framework (nonlinear equations) is produced.

Step-V: Algebraic equations are simulated utilizing appropriate halting criterion through 10^{-5} (supercomputing tolerances).

$$\left| \frac{\xi_{i+1} - \xi_i}{\xi_i} \right| < 10^{-5}.$$

Further, The Galerkin finite element technique’s flow chart is depicted in Figure 2.

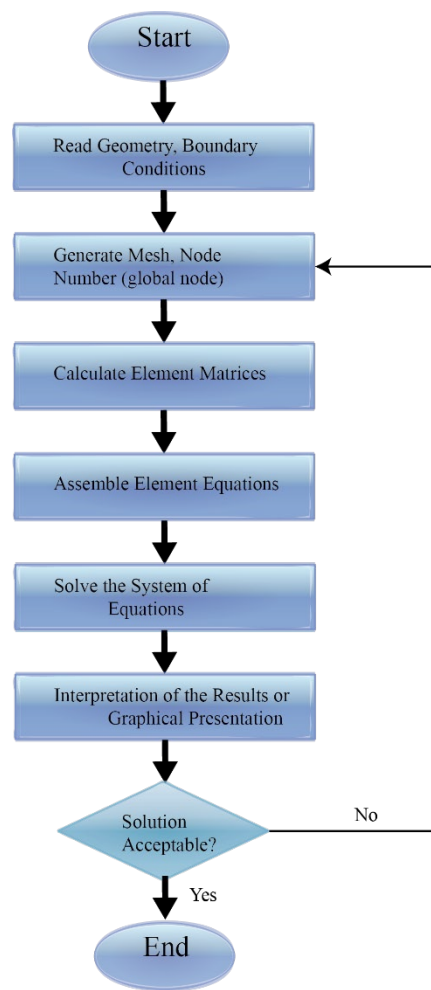


Figure 3. Flow chart of G-FEM.

4. Validity of Code

The computational technique’s authenticity was evaluated by comparing the heat transition rate from the previous methods to the authenticated results of previous research [72]. Table 1 compares the findings of the present study to the findings of the previous study. The present study is significantly compared, and the outcomes are remarkably accurate.

Table 1. Comparison of $-\theta'(0)$ with alteration in Prandtl number, taking $\delta = Rd = \lambda_T = Nt = \gamma_1 = \gamma_2 = \gamma_3 = 0$ and $Nb = 0$.

P_r	Qureshi [72]	This Study
0.72	0.8087618	0.8087612
1.0	1.0000000	1.0000000
3.0	1.9235742	1.9235734
7.0	3.0731465	3.0731465
10	3.7205542	3.7205511

The important physical parameters in this problem are the local heat and mass fluxes, as well as the local motile microorganisms flux, which are specified as follows:

$$Nu_x = \frac{xq_w}{k(T_w - T_\infty)}, \quad Sh_x = \frac{xq_m}{D_B(\phi_w - \phi_\infty)}, \quad Nn_x = \frac{xq_n}{D_m(N_w - N_\infty)}, \quad (14)$$

in which

$$q_w = -k \left(\frac{\partial T}{\partial y} \right)_{y=0}, q_m = -D_B \left(\frac{\partial \phi}{\partial y} \right)_{y=0}, q_n = -D_m \left(\frac{\partial N}{\partial y} \right)_{y=0}. \quad (15)$$

Using the similarity transform presented above, Equation (14) can be described as follows:

$$Nu_x Re_x^{-1/2} = -\theta'(0), Sh_x Re_x^{-1/2} = -\phi'(0), Nn_x Re_x^{-1/2} = -\chi'(0). \quad (16)$$

5. Results and Discussion

To enhance understanding of the analysis, the results are demonstrated in tables and figures showing the impact of the thermofluid parameters on the flowing velocity, heat distribution, mass transfer, and motile microbes' distribution. These are presented in Figures 4–28 and Tables 1 and 2 for a variational increase in the thermophysical terms. Figures 4–7 demonstrate the material effect on flowing fluid velocity fields. A rise in dilatant Deborah number α_1 resulted in a significant decline of the nanofluid velocity magnitude as displayed in Figure 4. This is a result of enhancing shear material thickness that stimulated the bonding force. The opposed nanoparticles' molecular interaction reduced thermal transfer, which consequently decreased the velocity distribution. Moreover, the Burgers' nanoliquid material term α_2 increased the flow rate distribution as seen in Figure 5. The pseudoplastic term inspired Fick's and Fourier's thermal conductivity to boost the spinning of motile microbes along with the stretching sheet. Accordingly, the random motion of the nanoparticles was propelled, thereby encouraging the current-carrying nanofluid. As such, the flow rate past the streaming boundless medium was raised in magnitude. Likewise, the Deborah pseudoplastic number α_3 and α_4 enhanced the flow regime towards the far stream as presented in Figures 6 and 7. The flow velocities were significantly raised with increasing pseudoplastic material terms. As the terms are increased, the nanoparticles' bonding force is dominated by an internally generated heat to allow free molecular interaction of the fluid particles. Therefore, the velocity distributions were enhanced with rising Deborah numbers across the flow domain.

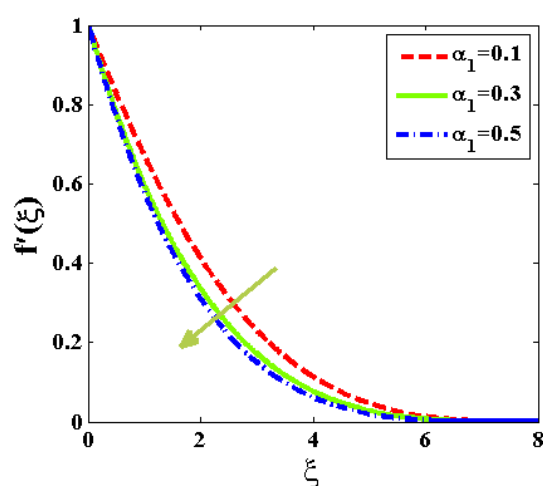


Figure 4. Outlines of f' at diverse quantities of α_1 .



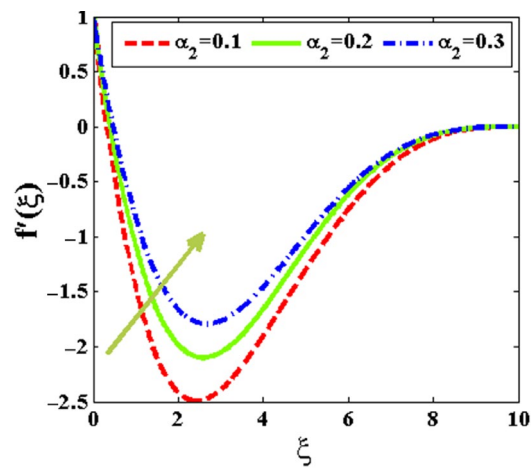


Figure 5. Outlines of f' at diverse quantities of α_2 .

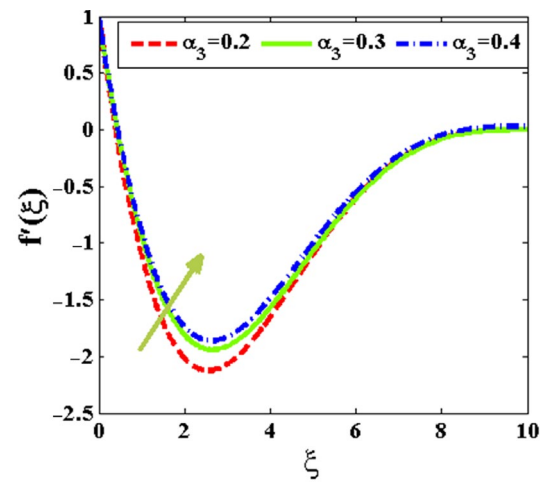


Figure 6. Outlines of f' at diverse quantities of α_3 .

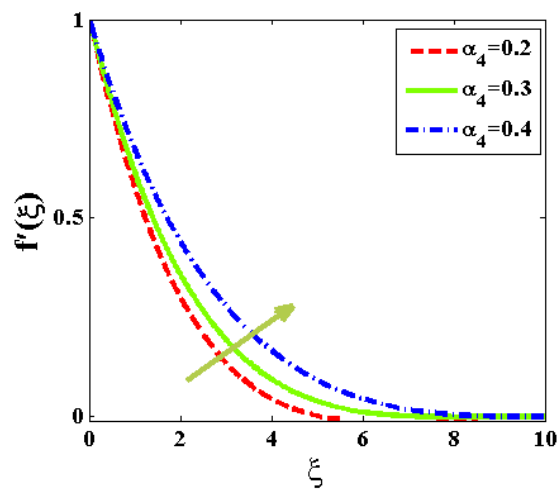


Figure 7. Outlines of f' at diverse quantities of α_4 .



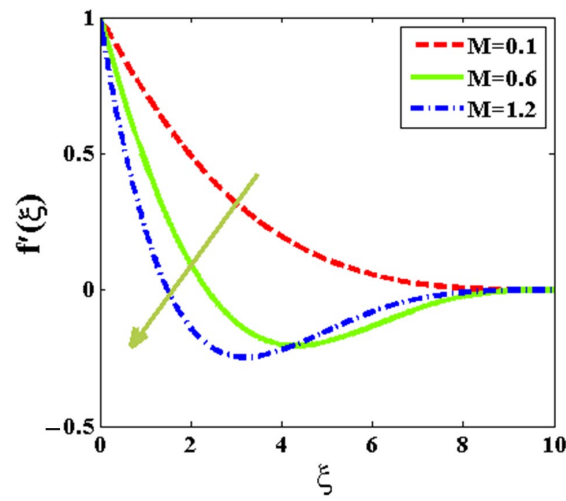


Figure 8. Outlines of f' at diverse quantities of M .

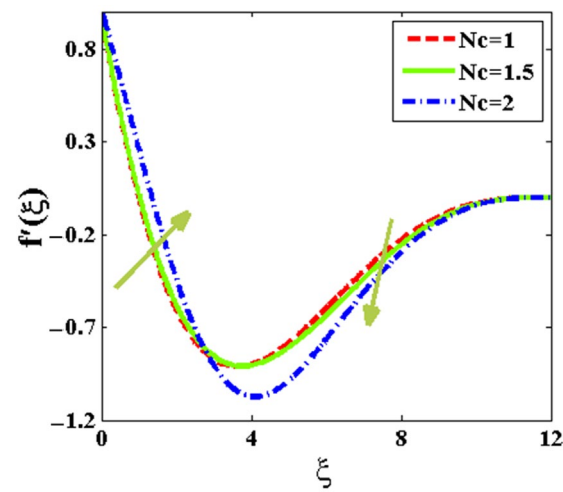


Figure 9. Outlines of f' at diverse quantities of Nc .

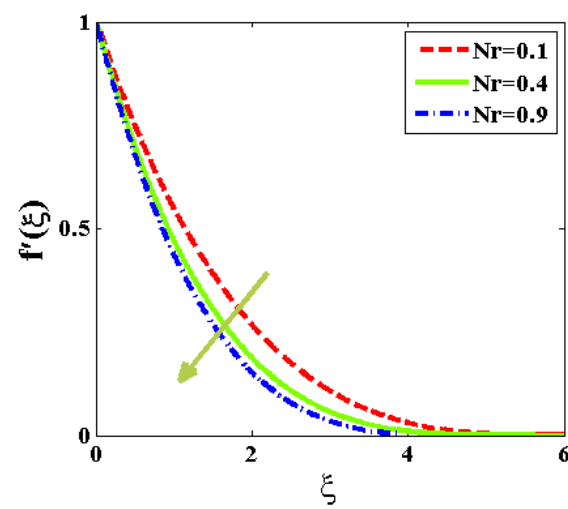


Figure 10. Outlines of f' at diverse quantities of Nr .

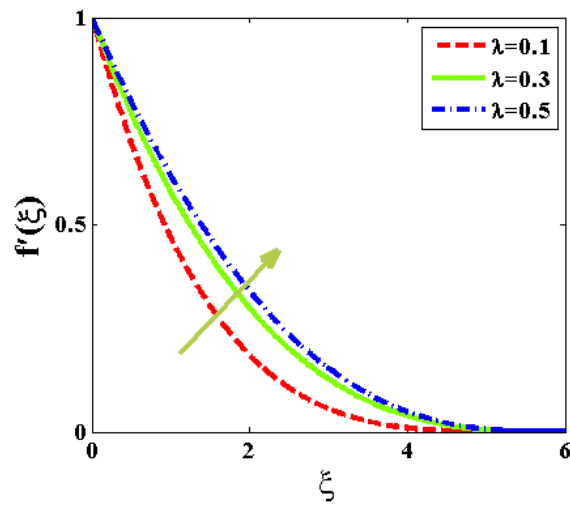


Figure 11. Outlines of f' at diverse quantities of λ .

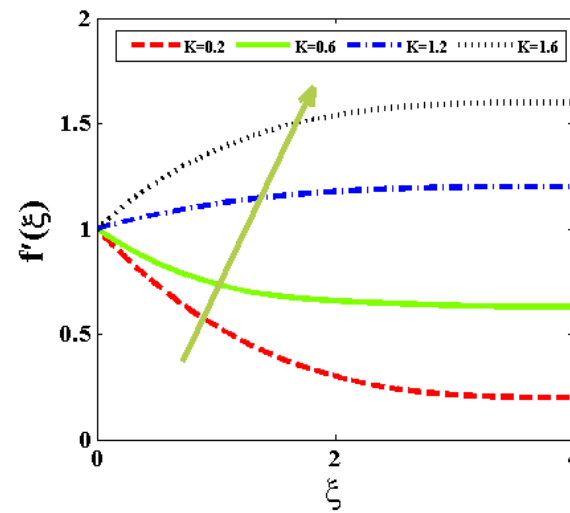


Figure 12. Outlines of f' at diverse quantities of K .

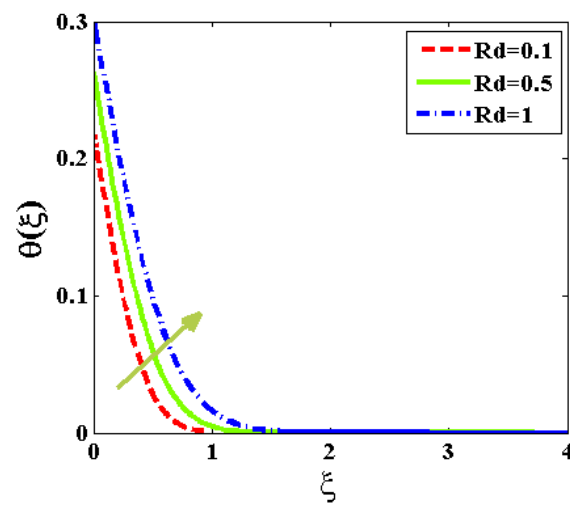


Figure 13. Outlines of θ at diverse quantities of Rd .

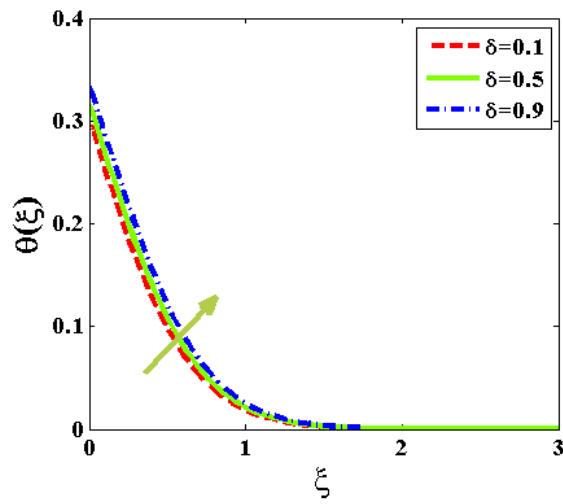


Figure 14. Outlines of θ at diverse quantities of δ .

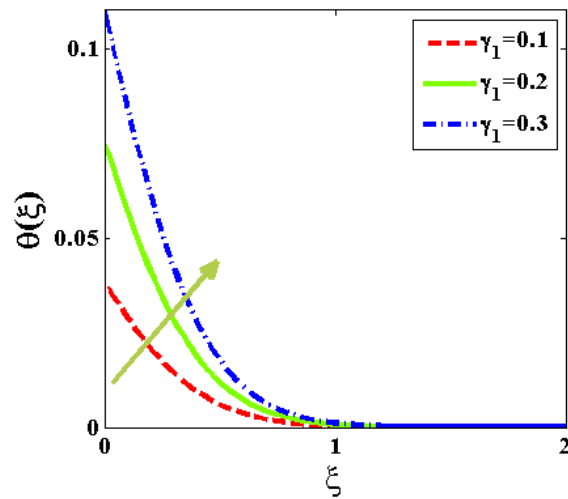


Figure 15. Outlines of θ at diverse quantities of γ_1 .

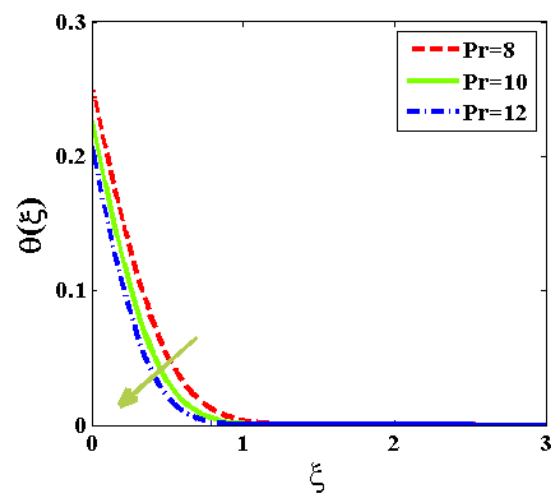


Figure 16. Outlines of θ at diverse quantities of Pr .

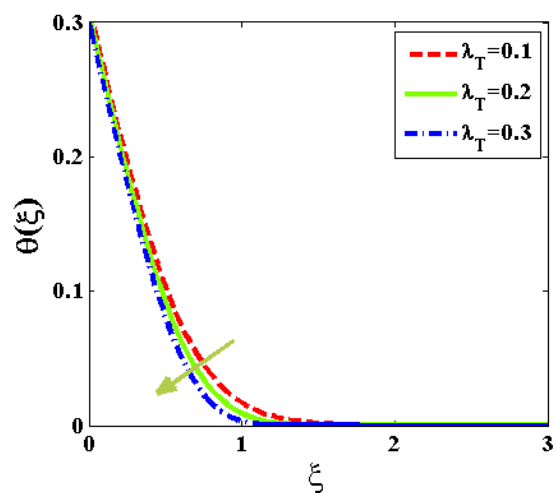


Figure 17. Outlines of θ at diverse quantities of λ_T .

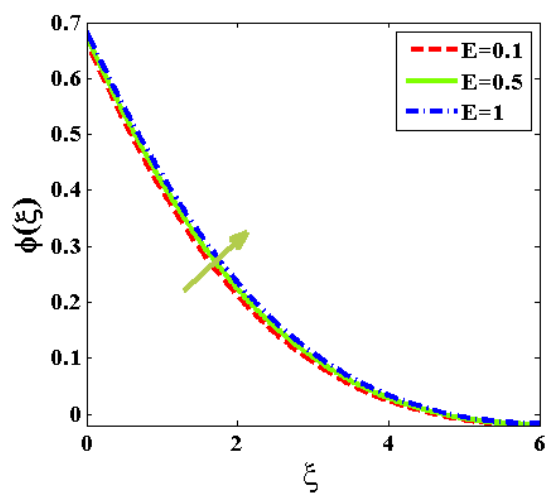


Figure 18. Outlines of ϕ at diverse quantities of E .

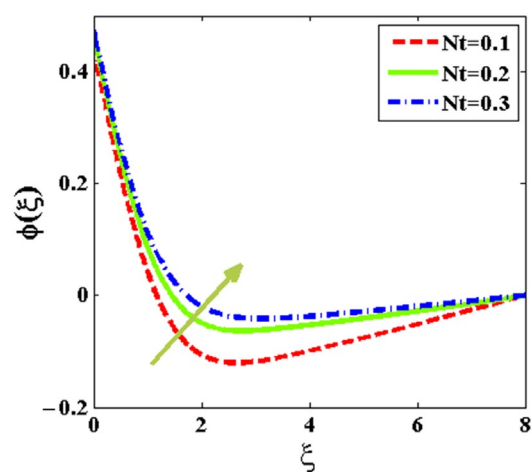


Figure 19. Outlines of ϕ at diverse quantities of Nt .

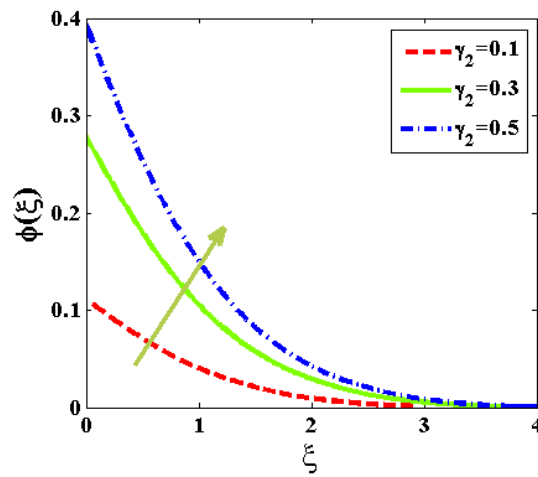


Figure 20. Outlines of ϕ at diverse quantities of γ_2 .

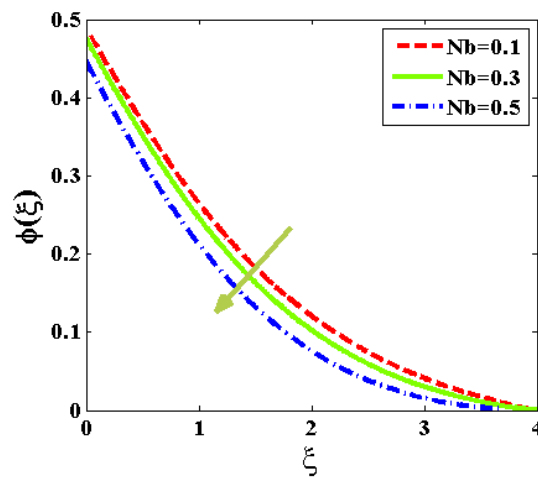


Figure 21. Outlines of ϕ at diverse quantities of Nb .

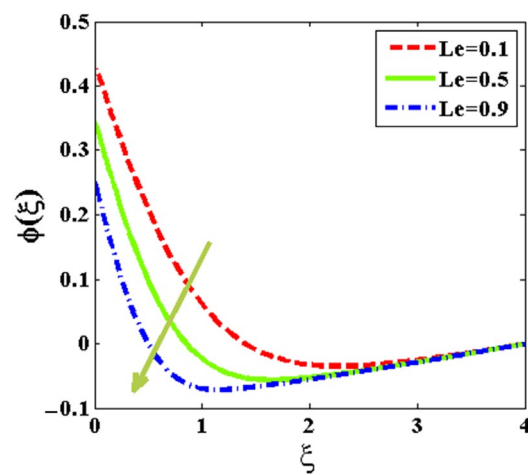


Figure 22. Outlines of ϕ at various values of Le .

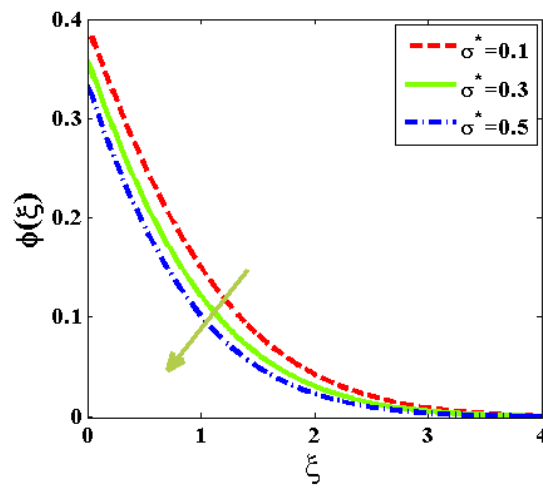


Figure 23. Outlines of ϕ at diverse quantities of σ^* .

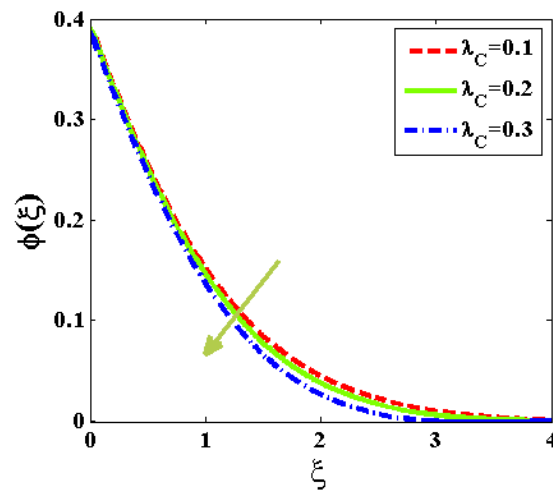


Figure 24. Outlines of ϕ at diverse quantities of λ_C .

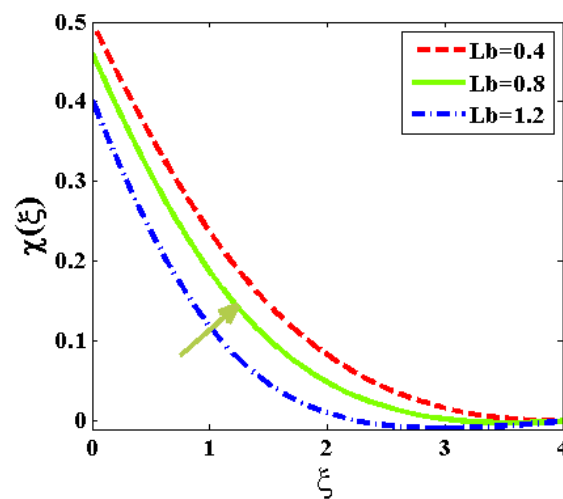


Figure 25. Outlines of χ at diverse quantities of Lb .

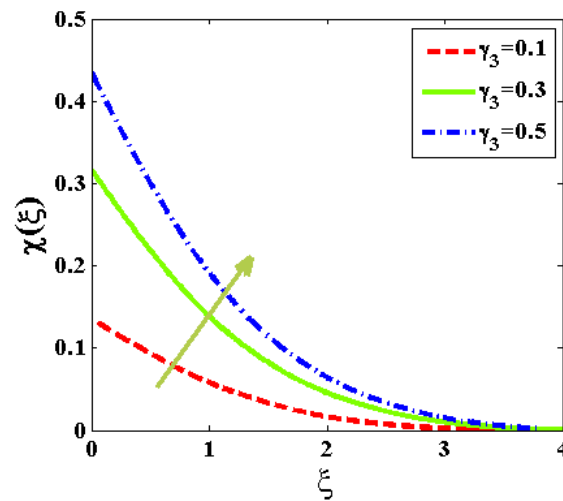


Figure 26. Outlines of χ at diverse quantities of γ_3 .

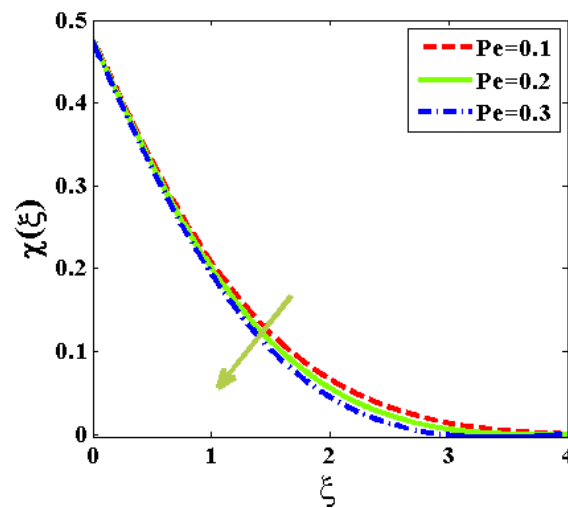


Figure 27. Outlines of χ at diverse quantities of Pe .

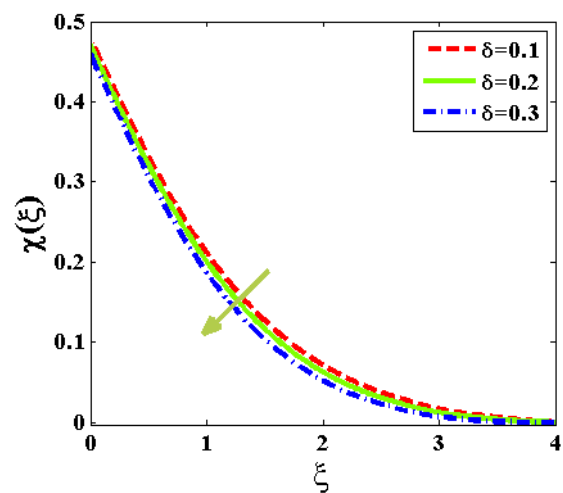


Figure 28. Outlines of χ at diverse quantities of δ .

In Figure 8, the increasing number of the magnetized force opposed the flowing velocity outline as presented. The motile microorganisms were damped due to an induced electromagnetic force that resists the nanoparticles' free collision. This accordingly affects

heat transfer, thereby meaningfully impacting the flow rate. The impact of the bioconvective Rayleigh quantity on the nanofluid flow rapidity is investigated in Figure 9. The Rayleigh number is connected with the convective buoyancy-driven flow; an increase in the Rayleigh number caused a rising flow velocity field near the stretching wall due to an enhanced heat gradient. The effect reduces along the far stream because of an increased fluid shear stress, which restricts the free flow of motile microbes. Hence, the velocity profile reduced and increased with the Rayleigh number variation. The sensitivity of the flow velocity to rising buoyancy ratio number Nr is displayed in Figure 10. The velocity distribution was reduced as a result of the dominance of the fluid viscosity over the thermal buoyancy. As observed, the motile microorganisms of the nanofluid interaction were hampered, resulting in a significant decrease in the flow rate field. In Figure 11, the effect of increasing combined convective term λ on the rapidity distribution is examined. The combined natural and force convection denoting mixed convection raised the up-swimming of the microorganisms in a suspended nanoparticle, which led to an enhanced flow rate profile. The flow dimension is a result of the acted coupled convection mechanism on the Burger's nanofluid, which propels high heat transfer past the stretched sheet. As such, the buoyancy and pressure forces interacted to boost heat propagation, which inspired the magnetized fluid velocity field. As well, in Figure 12, the parameter K significantly increased the velocity field of the motile microbes in the Burger's nanofluid. The thermal conductivity of the fluid is stretched to create a free particle collision, thereby magnifying the velocity distribution.

Figures 13–15 display the influence of the radiation term Rd , bio-convective term δ , and heat Biot number γ_1 on the temperature distribution. The terms are a strong source of heat generation that stimulate internal heating. As observed, the heat propagation in the stretching device was boosted by the existence of Fourier and Fick thermal conductivity and low thermal diffusion. Hence, the temperature profile was increased as the nanoparticle random movement was enhanced. Therefore, in a chemical and thermal system, the terms that enhance heat transfer should be monitored to guide against chemical reaction blowup. In Figures 16 and 17, The response of the heat transfer to enhancing Prandtl number Pr and heat relaxation term γ_T is demonstrated. As noticed, the temperature field was reduced in magnitude along with the swimming motile microorganisms due to the high diffusion of heat to the environment, which was a result of a thinner energy boundary layer. The rising ambient heat dispersion reduces nanoparticles' thermal conductivity. Hence, momentum viscosity dominates the thermal conductivity, thereby restricting Burger's fluid molecular interaction. As such, the temperature distribution is decreased.

The effect of the thermofluid terms on the mass transfer are displayed in Figures 18–24. The sensitivity of the reacting species to varying parameters is shown in the respective plots. In Figures 18–20, the impression of active energy E , thermophoresis term Nt , and the species Biot quantity γ_2 is checked on the concentration distribution. The terms propel the solution concentration field due to the stimulation of internal energy that induced the species reaction along the boundless stream. Motile microorganism reaction close to the stretchable sheet is more noticeable than at far stream because of the rising wall thermal conductivity. Moreover, Burger's nanofluid thermal reaction is boosted to inspire heat transfer, thereby leading to an enhanced chemical concentration distribution. In Figures 21–24, the mass transfer diminished with a variational rise in the Brownian diffusion Nb , Lewis number Le , chemical reaction term σ^* , and relaxation time λ_C . The low heat transfer through nanoparticles and motile microorganisms is due to the high molecular bond and shear stress that resists the concentration profiles. This is as well supported by the species boundary layer viscosity that supports chemical solution diffusion, thereby damping the species mass distribution. The plot of $\chi(\xi)$ against ξ depicting the motile microorganism distribution for parameter variations is given in Figures 25–28. In Figures 25 and 26, the impact of the bioconvective term Lb and microorganism Biot number γ_3 are examined. As is shown, the swimming microorganism distribution is increased with

an enhanced parameter value because of created internal heating. The flow dimensions are due to the high-density gradient caused by the collection of convective macroscopic motion. The Biot number creates microorganism thermal resistances at the surface and inside the body to stimulate heat transfer. Therefore, the motile microbes profiled are propelled. Meanwhile, the opposite effect was obtained for the rising Peclet number Pe and microorganism different number δ as seen in Figures 27 and 28. The flow behavior is due to the shallow random suspensions and volume cell fraction of the motile microorganism dispersion pattern. As such, the microorganism distribution is damped in magnitude significantly.

6. Table Discussion

The numerically computed outcomes for the wall temperature gradient, mass gradient, and the motile microorganisms are presented in Table 2. The impact of different thermophysical terms has been investigated and obtained computationally. As can be seen, a rise or decline in the engineering thermofluid wall quantities could be obtained, a consequence of the thinness or thickness of the boundary layers. The boundary viscidness determines the thermal diffusion, species diffusion, and microorganism volume cell fraction. Therefore, an increase or decrease in the computed values could be obtained depicting various stretching wall effects.

Table 2. Nusselt and Sherwood quantities and consistency amount at the stretching walls.

α_1	α_4	M	E	δ	Nt	Nb	Lb	λ_T	Le	λ_c	$Nu_x Re_x^{-\frac{1}{2}}$	$Sh_x Re_x^{-\frac{1}{2}}$	$Nn_x Re_x^{-\frac{1}{2}}$
0.1	0.2	0.1	0.1	0.1	0.1	0.1	0.8	0.2	0.5	0.2	0.37638	0.33370	0.31245
0.3											0.37637	0.33368	0.31241
0.5											0.37636	0.33366	0.31237
	0.2										0.37638	0.33370	0.31244
	0.3										0.37638	0.33370	0.31245
	0.4										0.37639	0.33371	0.31246
		0.1									0.37449	0.30341	0.31175
		0.6									0.37448	0.30338	0.31171
		1.2									0.37443	0.30328	0.31156
			0.1								0.37449	0.30340	0.31174
			0.5								0.37450	0.30001	0.31166
			1.0								0.37451	0.29711	0.31159
				0.1							0.37449	0.30340	0.31174
				0.2							0.37298	0.30340	0.31701
				0.3							0.37100	0.32076	0.32332
					0.1						0.41908	0.31143	0.31185
					0.2						0.41314	0.30657	0.31178
					0.3						0.40608	0.30495	0.31176
						0.1					0.36629	0.30721	0.31179
						0.3					0.33780	0.31810	0.31194
						0.5					0.30110	0.32900	0.31209
							0.4				0.37449	0.30340	0.24656
							0.8				0.37449	0.30340	0.30087
							1.2				0.37449	0.30340	0.33914
								0.1			0.37607	0.30340	0.31174
								0.2			0.37568	0.30340	0.31174
								0.3			0.37529	0.30340	0.31174
									0.1		0.37449	0.30340	0.31174
									0.5		0.37417	0.35409	0.31293

0.9	0.37411	0.37965	0.31360
0.1	0.37450	0.30280	0.31175
0.2	0.37450	0.30294	0.31175
0.3	0.37450	0.30309	0.31175

7. Conclusions

The developed model describing the flow characteristics of the bioconvection and swimming microorganisms of a magnetized generalized Burgers' nanomaterial with Fourier's and Fick's laws has been considered. Transformed invariant coupled quasilinear differential equations were obtained and solved using the finite element Galerkin technique via COMSOL software. The qualitative and quantitative results are provided graphically and in tables to give a clear insight into the study. The outcomes of the parameter sensitivities study are as follows:

- A significant monotonic increase in the flow velocity is seen for variations in the Rayleigh number and Deborah pseudoplastic number, α_3 and α_4 .
- A growing magnetic field term generates significant electromagnetic force, which increases shear stress and dampens the velocity profile.
- The suspended nanoparticles' heat conduction and distribution of motile microbes are enhanced with rising radiation, bioconvective, and heat Biot number terms.
- The mass transfer and concentricity distribution are decreased for an increasing value of Brownian motion, Lewis number, and relaxation time.
- It is plausible to conclude that increasing the chemical reaction parameter and concentricity relaxation variable or reducing the Prandtl number, concentricity Biot quantity, and active energy factor can considerably enhance the concentration dispersion of nanoparticles.
- A rising value of bioconvective and microorganism Biot number spurred motile microorganism distribution.

The outcomes of this study apply to the promotion of thermal and chemical industrial productivity. As such, more investigation is encouraged along the research direction and study extension can be considered for the annular concentric cylinder flow with Arrhenius chemical kinetics. Some recent developments exploring the significance of the considered research domain are reported by [73–82].

Author Contributions: F.S. and W.J. formulated the problem. F.S., W.J., R.S. and M.R.E. solved the problem. F.S., W.J., T.S., M.S., R.S., S.O.S., M.R.E. and M.B.H. computed and scrutinized the results. All the authors equally contributed to the writing and proofreading of the paper. All authors reviewed the manuscript. All authors have read and agreed to the published version of the manuscript.

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Conflicts of Interest: The authors declare no conflict of interest.

Nomenclature

λ_1, λ_3	relaxation time parameters of Burgers' fluid
λ_2, λ_4	retardation time parameters of Burgers' fluid
E	activation energy
λ_t	relaxation time of heat
λ_c	relaxation time of mass
T	liquid temperature

C	liquid concentration
T_{∞}	ambient temperature
C_{∞}	ambient concentration
D_B	coefficient of diffusion
q	heat flux
J	mass flux
ρ	density
p	pressure
C_p	specific heat capacity
k	thermal conductivity of the liquid

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