

## Double ZIF-L structures with exceptional CO<sub>2</sub> capacity

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### Abstract

*Carbon dioxide emission is an emerging problem nowadays and new methods are designed for its control. In this article, a report on the formation of zeolitic imidazole framework with an apparent double leaf-like morphology DZIF-L is given. The special structure of the materials prevents from aggregation of the particles providing remarkable CO<sub>2</sub> capacity. At 0.1 MPa the CO<sub>2</sub> uptake was  $2.99 \pm 0.06$  mmol/g. The capacity of synthesized material is higher than that of any other structure that was so far identified between single ZIF-L and ZIF-8. Fourier transform infrared (FT-IR), X-ray diffraction (XRD), scanning electron microscopy (SEM) and Brunauer-Emmett-Teller surface area analysis were used to characterize the material.*

Key words: zeolitic imidazole framework, carbon dioxide, uptake, adsorption

### 1. Introduction

The rapid increase of the population and resulting energy consumption contribute to a high emission of pollutants to the atmosphere, from which carbon dioxide is an emerging problem. Therefore, there is a great necessity to develop new effective separation technologies. In recent decades a lot of focus was put on new solvents like ionic liquids or deep eutectic solvents and their use in membrane separation process as well as mixed matrix membranes filled with metal organic frameworks (MOFs). Mixed matrix membranes can incorporate several types of fillers, like zeolites [1–3], silica, activated carbon [4], carbon molecular sieves [5,6], metal organic frameworks (MOFs) [7] and other. Metal-organic frameworks are crystalline materials with high surface area and porosity that form a network of metal ion node coordinated to organic ligands. They are obtained in the reaction of metal salts and organic linkers, like imidazoles, carboxylates etc. which have oxygen or nitrogen atoms built in. Typically, MOFs are obtained by solvothermal method, where the organic and metal precursors are dissolved in polar solvents like water or alcohol [8] and simply mixed to make the product that precipitates from the solution.

Among MOFs there is a large group of materials based on Zn or Co that together with imidazole ligand constitute large molecular structures called zeolitic imidazole frameworks (ZIFs). The bond angle in ZIFs is similar to that in zeolites therefore ZIFs present many characteristics specific for zeolites like stability, high surface area and crystallinity [9] and at the same time advantages of MOFs. Unlike some MOFs ZIFs can be obtained easier and cheaper and are stable in moist conditions and at high temperatures. ZIFs has been widely studied due to the simplicity of the synthesis procedure, sorption capacity and potential in use as a filler for gas separation membranes.

21 Even though the preparation procedure seems to be simple, it should be carefully developed, because  
22 concentration of chemicals, solvent type, pH, agitation speed, temperature, additives [10], aging etc. can  
23 have a remarkable effect on the ZIF type, its structure, shape and size. Mainly ZIF-8 is studied in the  
24 literature, but lately two-dimensional leaf-like shape ZIF-L gained attention. There are several types of  
25 ZIF-L reported in the literature, flower-like, hierarchical and single cushion-shape ZIF-L, which is the  
26 most frequently examined [11–13].

27 Single ZIF-L are mostly studied in the membrane systems. One of the examples is H<sub>2</sub>/CO<sub>2</sub> separation  
28 examined by Yang et al. The authors obtained selectivity of ~208 [14]. Pebax membranes incorporating  
29 ZIF-L for CO<sub>2</sub>/CH<sub>4</sub> separation with the selectivity reaching 19 were also used [15]. Low et al. used ZIF-  
30 L nanoflakes in polyethersulfone ultrafiltration membrane [11]. Valencia et al. used leaf-like zeolite  
31 imidazole framework foams for carbon dioxide capture with the capacity of 0.75 mmol/g for 50% ZIF-  
32 L in the foam, for pure powder CO<sub>2</sub> capacity was 0.9 mmol/g at 298 K and 1 bar [16]. Similar results  
33 for carbon dioxide capacity of single ZIF-L were obtained by Chen et al. [17]. The authors proved higher  
34 CO<sub>2</sub> capacity of ZIF-L (0.94 mmol/g) than that of ZIF-8 (0.68 mmol/g), ZIF-95 and ZIF-100.

35 In the literature more complex forms of ZIF-L can also be found, these are flower-shaped and  
36 hierarchical shapes. Synthesis of flower shaped ZIF-L was reported by Wang et al [18]. CO<sub>2</sub> capacity of  
37 hierarchical ZIF-L was determined by Ding et al at the level of 1.56 mmol/g. Park et al examined wide  
38 range of different ZIFs and reported that ZIF-8 can be obtained by crystal transformation of ZIF-L [19].  
39 Moreover, in research focused on single ZIF-L, a propeller-shaped double structures occur as a defect.  
40 In some studies the CO<sub>2</sub> uptake of single ZIF-L occurred to be higher than that of ZIF-8 [17] and lower  
41 than that of hierarchical and flower-shaped ZIF-L [18,20], for that reason this research focused on  
42 obtaining the least complex three-dimensional ZIF-L structure, namely double ZIF-L (DZIF-L). This  
43 structure should limit aggregation in comparison to single ZIF-L and ZIF-8 that tend to agglomerate  
44 forming a dense layer. Since ZIF-L are often dedicated to membrane systems, such behaviour would  
45 decrease the permeability of resulting membrane and double ZIF-L could resist from aggregation and  
46 may be capable of forming oriented porous surface. In this regard, we expect that this special double  
47 leaf like shape has potential in gas separation applications.

## 48 2. Experimental

### 49 2.1. Preparation of DZIF-L

50 Hydrothermal method for DZIF-L fabrication was used. The molar ratio of the components was set at  
51 1:8:2250, accordingly for Zn<sup>2+</sup>:Im:H<sub>2</sub>O. Zn<sup>2+</sup> ions originated from Zn(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O, supplied by  
52 Chempur Poland, Im source was 2-methylimidazole (99%) from Acros Organics and methanol (99.8%)  
53 from Avantor Performance Materials Poland S.A. All chemicals were used without further purification.  
54 The water solutions of the components were prepared at 298 K and mixed together for the reaction. The  
55 reaction mixture was stirred with a speed of 500 rpm for 5 hours at 288 K. The resulting precipitate was  
5 then twice washed with deionised water and twice with methanol, each time being collected by  
6 centrifugation (4000 rpm for 10 minutes). Then the sample was dried in a vacuum oven at 343 K  
7 overnight.  
8  
9  
0

### 1 2.2. Characterization



63  
64 Prior to the measurements samples were degassed under vacuum at 423 K for 24 h. Nitrogen adsorption  
65 isotherms and total pore volumes were measured using Micromeritics Gemini V Analyzer at 77 K.  
66 Nitrogen adsorption curves were determined in the range of  $P/P_0$  from 0.01 to 0.98. Specific surface area  
67 was calculated using the Brunauer–Emmett–Teller (BET) linear equation in the approximate relative  
68 pressure range from  $P/P_0$  0.05 to 0.3. Total pore volume was calculated at  $P/P_0$  0.95.

69 The morphology of the samples with particle size analysis was investigated by the Schottky field  
70 emission scanning electron microscope SEM (FEI Quanta FEG 250) with an ET secondary electron  
71 detector. The beam acceleration voltage was kept at 10 kV. The samples were coated with gold before  
72 imaging.

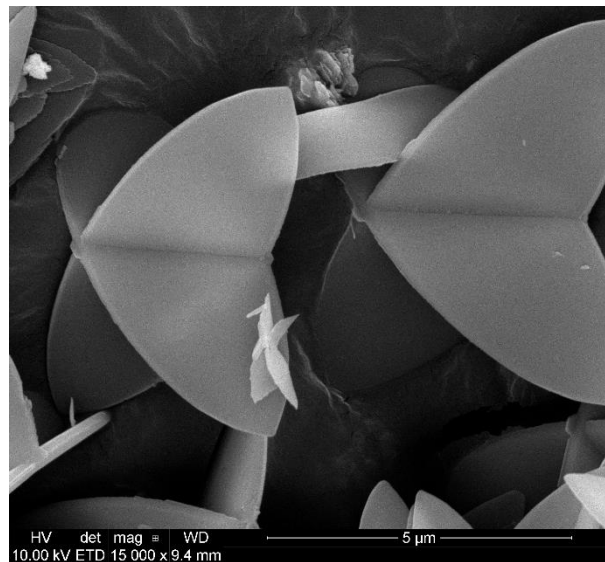
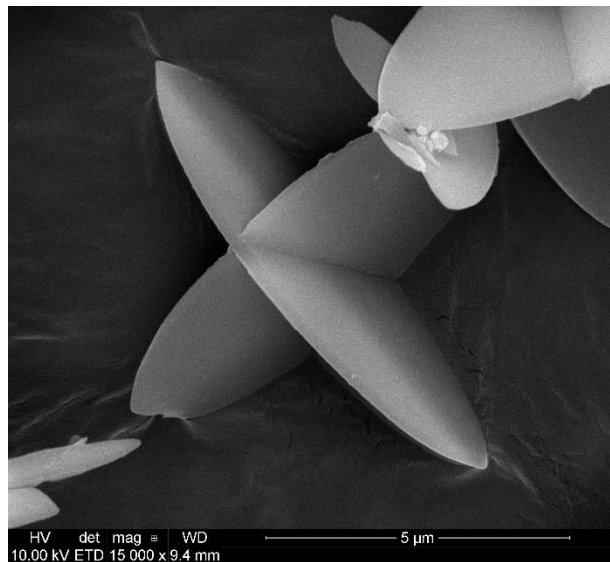
73 X-ray diffraction measurements were made using Cu-K $\alpha$  radiation on a Rigaku Miniflex 600. XRD data  
74 was obtained within the angle range of 5-50 degrees operating at a scanning rate of  $1^\circ \text{ min}^{-1}$ .

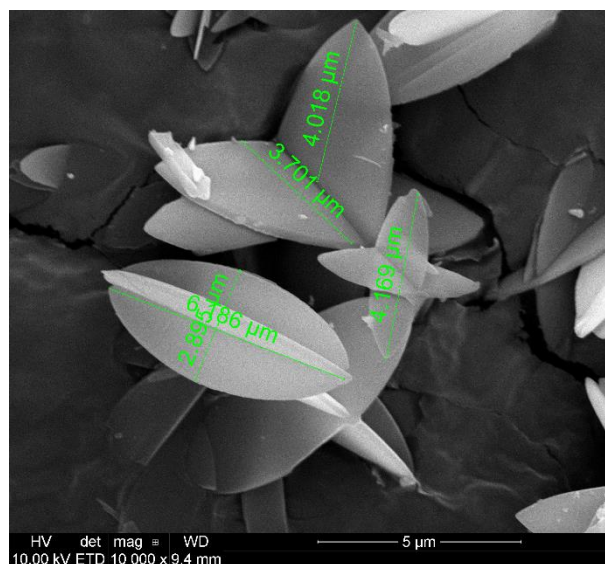
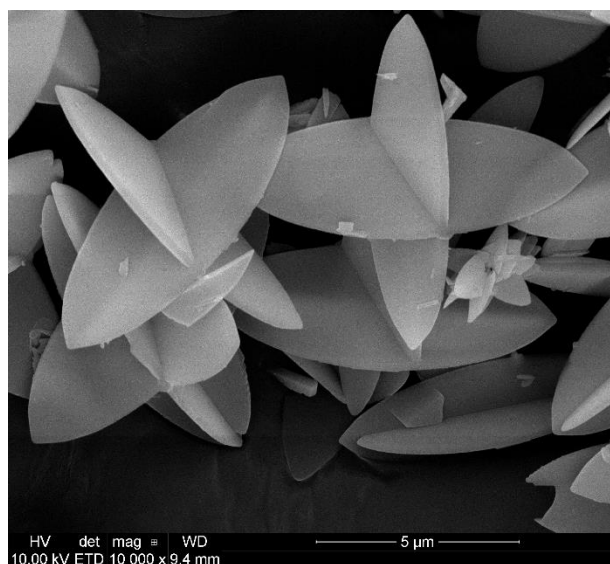
75 The Fourier transform infrared spectrum was recorded in transmittance mode with  $x \text{ cm}^{-1}$  spectra cl  
76 resolution using ThermoSCIENTIFIC Nicolet iS10.

77 The CO<sub>2</sub> adsorption capacity was determined using volumetric method as described in the literature  
78 [18,20]. Briefly, the capacity was determined at 298 K up to 250 kPa. Prior to the test, dry and degassed  
79 samples were placed in the testing chamber and kept under vacuum for 12 h at 373 K. The samples were  
80 cooled to 298 K and pure CO<sub>2</sub> was introduced to reach equilibrium. The equilibrium pressure was  
81 recorded when the value did not change over 4 hours.

### 83 3. Results and discussion

84 The sample morphology was characterized by SEM. The material is white and is a 3D framework with  
85 well-defined leaf-shaped crystals, composed of two ZIF-L structures crossing each other along the long  
86 or short axis. The morphology is well defined and different from that of single ZIF-L and flower-shaped  
87 ZIL-L. As shown in Figure 1 the average nominal size of the DZIF-L was found to be 7.8  $\mu\text{m}$  along the  
88 long axis and 3.4  $\mu\text{m}$  along the short axis. The main difference between these two identified structures  
89 is the ration of length to width

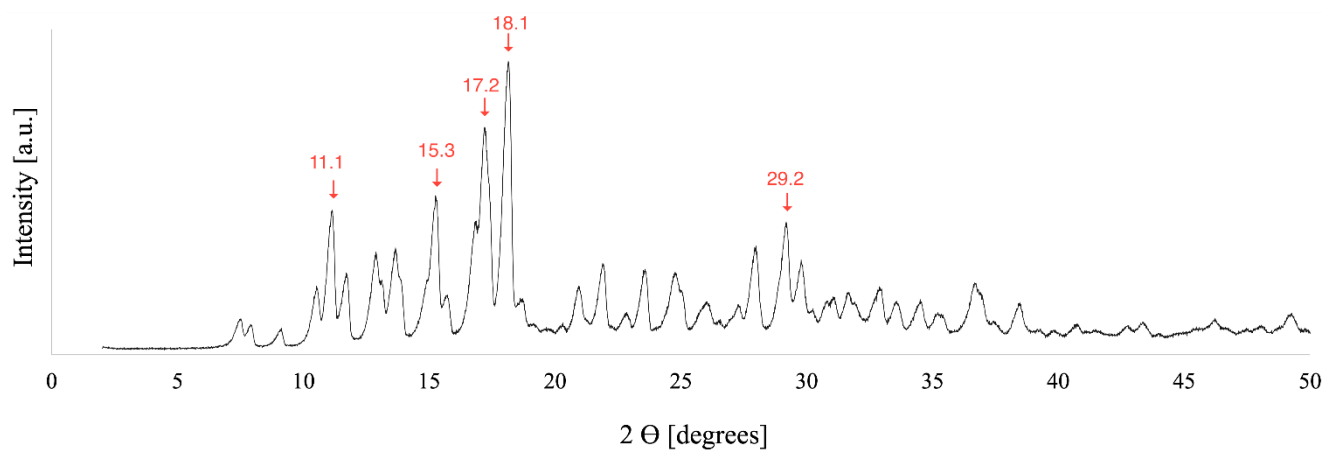




90  
91 **Figure 1 SEM micrograph of the DZIF-L**

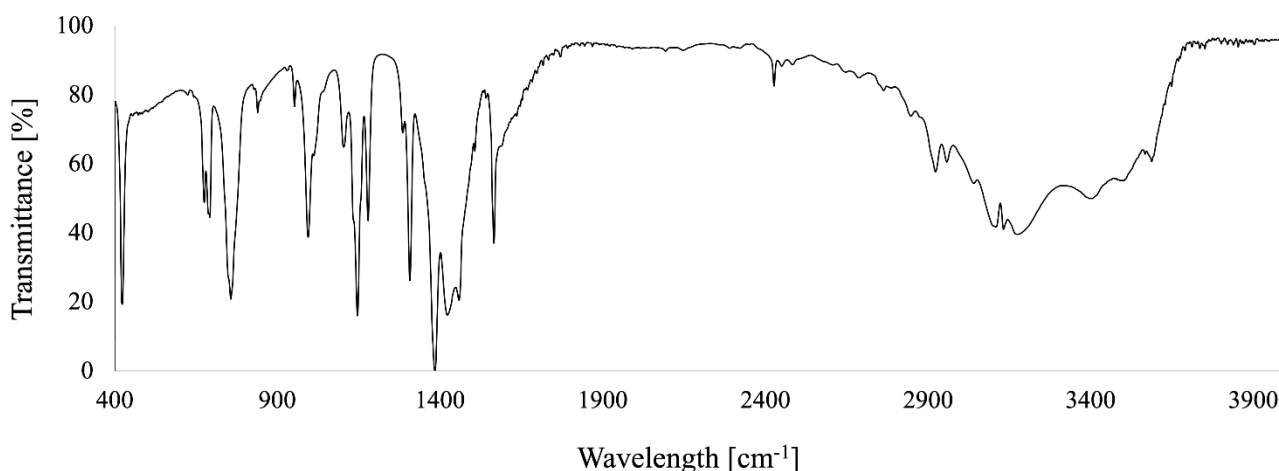
92  
93 The structure of obtained material was analysed using XRD as shown in Figure 2 a). All the diffraction  
94 peak positions agree well with the spectra reported in the literature for ZIF-L with relatively strongest  
95 XRD peaks observed at  $2\theta$  of  $11.1^\circ$ ,  $15.3^\circ$ ,  $17.2^\circ$ ,  $18.1^\circ$ ,  $29.2^\circ$  that stay in agreement with the several  
96 reports from ZIF-L studies [21,22].  
97

a)



b)





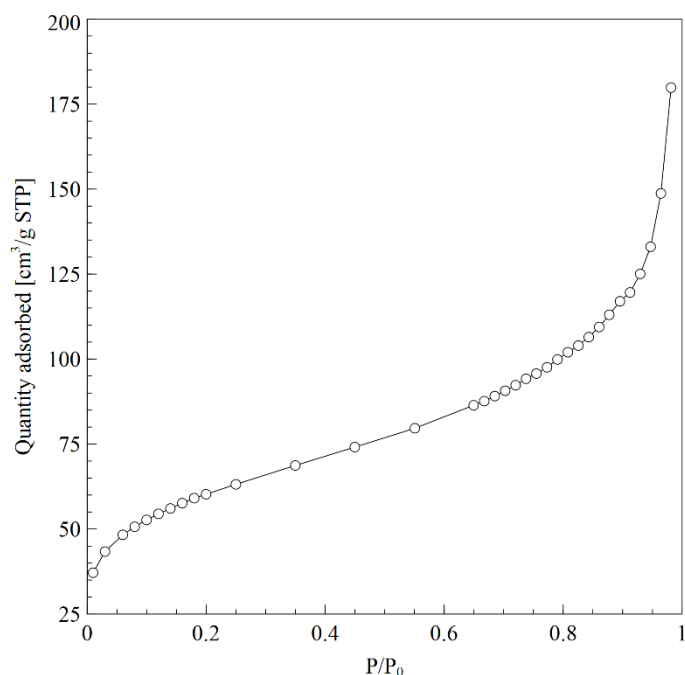
98  
99 **Figure 2 a) XRD pattern and b) FTIR spectrum of DZIF-L**

100  
101 As shown in Figure 2 b) the chemical structure of the DZIF-L was verified by FTIR spectroscopy.

102 Presence of the characteristic peaks for C=N, C-N, CH, and Zn-N was confirmed and agrees well with  
103 ones reported in the literature for ZIF-L.

104 The results indicated the main bands at 422 cm<sup>-1</sup>, 692 cm<sup>-1</sup>, 758 cm<sup>-1</sup>, 995 cm<sup>-1</sup>, 1147 cm<sup>-1</sup>, 1179 cm<sup>-1</sup>,  
105 1307 cm<sup>-1</sup>, 1386 cm<sup>-1</sup>, 1566 cm<sup>-1</sup> and 2426 cm<sup>-1</sup>. The absorption band at 422 cm<sup>-1</sup> represents stretching  
106 of Zn-N. The bands in the spectral region of 600-800 cm<sup>-1</sup> are associated with bending of the imidazole  
107 ring outside the plane, those in 900-1350 region with in-plane bending. Peaks at 1307 cm<sup>-1</sup>, 1179 cm<sup>-1</sup>,  
108 1147cm<sup>-1</sup> and 995 cm<sup>-1</sup> are associated with C-N stretching vibrations. Peaks at 1386 cm<sup>-1</sup> and 758 cm<sup>-1</sup>  
109 can be assigned to CH aromatic bending. The C=N bonds are represented by peak at about 1566 cm<sup>-1</sup>  
110 and are attributed to stretching vibration. The peak at about 2426 cm<sup>-1</sup> is ascribed to N-H...N hydrogen  
111 bond, while the broad band from 2350 to 3700 N-H...N results from the bridging the ZIF-L layers and  
112 the N-H group in methylimidazole [19].

113 For the obtained DZIF-L, N<sub>2</sub> adsorption measurement was performed to determine the specific surface  
114 area, as presented in Figure 4. The isotherm is of type II according to the IUPAC classification, which  
115 indicates the macroporous structure of the material.  
116

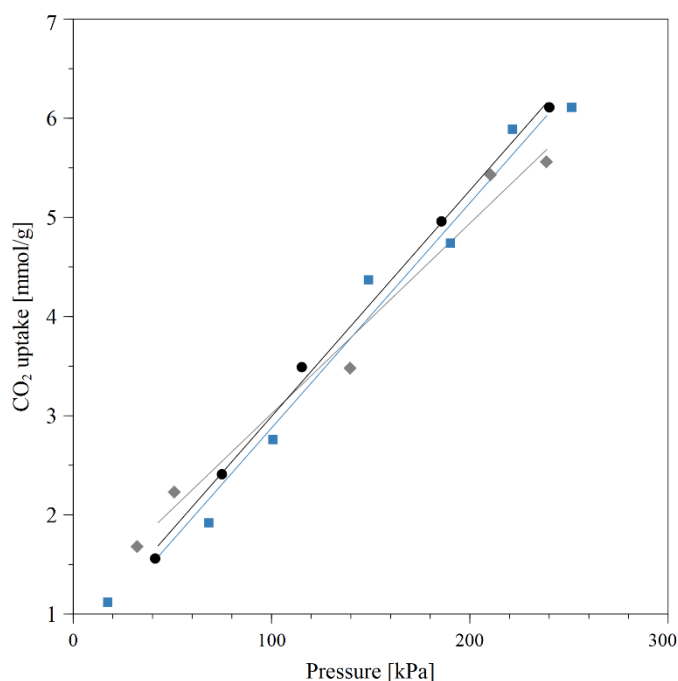


**Figure 3 Exemplary N<sub>2</sub> adsorption isotherm of the DZIF-L**

The specific surface area of the obtained DZIF-L samples was  $223 \pm 10 \text{ m}^2/\text{g}$  and is in a good agreement with the values presented in the literature for individual ZIF-L structures. The area is larger than that observed for leaf-like ZIF-L and lower than that reported for flower-shaped structures and ZIF-8. For single ZIF-L, Chen et al. reported  $161 \text{ m}^2/\text{g}$  and micropore volume of  $0.066 \text{ cm}^3/\text{g}$  [17], by Deacon et al. reported  $93 \text{ m}^2/\text{g}$  for single ZIF-L and  $1651$  for ZIF-8 [23]. Hierarchical structures were proved to have  $304 \text{ m}^2/\text{g}$  [20]. Still, values reported by different authors vary. Low et al. obtained  $18 \text{ m}^2/\text{g}$  and porosity of  $0.02 \text{ cm}^3/\text{g}$  for single ZIF-L [19]. Kahn et al. obtained surface area of  $2.5 \text{ m}^2/\text{g}$  and pore volume of  $0.0034 \text{ cm}^3/\text{g}$  for 2D ZIF-L and  $1472 \text{ m}^2/\text{g}$  and  $0.6067 \text{ cm}^3/\text{g}$  for ZIF-8 [24].

Within this study, for DZIF-L we obtained total pore volume of  $0.188 \pm 0.02 \text{ cm}^3/\text{g}$  at  $P/P_0$  of 0.95, which is compliant with the values reported by other researchers, higher than the values obtained for single ZIF-L and lower than the values reported for ZIF-8.





**Figure 4** Adsorption isotherm of CO<sub>2</sub> by DZIF-L at 298 K (●; ■; ◆ represent experimental points of three experiments)

The adsorption isotherms of CO<sub>2</sub> by the DZIF-L are shown in Figure 4. In the three experiments at 0.1 MPa the CO<sub>2</sub> uptake was 3.02, 3.05 and 2.91 mmol/g, resulting in the average capacity of  $2.99 \pm 0.06$  mmol/g. The capacity of synthesized material is higher than that of any other structure that was so far identified between single ZIF-L and ZIF-8 (Figure 5).

Only Shi et al. obtained comparable capacity of ZIF-8. The authors performed test on CO<sub>2</sub> adsorption capacity of ZIF-8 obtained at different conditions and reported capacity in a range 2.18 – 3.04 g/mmol. The structure of 3.04 mmol/g capacity was synthesized at 358 K [25]. Flower-shaped ZIF-L synthesized by Wang et al. exhibited CO<sub>2</sub> uptake of 1.15 mmol/g at 298 K and 0.1 MPa [18]. Chen et al. reported 0.94 mmol/g uptake for single ZIF-L and 0.68 mmol/g for ZIF-8 [17]. Hierarchical ZIF-L structures, which is between flower-shaped ZIF and double- ZIF-L, obtained by Ding et al. exhibited 1.56 mmol/g uptake with 304 m<sup>2</sup>/g of surface area [20]. Double ZIF-L presents higher CO<sub>2</sub> capacity than single one. This is attributed to the structure, and anti-aggregation properties [18]. The special structure of the particles prevents from stacking together as it is seen in case of leaf-like ZIF. Moreover ZIF-L has a smaller pore size and higher density of metal atoms per unit volume than ZIF-8 [17] and despite the larger surface area of ZIF-8, double ZIF-L has a comparable CO<sub>2</sub> adsorption capacity because of the special shape and cavity. It enables a strong interaction between CO<sub>2</sub> and the 2-methylimidazole originating from the short distance of O atom in CO<sub>2</sub> and H atoms in methylimidazole [17].



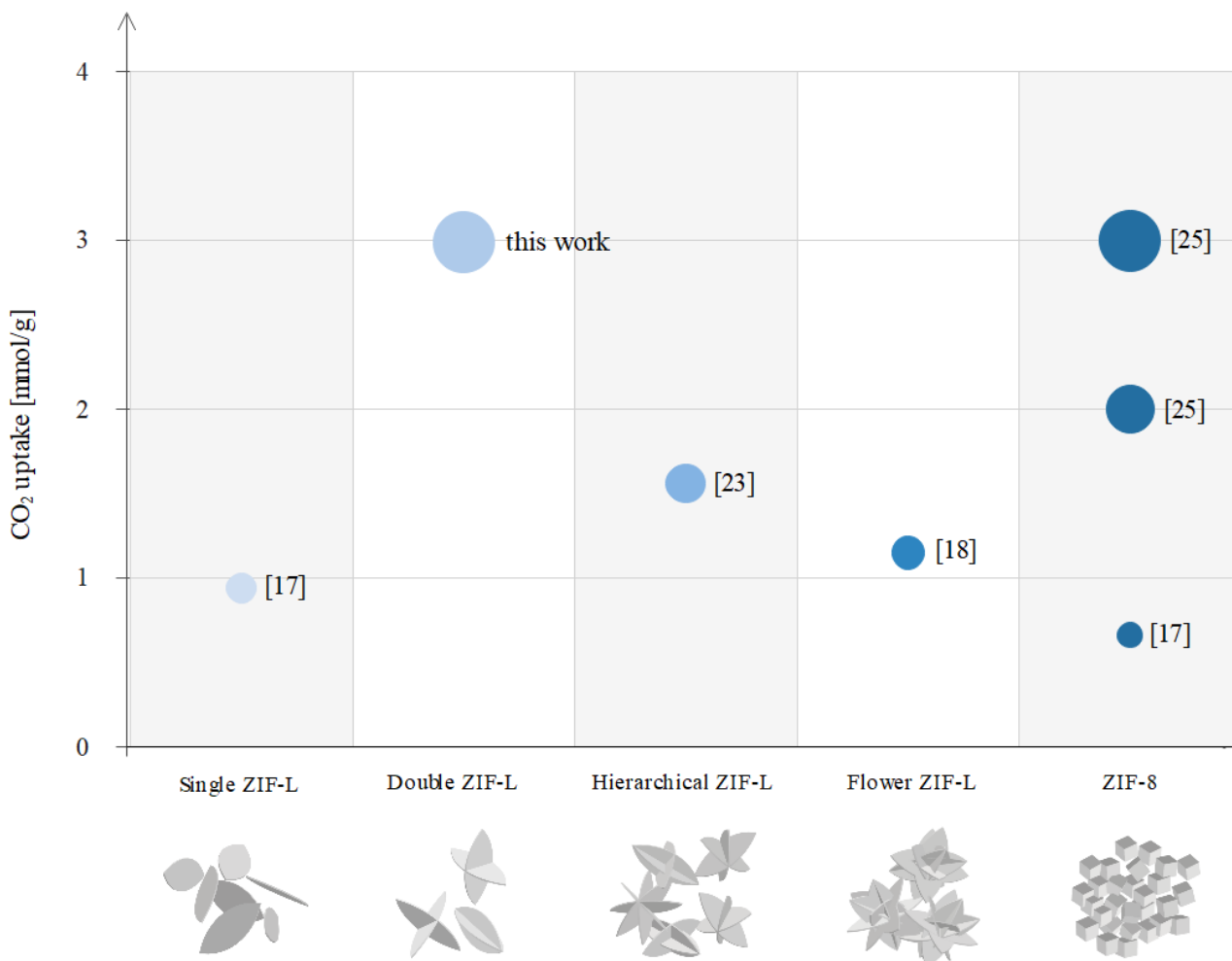


Figure 5 CO<sub>2</sub> uptake of individual ZIF-L structures

#### 4. Conclusions

To our best knowledge it is the first time when the apparent DZIF-L structure was obtained for CO<sub>2</sub> capture. Literature data show that on the transition route from ZIF-L to ZIF-8 there also three other structures that can be distinguished, namely flower-shaped ZIF-L, hierarchical ZIF-L and double ZIF-L obtained within this study. There is only one report in which the authors described ZIF-8 with CO<sub>2</sub> capacity at the same level [25] as capacity of DZIF-L obtained in this research. In general, the specific surface area increases as the ZIF-L transforms to the ZIF-8, but CO<sub>2</sub> capacity is higher for ZIF-L than for ZIF-8 and the intermediate structures present even higher capacity than both ZIF-L and ZIF-8. From all the structures that can be distinguished DZIF-L presented the best performance. Agglomeration can be the reason for lower capacity of single ZIF-L and ZIF-8 as the molecules stick to each other forming a dense layer that limits adsorption capacity. Within the study we succeeded in obtaining the least complex three-dimensional ZIF-L structure, that reduces aggregation and thus enables high adsorption. Since ZIF-Ls are often dedicated to membrane systems, such structure may be capable of forming oriented porous surface which can enhance permeability of resulting membrane. In this regard, we expect that the obtained double ZIF-L structure, which was proven to have remarkable CO<sub>2</sub> capacity in



171 comparison to ZIF-8, hierarchical, flower-shaped and single ZIF-L, has the potential in gas separation  
172 applications.

### 174 **Declaration of Competing Interest**

175 The authors declare that they have no known competing financial interests or personal relationships that  
176 could have appeared to influence the work reported in this paper.

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### 182 **Author contributions**

183 Iwona Cichowska-Kopczyńska conceived and supervised the project, planned the experiments,  
184 performed the sorption experiments, contributed to the data analysis, interpretation and wrote the paper.  
185 Joanna Mioduska synthesized the material, performed analyses including BET analyses, FTIR, XRD,  
186 contributed to the data analysis, interpretation and paper writing. Jakub Karczewski performed the  
187 analyses.

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