



## Research article

## High-performance activation of ozone by sonocavitation for BTEX degradation in water

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## ARTICLE INFO

## Keywords:

Cavitation

Aromatic hydrocarbons

Environmental remediation

Wastewater treatment

Persistent organic pollutants

## ABSTRACT

This work presents a novel advanced oxidation process (AOP) for degradation of emerging organic pollutants – benzene, toluene, ethylbenzene and xylenes (BTEXs) in water. A comparative study was performed for sonocavitation assisted ozonation under 40–120 kHz and 80–200 kHz dual frequency ultrasounds (DFUS). Based on the obtained results, the combination of 40–120 kHz i.e., low-frequency US (LFDUS) with O<sub>3</sub> exhibited excellent oxidation capacity degrading 99.37–99.69% of BTEXs in 40 min, while 86.09–91.76% of BTEX degradation was achieved after 60 min in 80–200 kHz i.e., high-frequency US (HFDUS) combined with O<sub>3</sub>. The synergistic indexes determined using degradation rate constants were found as 7.86 and 2.9 for LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> processes, respectively. The higher extend of BTEX degradation in both processes was observed at pH 6.5 and 10. Among the reactive oxygen species (ROSS), hydroxyl radicals (HO•) were found predominant according to scavenging tests, singlet oxygen also importantly contributed in degradation, while O<sub>2</sub><sup>•-</sup> radicals had a minor contribution. Sulfate (SO<sub>4</sub><sup>2-</sup>) ions demonstrated higher inhibitory effect compared to chloride (Cl<sup>-</sup>) and carbonate (CO<sub>3</sub><sup>2-</sup>) ions in both processes. Degradation pathways of BTEX was proposed based on the intermediates identified using GC-MS technique.

## 1. Introduction

Rapid urbanization and industrialization in the absence of proper environmental management are a one of main sources of the growing emission of volatile organic compounds (VOCs) in the environment. VOCs of anthropogenic nature are considered as the contributor of air pollution indirectly causing stratospheric ozone depletion, tropospheric ozone formation, ground level smog formation as well as climate change (Zhong et al., 2017; Khan and Ghoshal, 2000). Particularly, petroleum refineries, chemical industries, textile manufacturers, paper production and food processing can be classified as the major contributors of air pollution. VOCs represent the large family of carbon-based compounds and depending on the source of emission, they can be halogenated hydrocarbons, alcohols, aldehydes, aromatics, alkenes, ketones, esters, polycyclic hydrocarbons (Kamal et al., 2016; Hashemi et al., 2020; Boczkaj et al., 2016a, 2016b, 2017). These compounds are highly toxic to human and may cause many symptoms and diseases, such as throat,

eye and nose irritation, nasopharyngeal cancer, pulmonary damage, leukemia (Guo et al., 2004; Hazrati et al., 2016). As VOCs threaten the environment and public health, they attracted the global attention and strictly regulated in many countries.

As a natural constituent of a crude oil, gasoline and other petroleum-based products, BTEX enter aquatic environment due to inadequate sewage treatment practices and pipeline leakages (Emmanuel et al., 2023; Vellingiri et al., 2022). Besides, petroleum industry, the origin of BTEX contamination may include a variety of production sites, in which BTEX are utilized, such as synthesis of plastic, rubber, paintings and agriculture (Emmanuel et al., 2023; Wang et al., 1995). The maximum permissible concentration of benzene, toluene, ethylbenzene and xylenes in drinking water were estimated as 5, 1000, 700 and 1000 µg L<sup>-1</sup>, respectively, according to the US Environmental Protection Agency (EPA) (Vellingiri et al., 2022; Carneiro et al., 2014). Introduced into the human body by skin contact, digestive system and inhalation, BTEX are associated with the development of various environmental diseases

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<https://doi.org/10.1016/j.jenvman.2024.121343>

Received 27 February 2024; Received in revised form 10 May 2024; Accepted 30 May 2024

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(Durmusoglu et al., 2010). Thus, low-concentration exposure to benzene is reported to induce confusion, tiredness, nausea as well as development of aplastic anemia, leukemia and solid tumors (Al-Harbi, 2019). Ethylbenzene increased the incidences of serious problems with respiratory system and kidneys. Furthermore, the environmental exposure to toluene and xylenes led to toxic effects on the nervous system, liver and kidneys (Hazrati et al., 2016). Considering the persistence of BTEX to the conventional water treatment technologies, its widespread occurrence and inherent toxicity, the development of efficient and economically viable degradation method is highly desired.

In the past few decades, advanced oxidation processes (AOPs) have been proven to satisfactorily remove a wide list of persistent water pollutants (Li et al., 2024; Liu et al., 2023). AOPs consist of a set of processes which principal operation mechanism is the generation of highly oxidizing radicals. Hydroxyl ( $\text{HO}^\bullet$ ) radicals with oxidation potential of 1.7–2.8  $V_{\text{NHE}}$  are the primary species in many AOPs (e.g., Fenton's process, ozonation at  $\text{pH} > 7$ , perozone, photocatalysis) and react with majority of organic pollutants at a rate constant of  $10^6\text{--}10^9 \text{ M}^{-1} \text{ s}^{-1}$ . The rapid oxidation induced by  $\text{HO}^\bullet$  radicals is non-selective and sufficient to attain a complete mineralization of persistent organic pollutants to  $\text{CO}_2$  and  $\text{H}_2\text{O}$ . Among the AOPs that are utilizing  $\text{HO}^\bullet$  radicals, ultrasound (US) emerged as promising method that can be easily applied in water and sewage treatment of larger operating scales. The formation of  $\text{HO}^\bullet$  radicals under the action of US in liquid is associated with the term of "cold boiling" or cavitation. The cavitation can be defined as the process of formation, growth and subsequent collapse of cavitation bubbles in an extremely short interval of time (Cako et al., 2020; Fedorov et al., 2020). The collapse of cavitation bubbles releases a large magnitude of energy creating high local temperature and pressure above 5000 K and 1000 atm. Such local "hot spots" promote a variety of reactions in liquid which result in generation of  $\text{HO}^\bullet$ ,  $\text{HO}_2^\bullet$ ,  $\text{H}^\bullet$  radicals and  $\text{H}_2\text{O}_2$  (Makino et al., 1982; Adewuyi, 2001; Fitzgerald et al., 2004). Consequently, US-based treatment methods were shown sufficient to degrade *p*-nitrophenol (Pradhan and Gogate, 2010; Sivakumar et al., 2002), dyes (Cako et al., 2020; Sivakumar and Pandit, 2001), polycyclic aromatic hydrocarbons (Psillakis et al., 2004), phenol (Okouchi et al., 1992; Gogate et al., 2003a; Gagol et al., 2020), sulfide ions and organic sulfides (Gagol et al., 2019). The oxidative degradation of pollutants in water by US is attributed to the generation of highly reactive species and facilitated mass transfer in the system by liquid circulation currents and intensive turbulence (Ammar, 2016; Gagol et al., 2018a). Whereas, the utilization of sole US has been reported to rapidly transform organic substrates into short-chain organic acids or  $\text{CO}_2$  and  $\text{H}_2\text{O}$ , it has often been challenging to achieve complete mineralization of persistent organic contaminants. The persistent pollutants can be mineralized or degraded in higher extend by integration of US with other AOPs (Gagol et al., 2018b; Zhou et al., 2008; Sun et al., 2007). The coupled processes exhibit higher degradation efficiency at lower cost compared due to the synergistic effect ensuring a greater efficacy than the cumulative effect of individual processes (Zanias et al., 2020; Nikolaou et al., 2020). Thus, US-assisted ozonation degraded 99.2% of the reactive red X-3B dye in 6 min at the initial concentration of  $100 \text{ mg L}^{-1}$  (Shen et al., 2017). Compared to sole US and  $\text{O}_3$  processes, US/ $\text{O}_3$  system exhibited significantly higher decolorization efficacy with the synergetic factor of 1.42. It was concluded that in the system of conjugated ozonation and sonolysis, acoustic cavitation induced played a crucial role facilitating the mass transfer of  $\text{O}_3$  in aqueous phase. The synergistic index of 1.5 was obtained for the degradation triazophos using the combination of  $\text{O}_3$  and US (Jawale and Gogate, 2018). Particularly, 52.4% of triazophos with the initial concentration of 20 ppm were degraded in 90 min with  $\text{O}_3$ , whereas sole US degraded 43% of triazophos. The higher extend of triazophos degradation by the hybrid technique was attributed to the increased mass transfer giving better utilization of  $\text{O}_3$  and the enhanced amount of generated  $\text{HO}^\bullet$  radicals. Similarly, enhanced generation of reactive radical species, such as  $\text{HO}^\bullet$  radicals and nascent oxygen was observed in US/ $\text{O}_3$  system during the treatment of the pharmaceutical

industry effluent (Chandak et al., 2020). In this case, the COD reduction above 30% was attained after 120 min. To conclude, the synergistic effect in US/ $\text{O}_3$  processes is attributed to acoustic cavitation, which is responsible for the effective decomposition of  $\text{O}_3$  to yield reactive radical species. Additionally, microcirculations and turbulence in the bulk liquid induced by US waves provide an effective dispersion of  $\text{O}_3$  thereby reducing the mass transfer resistance. Nevertheless, the sonochemical transformations (e.g., generation of  $\text{HO}^\bullet$  radicals) in single-frequency US are limited due to non-uniform volumetric energy dissipation in the treated liquid due to directional sensitivity of the US field (Moholkar, 2009). The utilization of dual or multiple frequency US was explored to overcome the disadvantage associated with the directional sensitivity through the production of strong interference pattern in the reactor. The effect of dual-frequency US was studied in a diverse range of applications, such as sonoluminescence (Lu et al., 2003; Lee and Oh, 2011; Ciuti et al., 2000), KI oxidation (Ebrahimi et al., 2016; Feng et al., 2002), leaching of valuable metals (Swamy and Narayana, 2001) and degradation of water pollutants (Sivakumar et al., 2002; Hua et al., 1995; Gogate et al., 2003b; Wang et al., 2006; Zhao et al., 2010).

Among AOPs combined with dual-frequency US, ozonation under dual-frequency US has been demonstrated as an effective method for water treatment application. Thus, the combination of 20 kHz–40 kHz dual-frequency US with  $\text{O}_3$  was shown to degrade 83.8% of nitrobenzene in 60 min representing an increment of 30.6% compared the cumulative effect of sole US and  $\text{O}_3$  (Zhao et al., 2010). Up till now, the range of selected dual frequencies applied in US/ $\text{O}_3$  was narrow (i.e., 20 kHz–28 kHz and 20 kHz–40 kHz). Moreover, the effect on dual-frequency US on BTEX ozonation has not been reported. Herein, we extend the investigation on sonochemical transformations of  $\text{O}_3$  occurring over acoustic cavitation induced by dual-frequency US, comparing the effect 40 kHz–120 kHz and 80 kHz–200 kHz DFUS on BTEX degradation. The outcomes of this study contribute to a more comprehensive understanding of the role of acoustic cavitation in AOPs, allowing for the optimization of operating parameters in order to achieve the highest sonochemical efficiency in US-assisted AOPs. The study concerns the radical mediated process potentially employed in water treatment industry, therefore, several operating aspects critical in practical application, such as pH, the effect of radical scavengers and co-existing anions were studied. The mechanism of BTEX degradation was proposed based on the intermediates identified by gas chromatography coupled with mass spectrometry (GC-MS). The obtained results were discussed in order to elucidate the role of combined frequencies in synergistic mechanism of US/ $\text{O}_3$  for the degradation of BTEX in water.

## 2. Materials and methods

### 2.1. Materials

Benzene (99.7%), toluene (pure), were purchased from Chempur (Poland) and POCH (Poland), respectively. Ethylbenzene (99%) and *o*-xylene ( $\geq 98\%$ ) were purchased from Merck KGaA (Germany) and Merck Schuhard OHG (Germany), respectively. Sulfuric acid (pure,  $\geq 98\%$ ) and sodium hydroxide (pure,  $\geq 85\%$ ) were supplied from POCH (Poland). Potassium iodide (pure, p. a.) and sodium thiosulfate pentahydrate (acs pure p. a.) were purchased from POCH (Poland). Methanol (pure, 95%) used for quenching experiments was obtained from POCH (Poland). Sodium azide (pure p. a., 99.0%) was purchased from Chempur (Poland), while 1,4-benzoquinone (99%) was obtained from Acros Organics (Belgium). Sodium chloride (pure) was purchased from POCH (Poland), sodium carbonate (99.8%) and sodium sulfate (99.0%) were supplied from Chempur (Poland). All solutions were prepared using ultrapure quality water ( $18.2 \text{ M}\Omega\text{cm}^{-1}$ ) from Millipore® system (Direct-Q UV-R model). All chemical and solvents were used as received.

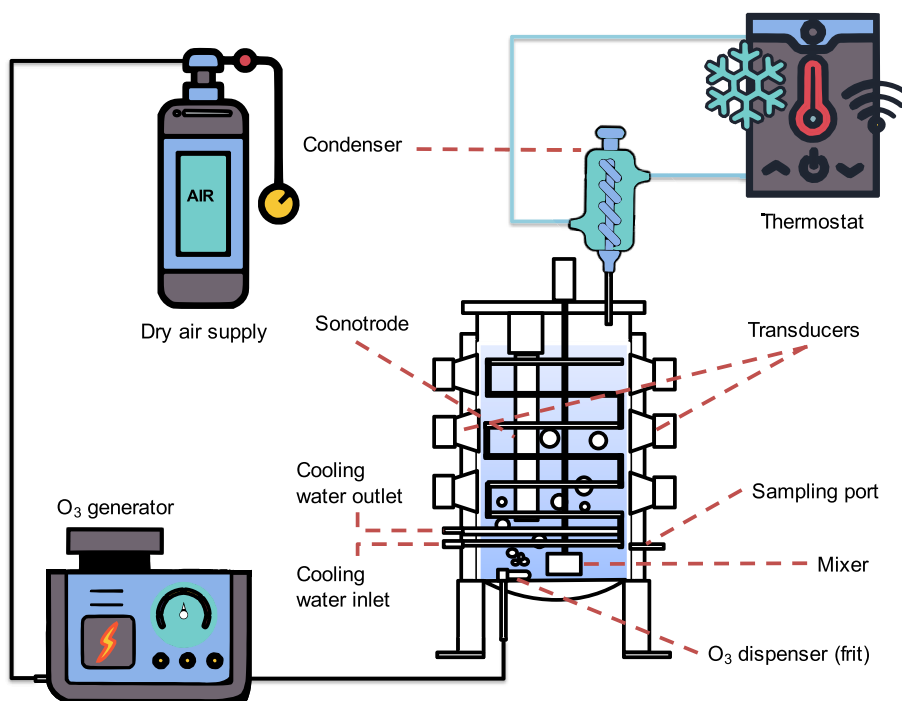


Fig. 1. Scheme of the experimental setup for BTEX ozonation under dual-frequency US.

Table 1

Pseudo-first-order kinetic model constant rates of BTEX degradation in LFDUS and HFDUS systems.

Process	Frequency kHz	Benzene $k, \text{min}^{-1}$	Toluene $k, \text{min}^{-1}$	Ethylbenzene $k, \text{min}^{-1}$	<i>o</i> -Xylene $k, \text{min}^{-1}$
US	40	0.0026	0.0025	0.0024	0.0021
	80	0.0039	0.0037	0.0034	0.0034
	120	0.0034	0.0030	0.0028	0.0027
	200	0.0027	0.0027	0.0030	0.0025
LFDUS	40–120	0.0064	0.0062	0.0059	0.0058
HFDUS	80–200	0.0060	0.0059	0.0061	0.0058

## 2.2. Experimental procedure

Ozonation experiments were performed in a custom-designed sono-reactor manufactured by Beijing Yongda Ultrasonic CO., LTD (China). The experimental setup is presented in Fig. 1. The reactor was equipped with a sonotrode, transducers, temperature sensor, mixer and cooling system. The transducers mounted on the walls of the reactor were capable to produce ultrasonic waves with a frequency of 120 kHz and 200 kHz, respectively. A sonotrode attached on the removable cover of the reactor had an operating frequency of 120 kHz and 200 kHz, respectively. A combination of 40 kHz sonotrode and 120 kHz transducers were utilized for low-frequency sonication experiments, while 80 kHz sonotrode and 200 kHz transducers – for high-frequency sonication mode. In a typical experiment, 3.8 L of model solution containing 50 ppm of BTEX (i.e. 50 mg/kg of each compound (benzene, toluene,

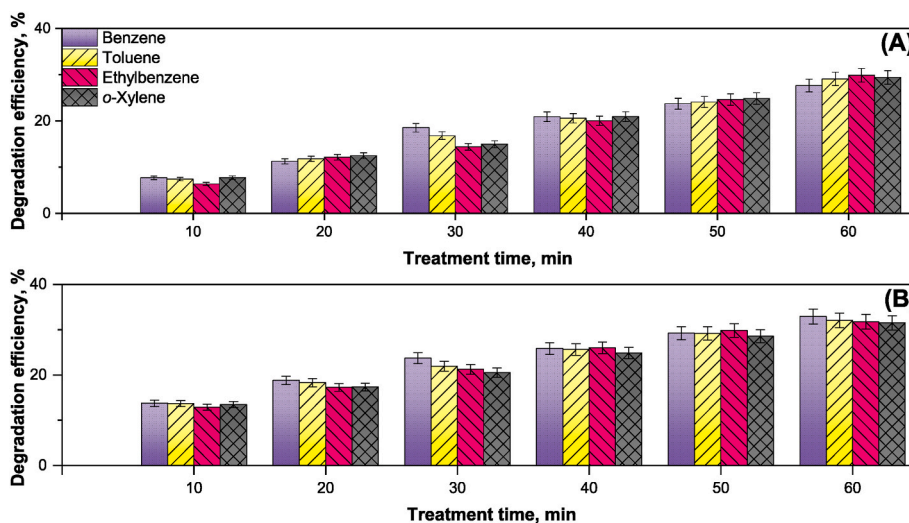


Fig. 2. Degradation efficiency of BTEX in (a) LFDUS, (b) HFDUS; [BTEX]<sub>0</sub>: 50 ppm (v/v), pH 6.5, T = 20 ± 2.5 °C, US power input 600 W, US frequencies: 40/120 kHz and 80/200 kHz for LFDUS and HFDUS, respectively.

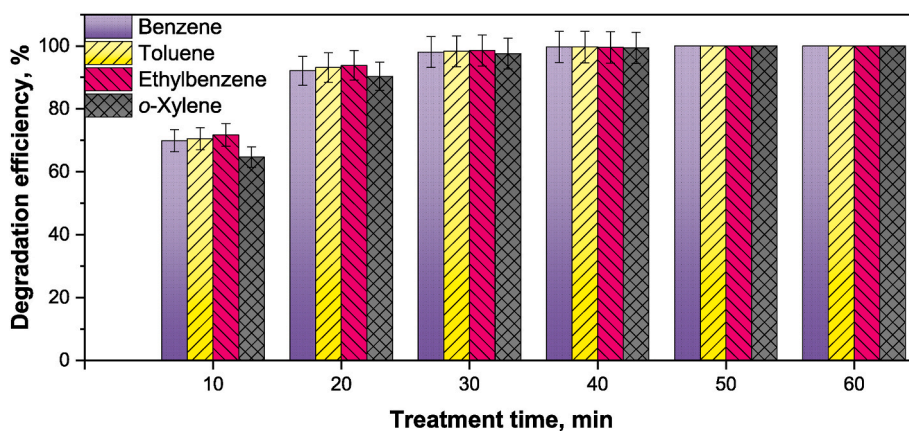


Fig. 3. Degradation efficiency of BTEX in LFDUS/O<sub>3</sub>; [BTEX]<sub>0</sub>: 50 ppm (v/v), pH 6.5, T = 20 ± 2.5 °C, O<sub>3</sub> flow rate 0.5 L min<sup>-1</sup>, US power input 600 W, US frequencies: 40/120 kHz.

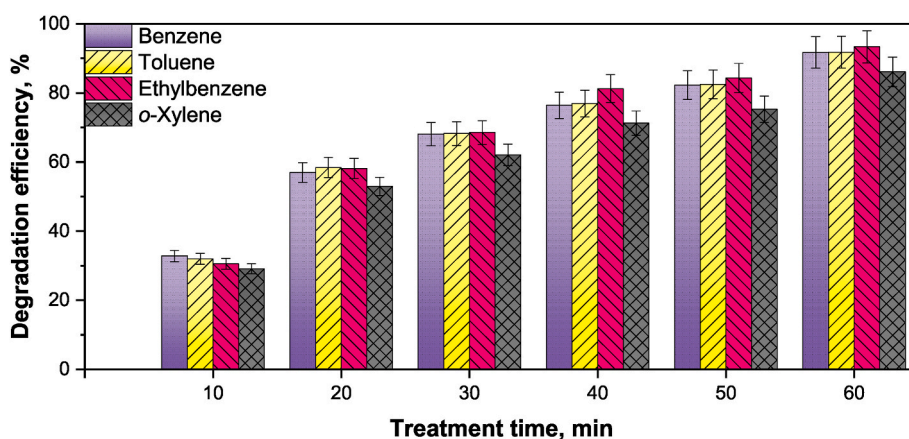


Fig. 4. Degradation efficiency of BTEX in HFDUS/O<sub>3</sub>; [BTEX]<sub>0</sub>: 50 ppm (v/v), pH 6.5, T = 20 ± 2.5 °C, O<sub>3</sub> flow rate 0.5 L min<sup>-1</sup>, US power input 600 W, US frequencies: 80/200 kHz.

Table 2

Pseudo-first-order kinetic model constant rates of BTEX degradation in O<sub>3</sub>-assisted processes.

Process	Frequency kHz	Benzene k, min <sup>-1</sup>	Toluene k, min <sup>-1</sup>	Ethylbenzene k, min <sup>-1</sup>	o-Xylene k, min <sup>-1</sup>
Sole O <sub>3</sub>	–	0.0055	0.0067	0.0081	0.0067
US/O <sub>3</sub>	40	0.0094	0.0093	0.0089	0.0070
	80	0.0144	0.0144	0.0151	0.0119
	120	0.0143	0.0152	0.0172	0.0131
	200	0.0179	0.0182	0.0200	0.0141
LFDUS/O <sub>3</sub>	40/120	0.1431	0.1419	0.1387	0.1282
HFDUS/O <sub>3</sub>	80/200	0.0384	0.0385	0.0425	0.0304

ethylbenzene and *o*-xylene respectively), was placed in sono-reactor and treated for 60 min at 20 ± 2 °C. A Tytan 32 ozone generator (Erem) was used for ozonation and was connected to sono-reactor by PTFE tubes. Ozone was fed using dry air as a carrier gas at a flowrate of 0.5 L min<sup>-1</sup> through a porous frit at the bottom of sono-reactor to provide better distribution. Tap water was flowed continuously through stainless steel cooling coil placed in the reaction chamber to maintain constant temperature. A glass condenser was connected to ozone outlet to prevent BTEX evaporation. The condenser was connected to refrigerated circulator bath HAAKE DC30 K<sup>20</sup> (Thermo Scientific, Germany) filled with methanol to maintain -5 °C. Aliquots of samples (20 mL) were collected at certain time interval for analysis. All the experiments were performed in duplicate.

### 2.3. Analytical methods

Sample preparation for GC-FID analysis was conducted by dispersive liquid-liquid microextraction (DLLME) using dichloromethane (POCH, Poland) as an extraction solvent and acetone (POCH, Poland) as dispersive agent. The molar ratio between dichloromethane and acetone was taken as 50:40, respectively. The quantitative analysis of BTEX content was proceeded based on the internal standard method using 4-chlorophenol (POCH, Poland) as internal standard. The detailed description of DLLME procedure is provided in previously reported studies (Makoś et al., 2018). A Clarus 500 (PerkinElmer, USA) gas chromatograph equipped with flame ionization detector (GC-FID) was used for quantitative analysis of BTEX. A capillary column (60 m × 0.32 mm ID, 1.8 μm DB624, Agilent, USA) was used for separation of analytes. Operating conditions of GC-FID were as follows: oven temperature 50 °C (5 min) ramped at 10 °C min<sup>-1</sup> to 275 °C (20 min), 2 μL of the extract was injected to the GC-FID from each sample twice. The temperature of injection port and detector were 300 °C and 275 °C, respectively. The hydrogen and air flow were supplied in flow rates of 40 and 430 mL min<sup>-1</sup>, respectively.

The intermediates of BTEX degradation were identified by GCMSQP2010SE (Shimadzu, Japan) gas chromatograph coupled to a mass spectrometer (GC-MS). The separation of analytes was conducted using a capillary column (100 m × 0.2 mm ID, 0.1 μm DHA, Restek, USA). The GC column operated in a temperature programmed mode with initial temperature of 40 °C (isothermal for 5 min) which ramped at 5 °C min<sup>-1</sup> to 220 °C. A PGX500 hydrogen generator (PerkinElmer,

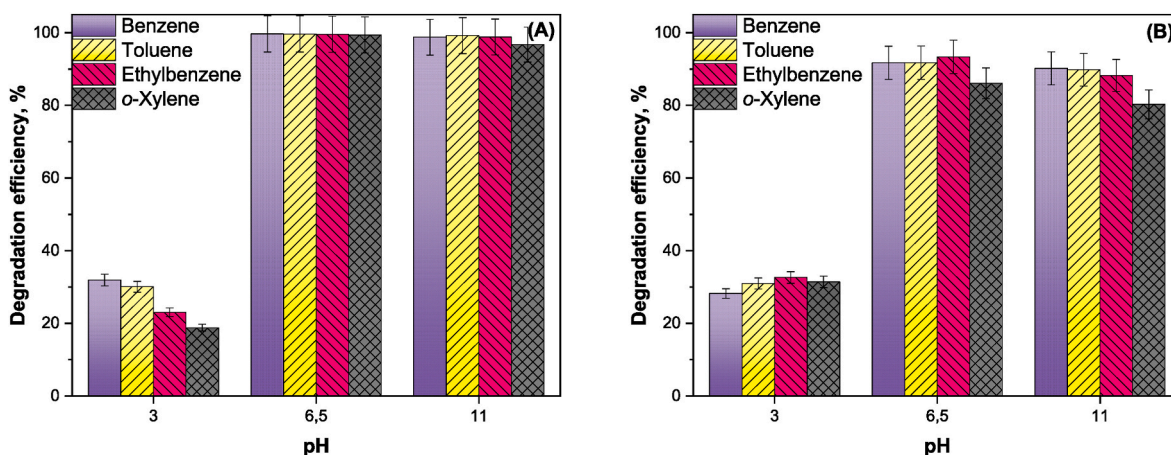


Fig. 5. Effect of pH on BTEX degradation in (a) LFDUS/O<sub>3</sub> and (b) HFDUS/O<sub>3</sub> [BTEX]<sub>0</sub>: 50 ppm (v/v), pH 6.5, T = 20 ± 2.5 °C, Treatment time: 40 min for LFDUS/O<sub>3</sub> and 60 min for HFDUS/O<sub>3</sub>, O<sub>3</sub> flow rate 0.5 L min<sup>-1</sup>, US: 600 W, 40/120 kHz (LFDUS) and 80/200 kHz (HFDUS).

Table 3

Pseudo-first-order kinetic model parameters of BTEX degradation in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> at various pH.

pH	Process	Benzene	Toluene	Ethylbenzene	o-Xylene
		k, min <sup>-1</sup>	k, min <sup>-1</sup>	k, min <sup>-1</sup>	k, min <sup>-1</sup>
3	LFDUS/O <sub>3</sub>	0.0092	0.0091	0.0080	0.0063
	HFDUS/O <sub>3</sub>	0.0059	0.0062	0.0062	0.0057
6.5	LFDUS/O <sub>3</sub>	0.1431	0.1419	0.1387	0.1282
	HFDUS/O <sub>3</sub>	0.0384	0.0385	0.0425	0.0304
11	LFDUS/O <sub>3</sub>	0.1123	0.1233	0.1190	0.0877
	HFDUS/O <sub>3</sub>	0.0398	0.0393	0.0371	0.0274

USA) was used to supply hydrogen at a flow rate of 1 mL min<sup>-1</sup>, the temperature in GC-MS transfer line and injection port were set at 310 °C and 300 °C, respectively. A mass spectra were recorded in the range of 34–220 m/z using an electron impact ionization mode (EI 70 eV). The ionization source temperature was set at 200 °C.

The concentration of gaseous O<sub>3</sub> in dry air stream was determined by iodometric titration method. For this, the feed of O<sub>3</sub> was bubbled through two connected gas washing bottles filled with 500 mL of 2% KI (w/w). The solutions were acidified to pH 3 by adding 2 N H<sub>2</sub>SO<sub>4</sub> and the compresses air stream containing O<sub>3</sub> was sparged through KI solution using sintered glass disc located in the bottom half of bottles. A standardized 0.01 mol L<sup>-1</sup> Na<sub>2</sub>S<sub>2</sub>O<sub>3</sub> solution was used as a titrant in presence of 5% (w/v) starch indicator. The dose of applied O<sub>3</sub> was determined as 2.1 g h<sup>-1</sup> and the molar ratio of BTEX to O<sub>3</sub> (*r*<sub>ox</sub>) was 6.25.

### 3. Results and discussion

#### 3.1. Degradation of BTEX by single and dual frequency US

Prior to evaluating the effect of dual-frequency US (DFUS), the effect of single US of different frequency on BTEX degradation was investigated. As shown in Fig. S1 (Supplementary data), 19.87, 18.04, 15.48 and 15.82% of benzene, toluene, ethylbenzene and o-xylene were degraded in 60 min by 80 kHz US. The rate constants of BTEX degradation observed in US-80 kHz were the highest among the studied frequencies as presented in Table 1. Next, the effect of dual frequencies was studied. As illustrated in Fig. 2a, the combination of 40 and 120 kHz (LFDUS) increased the degradation efficiency of BTEX to 28.6–32.0% after 60 min of treatment. Likewise, the combination of 80 kHz sonotrode and 200 kHz transducers (HFDUS) degraded 31.5–32.9% of BTEXs in 60 min as shown in Fig. 2b. The degradation extent of BTEXs in both cases was similar and the highest degradation was observed for benzene, while o-xylene was the least degraded. This observation probably

indicates that the non-selective radical-induced oxidation at gas-liquid phase and bulk liquid were the main degradation sites as benzene, toluene and ethylbenzene with lower log*K*<sub>ow</sub> were degraded in higher extend. As a part of sonochemical processes taking place in the liquid, the oxidative degradation of pollutants relates to acoustic cavitation induced by US irradiation. The localized extreme conditions created due to the adiabatic collapse of cavitation bubbles are sufficient to promote a thermal decomposition of pollutants and water. The disassociation of water occurs in both gaseous and gas-liquid phases yielding HO• and H• radicals along with secondary HO<sub>2</sub>• radicals in air-saturated liquids (Eqs. 1, 2). In the absence of scavengers, these radicals undergo recombination with formation of H<sub>2</sub>O<sub>2</sub>, H<sub>2</sub> and H<sub>2</sub>O as shown in Eqs. (3)–(6) (Yusof et al., 2016; Beckett and Hua, 2000). Although, HO• radicals and H<sub>2</sub>O<sub>2</sub> are powerful oxidants, the degradation efficiency of BTEX in the studied single-frequency US is low due to the limited generation of ROSS.



The synergistic index values ( $\xi$ ) determined according to Eq. (7) were found as 1.13 and 0.94 for LFDUS and HFDUS, respectively. The synergistic effect observed in LFDUS implies that the application of DFUS increases the sonochemical yield of ROSS by acoustic cavitation and consistent with previously reported statements. In particular, it has been suggested that the cavitation bubbles affected by DFUS possess high collapse pressure and grow to the maximum size faster (Tatake and Pandit, 2002; Manickam et al., 2014). Therefore, it can be suggested that the higher collapse pressure achieved in LFDUS promoted the pyrolytic decomposition of BTEX, while the short collapse time intensified the yield of HO• radicals.

$$\xi = \frac{k_{a+b}}{k_a + k_b} \quad \text{Eq. 7}$$

where  $k_{a+b}$  is the rate constant of the combined process, while  $k_a$  and  $k_b$  – rate constants of sole processes.

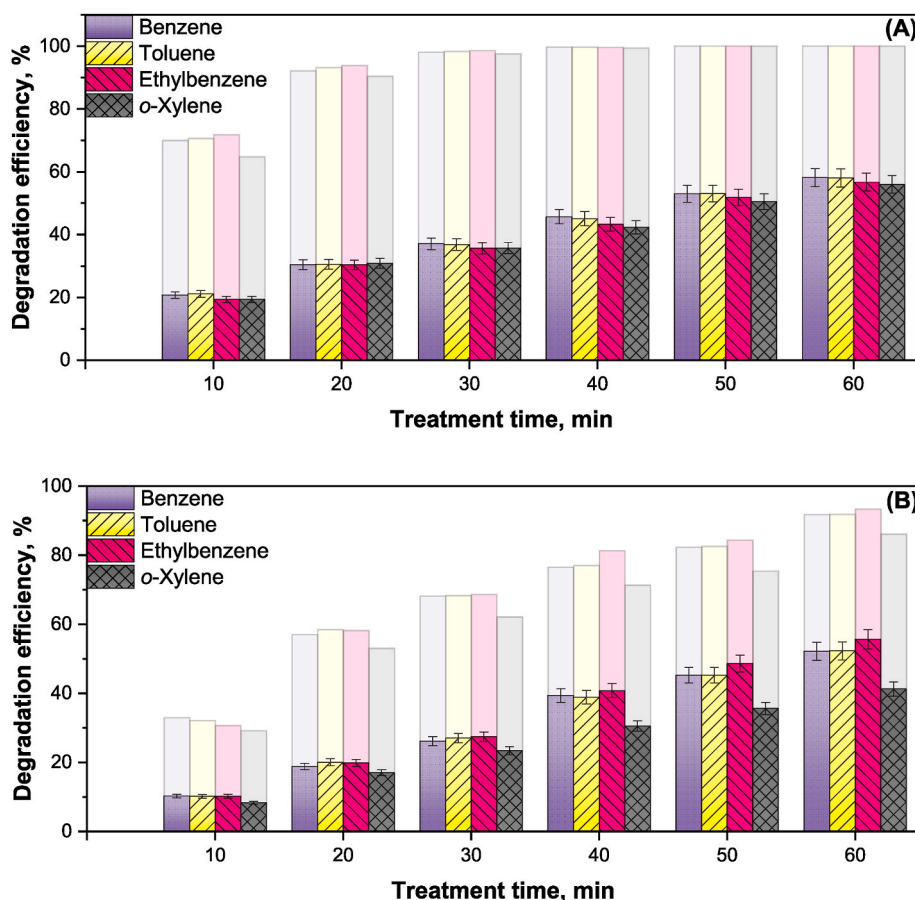


Fig. 6. Effect of MeOH on BTEX degradation in (a) LFDUS/O<sub>3</sub> and (b) HFDUS/O<sub>3</sub>; [BTEX]<sub>0</sub>: 50 ppm (v/v), [O<sub>3</sub>]: [MeOH] = 1:10, pH 6.5, T = 20 ± 2.5 °C, O<sub>3</sub> flow rate 0.5 L min<sup>-1</sup>, US: 600 W, 40/120 kHz (LFDUS) and 80/200 kHz (HFDUS). Shaded data - corresponding processes without additives.

Table 4

Pseudo-first-order kinetic model parameters of BTEX degradation in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> in the presence of scavengers.

Scavenger	Process	Benzene <i>k</i> , min <sup>-1</sup>	Toluene <i>k</i> , min <sup>-1</sup>	Ethylbenzene <i>k</i> , min <sup>-1</sup>	<i>o</i> -Xylene <i>k</i> , min <sup>-1</sup>
MeOH	LFDUS/O <sub>3</sub>	0.0139	0.0138	0.0134	0.0129
	HFDUS/O <sub>3</sub>	0.0125	0.0124	0.0138	0.0089
<i>p</i> -BQ	LFDUS/O <sub>3</sub>	0.0165	0.0181	0.0201	0.0166
	HFDUS/O <sub>3</sub>	0.0210	0.0216	0.0237	0.0175
NaN <sub>3</sub>	LFDUS/O <sub>3</sub>	0.0052	0.0054	0.0056	0.0040
	HFDUS/O <sub>3</sub>	0.0056	0.0056	0.0055	0.0055

### 3.2. Dual-frequency US combined with ozone

The hybrid process of US/O<sub>3</sub> is a technically simple and efficient AOP capable to ensure a rapid degradation of recalcitrant pollutants due to the synergistic effect between the coupled techniques. In order to assess the effectiveness of single-frequency US/O<sub>3</sub>, the effect of sole ozonation and US at different frequencies coupled with O<sub>3</sub> were conducted and evaluated towards the degradation of BTEXs. Fig. 2S depicts the degradation efficiency of BTEX in the process of O<sub>3</sub> alone. In this process, 26.81–40.71% of BTEXs were degraded in 60 min. Upon the combination of ozonation with single US of different frequency (i.e., 40, 80, 120, 200 kHz), the degradation efficiency of BTEX was evidently increased as illustrated in Fig. 3S. Specifically, the degradation rate of BTEXs was increased to 57.21–67.45% after 60 min with the combination of US-200 kHz with O<sub>3</sub>. Although O<sub>3</sub> is a powerful oxidant with an oxidation potential of 2.08 V, the ozonation process of BTEX is limited due to the low direct reactivity and poor gas-liquid mass transfer rate

(Gagol et al., 2018c; Bein et al., 2023). In US/O<sub>3</sub> processes, the rate of O<sub>3</sub> mass transfer is accelerated by the mechanical effects of US, such as turbulences and microcirculations providing greater mixing. Besides, O<sub>3</sub> undergoes thermal decomposition in the gaseous phase of cavitation bubbles yielding HO<sup>•</sup> radicals via Eqs. 8, 9. The formation of HO<sup>•</sup> radicals from H<sub>2</sub>O is facilitated due the presence of highly reactive nascent oxygen atoms (Khan et al., 2023), which can also react with BTEXs. Consequently, these conversions contribute to the reduction of the dissolved O<sub>3</sub> concentration below the saturation value and promote the continuous diffusion of O<sub>3</sub> into the liquid. As a result, the combination of US and O<sub>3</sub> exhibited higher degradation efficiency of BTEX with respect to sole O<sub>3</sub>.



in order to demonstrate the effect of dual-frequency US on BTEX degradation by O<sub>3</sub>, the ozonation was performed under the sonication of 40–120 kHz (LFDUS) and 80–200 kHz (HFDUS). As depicted in Fig. 3, the combined process of ozonation and LFDUS degraded 99.37–99.69% of BTEXs in 40 min. In contrast, the simultaneous operation of ozonation and HFDUS (Fig. 4) reached 86.09–91.76% of BTEX degradation after 60 min. The synergistic indexes determined according Eq. (7) were 7.86 and 2.9 for LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub>, respectively. These results indicated that the ozonation of BTEX in water can be significantly enhanced by application of dual-frequency US as the efficiency of both combined processes exceeded the cumulative effect of sole O<sub>3</sub> and DFUS.

The effectiveness of ozonation under US is generally attributed to the enhanced generation of HO<sup>•</sup> radicals and reduced mass transfer

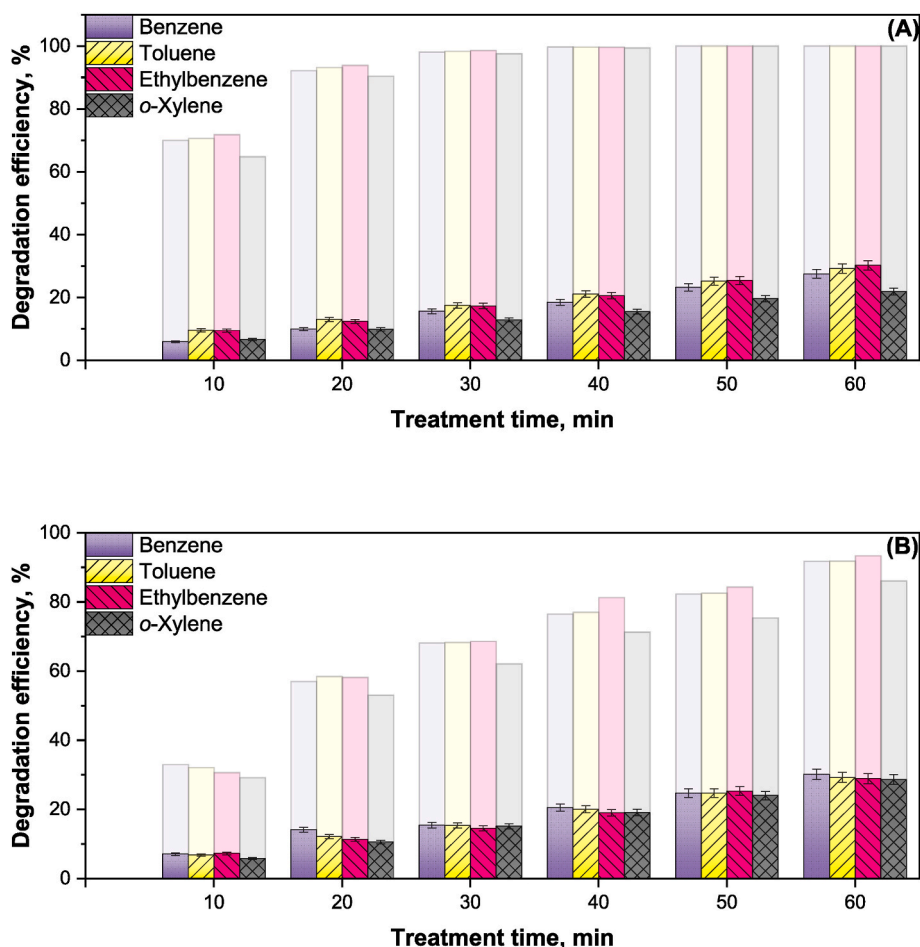


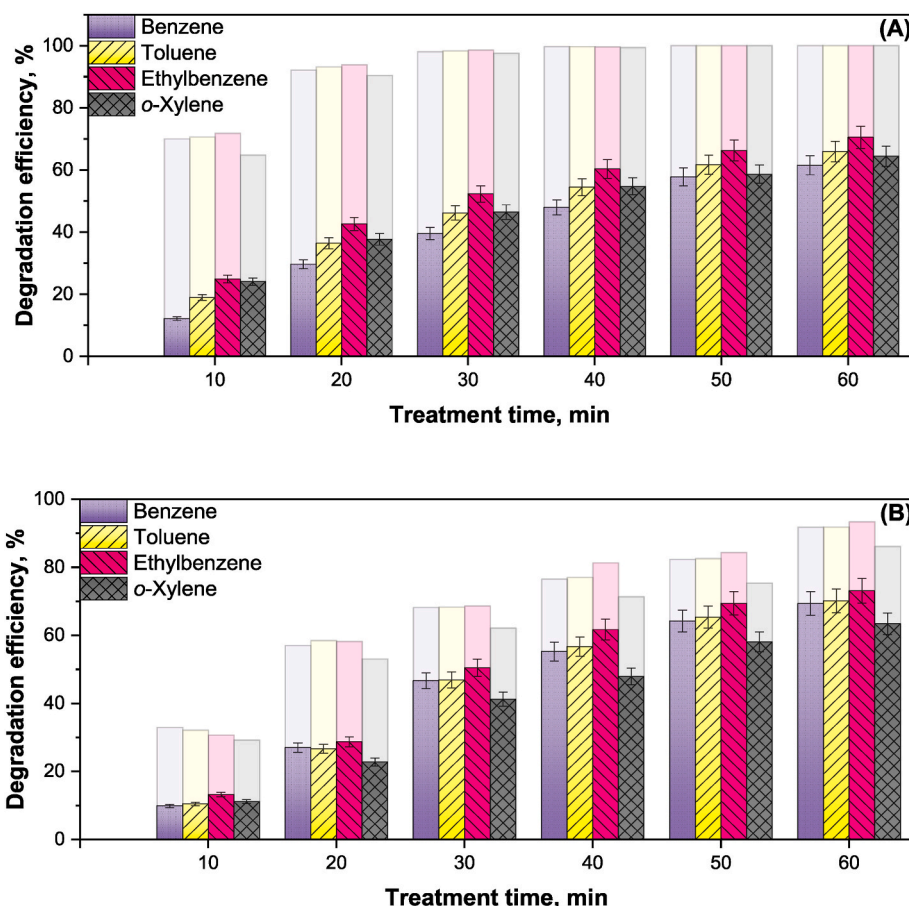
Fig. 7. Effect of Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub> on BTEX degradation in (a) LFDUS/O<sub>3</sub> and (b) HFDUS/O<sub>3</sub>; [BTEX]<sub>0</sub>: 50 ppm (v/v), [O<sub>3</sub>]: [Na<sub>2</sub>S<sub>2</sub>O<sub>8</sub>] = 1:10, pH 6.5, T = 20 ± 2.5 °C, O<sub>3</sub> flow rate 0.5 L min<sup>-1</sup>, US: 600 W, 40/120 kHz (LFDUS) and 80/200 kHz (HFDUS). Shadowed data - corresponding processes without additives.

resistance. The enhanced degradation of pollutants in US/O<sub>3</sub> process is mainly caused by the accelerated generation of ROSs due to O<sub>3</sub> decomposition induced by collapse of cavitation bubbles (Chandak et al., 2020; Weavers et al., 1998; Ghanbari et al., 2020). The energy emitted during the collapse of cavitation bubbles, in turn, creates localized extreme conditions, so-called “hot spots”, whereat O<sub>3</sub> undergo thermal decomposition (Gagol et al., 2018b, 2020). In such scenario, benzene, toluene, ethylbenzene, o-xylene with partition coefficient (logK<sub>ow</sub>) of 2.13, 2.73, 3.15 and 3.12, respectively, tend to diffuse to the interior and interfacial zones of the cavitation bubble. Inside the cavitating bubble, BTEXs are readily degraded via pyrolysis and oxidative degradation by a variety of generated ROSs at the interfacial zone.

Upon DFUS excitation, the steady-state oscillation of cavitation bubbles is disrupted and the evolution dynamics of cavitation bubbles is complex exhibiting unstable oscillation, which causes accelerated collapse of cavities (Ye et al., 2019). Importantly, the maximum radius and collapse pressure of cavitation bubbles in DFUS is significantly higher than that of obtained using single-frequency US at the same US power (Ye et al., 2019). Hence, the utilization of DFUS can disturb the treated solution more strongly and characterized by a high energy dissipation rate and cavitation yield compared to single-frequency US (Tatake and Pandit, 2002; Matafonova and Batoev, 2020; Zhang et al., 2017). Therefore, the formation of ROSs due to O<sub>3</sub> decomposition was increased in LDFUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> resulting in high degradation efficiency of BTEX. As listed in Table 2, the degradation rate constant values of BTEX in LFDUS/O<sub>3</sub> were significantly higher than that of US/O<sub>3</sub>-40 kHz and US/O<sub>3</sub>-120 kHz. Since DFUS-assisted processes are electric-energy-intensive, the electric energy per order (E<sub>EO</sub>) – electric

energy required to degrade 90% of 1 m<sup>3</sup>, 100 ppm BTEX solution were estimated. Taking into account the operating power of US reactor (0.3 kW for single-frequency US and 0.6 kW for dual-frequency) and O<sub>3</sub> generator (0.38 kW), the E<sub>EO</sub> of LFDUS/O<sub>3</sub> was to 71.78 kW h m<sup>-3</sup> order<sup>-1</sup>, while single frequency US/O<sub>3</sub> processes at 40 and 120 kHz required 794.40 and 459.63 kW h m<sup>-3</sup> order<sup>-1</sup>, respectively. If the cost of energy is 0.17 USD per kWh for industrial customers in Poland, the treatment cost of BTEX in LFDUS/O<sub>3</sub> from electrical cost will be 7.9 USD m<sup>-3</sup>. These observations highlight the superiority of DFUS over the single-frequency US in the ozonation of BTEX in water.

Taking into account that the decreased cavitation threshold is associated with a decrease in US frequency, the effect of the low frequency on cavitation events in DFUS is crucial (Matafonova and Batoev, 2020; Thanh Nguyen et al., 2017). It has been proposed that along with the generation of new cavitation nuclei, the low frequency US stimulates the diminishing of bubble interactions by the destruction of bubble clusters driven by high frequency US (Ciuti et al., 2000). Consequently, the application of low frequency US in DFUS increases the number of cavitation bubbles undergoing violent collapse and, thus, intensifies the cavitation events. With utilization of one low frequency US, high cavitation yields in DFUS were verified by measuring KI oxidation (Ebrahiminia et al., 2016), sonoluminescence generation (Ciuti et al., 2000) and H<sub>2</sub>O<sub>2</sub> production (Lee and Oh, 2011). To date, the effectiveness of DFUS operated in the range of 20–176 kHz, 25–40 kHz and 30–50 kHz have been showed for the degradation of hexachlorobenzene (Hayashi et al., 2009), p-nitrophenol (Sivakumar et al., 2002) and formic acid (Gogate et al., 2003b), respectively. The results obtained in this study demonstrate that the combination of 40 kHz and 120 kHz (LDFUS/O<sub>3</sub>)



**Fig. 8.** Effect of *p*-BQ on BTEX degradation in (a) LFDUS/O<sub>3</sub> and (b) HFDUS/O<sub>3</sub>; [BTEX]<sub>0</sub>: 50 ppm (v/v), [O<sub>3</sub>]: [*p*-BQ] = 1:10, pH 6.5, T = 20 ± 2.5 °C, O<sub>3</sub> flow rate 0.5 L min<sup>-1</sup>, US: 600 W, 40/120 kHz (LFDUS) and 80/200 kHz (HFDUS). Shaded data - corresponding processes without additives.

ensured a higher cavitation yield and generation of ROSs through O<sub>3</sub> decomposition, thereby providing higher degradation efficiency of BTEX. As listed in Table 2, the values of degradation rate constant of BTEX in LDFUS/O<sub>3</sub> were notably higher than those of HFDUS/O<sub>3</sub>, which indicates the pivotal contribution of low-frequency US in sonochemical processes associated with acoustic cavitation.

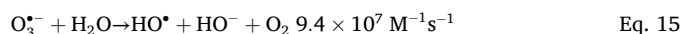
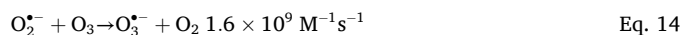
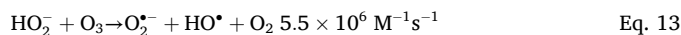
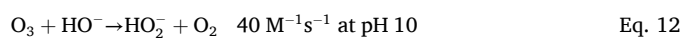
### 3.3. Effect of pH

As a powerful oxidizing agent with oxidation potential of 2.08 V, O<sub>3</sub> is capable to degrade a variety of organic compounds or to convert them into easily biodegradable compounds. Based on pH of the reaction media, the oxidative degradation of pollutants proceeds through direct electrophilic attack by molecular O<sub>3</sub> or indirect pathway induced by ROSs from O<sub>3</sub> decomposition. To evaluate the effect of pH, BTEX degradation in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> was performed at acidic and alkaline conditions. The pH study showed that BTEX degradation efficiency in both LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> systems was declined significantly at pH 3. Specifically, 18.78–31.88% of BTEXs were degraded by LFDUS/O<sub>3</sub> in 40 min (Fig. 5a). Similarly, the degradation efficiency of BTEXs in HFDUS/O<sub>3</sub> reached 28.18–32.59% in 60 min (Fig. 5b). The decreased degradation rate constants of BTEX observed at pH 3 (Table 3) suggested the predominance of direct pathway of oxidation by O<sub>3</sub>. This is due to the low decomposition rate of O<sub>3</sub> at acidic pH and slow direct interaction of molecular O<sub>3</sub> with organic substrates. Interestingly, the degradation rate constants of ethylbenzene and *o*-xylene in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> were decreased slightly compared to sole O<sub>3</sub>, which can be related to the scavenging of HO• radicals from Eqs. 1 and 9 by O<sub>3</sub> with formation of hydroperoxyl radicals (HO<sub>2</sub>) with lower oxidation

potential (Joseph et al., 2021):



The degradation of BTEX in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> occurred faster upon the increase of pH to 11. Thus, 98.76, 99.22, 98.81, 96.71% of benzene, toluene, ethylbenzene and *o*-xylene, respectively, were degraded by LFDUS/O<sub>3</sub> in 60 min. Whereas, these pollutants were correspondingly degraded to 90.20, 89.80, 88.24 and 80.28%, respectively, in 60 min by HFDUS/O<sub>3</sub>. At basic conditions, indirect oxidation of pollutants is the main route, as the dissolved O<sub>3</sub> undergoes decomposition to form highly reactive HO• radicals responsible for degradation of contaminants:



Despite the effective conversion of O<sub>3</sub> to HO• radicals at basic pH, the degradation rate constants were increased only for benzene and ethylbenzene in HFDUS/O<sub>3</sub> at pH 11 in 60 min, while the corresponding *k* values of BTEX in LFDUS/O<sub>3</sub> were lower compared to pH 6.5 (Table 3). Such effect could be related to the reduced amount of HO• radicals generated in the gas phase of cavitation bubbles, where hydrophobic BTEXs are degraded. In contrast, the alkaline reaction medium



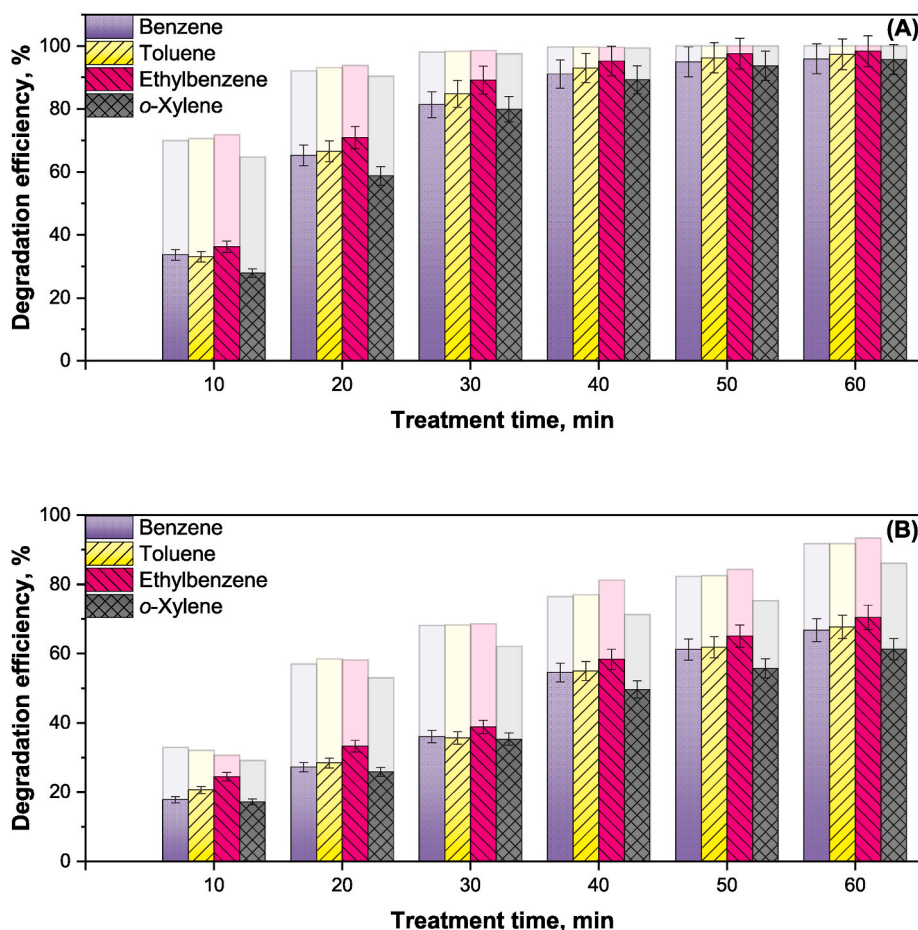
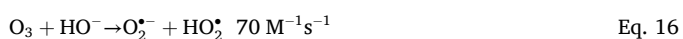


Fig. 9. The effect of  $\text{Cl}^-$  on BTEX degradation in (a) LFDUS/O<sub>3</sub> and (b) HFDUS/O<sub>3</sub>; [BTEX]<sub>0</sub>: 50 ppm (v/v), [O<sub>3</sub>]: [NaCl] = 1:10, pH 6.5, T = 20 ± 2.5 °C, O<sub>3</sub> flow rate 0.5 L min<sup>-1</sup>, US: 600 W, 40/120 kHz (LFDUS) and 80/200 kHz (HFDUS). Shaded data - corresponding processes without additives.

competitively consumed the dissolved O<sub>3</sub>, thereby increasing the fraction of HO• radicals in the bulk liquid. Since, the effectiveness of LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> was not improved significantly with the increase of pH, further experiments were conducted without pH adjustment.

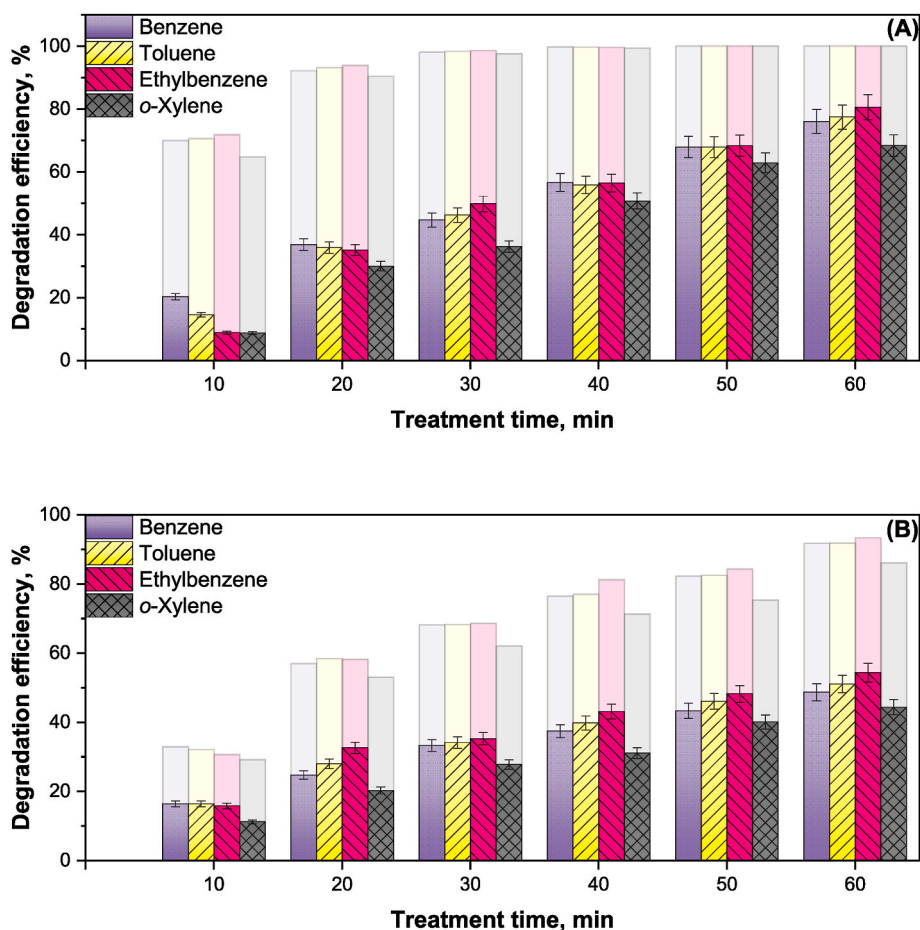
### 3.4. Identification of ROSs

Besides primary HO• radicals, the decomposition of O<sub>3</sub> can lead to the formation of secondary reactive radicals such as superoxide (O<sub>2</sub><sup>•-</sup>) radicals and singlet oxygen (<sup>1</sup>O<sub>2</sub>), which also contribute to the degradation of contaminants. The formation of O<sub>2</sub><sup>•-</sup> radicals is known to occur during the decomposition of O<sub>3</sub> in water at acidic to neutral conditions, while <sup>1</sup>O<sub>2</sub> is considered to derive from radical recombination reactions (Joseph et al., 2021; Kasprzyk-Hordern et al., 2003; Nan et al., 2024) (Eqs. (16)–(18)) In order to evaluate the contribution of ROSs in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub>, a series of quenching experiments were conducted. Owing to its high reactivity with HO• radicals (9.7 × 10<sup>8</sup> M<sup>-1</sup> s<sup>-1</sup>), methanol (MeOH) was employed to quench HO• radicals, while O<sub>2</sub><sup>•-</sup> radicals were quenched by *para*-benzoquinone (*p*-BQ) with a rate constant of 1.0 × 10<sup>9</sup> M<sup>-1</sup> s<sup>-1</sup> (Rao and Hayon, 1975; Buxton et al., 1988). Sodium azide (NaN<sub>3</sub>) with a rate constant of ~10<sup>8</sup> M<sup>-1</sup> s<sup>-1</sup> was used to verify the presence of <sup>1</sup>O<sub>2</sub> (Wang and Wang, 2020).



As presented in Fig. 6a and b, MeOH effectively inhibited BTEX degradation in both LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> processes. After 40 min of treatment only 42.3–45.7 % of BTEXs were degraded in LFDUS/O<sub>3</sub> in the presence of MeOH. On the other hand, the degradation efficiency of HFDUS/O<sub>3</sub> was decreased to 41.2–55.6 % after 60 min of treatment. Obtained results suggest HO• radicals as predominant species participating in the radical-induced oxidation of BTEX in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub>. The BTEXs degradation rate constant values determined in the presence of MeOH in LFDUS/O<sub>3</sub> (Table 4) were decreased in approx. 90.2% compared to LFDUS/O<sub>3</sub> without scavengers. In the case of HFDUS/O<sub>3</sub>, a trend of *k* decrease by the addition of MeOH was ~68%. These observations suggested that the impact of HO• radicals towards BTEX degradation was higher in LFDUS/O<sub>3</sub> compared to HFDUS/O<sub>3</sub>.

On the other hand, as shown in Fig. 7a, the degradation efficiency of BTEXs was significantly suppressed by 78.6–83.9%, respectively for 40 min of treatment with the addition of NaN<sub>3</sub> in LFDUS/O<sub>3</sub>. The presence of NaN<sub>3</sub> correspondingly inhibited the efficacy of HFDUS/O<sub>3</sub> by 57.4–64% in 60 min (Fig. 7b). According to literature, NaN<sub>3</sub> reacts with HO• and O<sub>3</sub> with rate constants of 1.2 × 10<sup>10</sup> M<sup>-1</sup> s<sup>-1</sup> and 2.5 × 10<sup>6</sup> M<sup>-1</sup> s<sup>-1</sup>, respectively (Betterton and Craig, 1999; Sun et al., 2021). Thus, the inhibitory effect of NaN<sub>3</sub> observed in this study can be attributed to the impact of both HO• radicals and <sup>1</sup>O<sub>2</sub>. Taking into account that MeOH verified the presence of HO• radicals in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub>, it can be assumed that both HO• radicals and <sup>1</sup>O<sub>2</sub> were involved in BTEX degradation, whereat <sup>1</sup>O<sub>2</sub> played a minor role. In addition, degradation rate constant of BTEX in LFDUS/O<sub>3</sub> (Table 4) was suppressed in lower extent in the presence of MeOH as compared to HFDUS/O<sub>3</sub>, while the rate constants obtained with addition of NaN<sub>3</sub> were similar. These findings may imply that Eqs. (17) and (18) were significant in larger



**Fig. 10.** The effect of  $\text{SO}_4^{2-}$  on BTEX degradation in (a) LFDUS/ $\text{O}_3$  and (b) HFDUS/ $\text{O}_3$ ; [BTEX]<sub>0</sub>: 50 ppm (v/v), [ $\text{O}_3$ ]: [ $\text{Na}_2\text{SO}_4$ ] = 1:10, pH 6.5,  $T = 20 \pm 2.5$  °C,  $\text{O}_3$  flow rate  $0.5 \text{ L min}^{-1}$ , US: 600 W, 40/120 kHz (LFDUS) and 80/200 kHz (HFDUS). Shaded data - corresponding processes without additives.

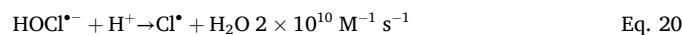
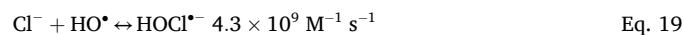
cavitation bubbles with longer collapse time generated in LFDUS/ $\text{O}_3$ .

As depicted in Fig. 8a and b, the addition of *p*-BQ inhibited the degradation efficiency of BTEX in both LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$ . The degradation efficiency of benzene, toluene, ethylbenzene, *o*-xylene with addition of *p*-BQ were 61.50, 65.88, 70.49, and 64.42%, respectively, after 60 min of treatment by LFDUS/ $\text{O}_3$ . As shown in Fig. 8b, HFDUS/ $\text{O}_3$ /*p*-BQ degraded 69.34, 70.11, 73.05, 63.36%, of benzene, toluene, ethylbenzene and *o*-xylene in 60 min, respectively. Since *p*-BQ can also partially quench  $\text{HO}^\bullet$  radicals ( $6.6 \times 10^9 \text{ M}^{-1}\text{s}^{-1}$ ) (Fónagy et al., 2021), these results are discussed to confirm the involvement of  $\text{O}_2^\bullet$  radicals in BTEX degradation. To conclude, it can be proposed that  $\text{HO}^\bullet$  radicals were the main reactive species responsible for the degradation of BTEX in LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$ , while  $\text{O}_2^\bullet$  radicals and  $^1\text{O}_2$  played a minor role.

### 3.5. Effect of co-existing inorganic anions

Practical implementation of novel chemical processes in water treatment strategies presumes operations with natural water containing a variety of constituents, such as natural organic matter (NOM), co-existing inorganic anions, mineral cations etc. In order to determine the effect of inorganic anions, the degradation of BTEX by LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  was performed in the presence of chloride ( $\text{Cl}^-$ ), carbonate ( $\text{CO}_3^{2-}$ ) and sulfate anions ( $\text{SO}_4^{2-}$ ). Fig. 9a and b illustrate the degradation efficiency of BTEX during LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  in presence of  $\text{Cl}^-$  anions. It can be seen that the addition of  $\text{Cl}^-$  anions had an adverse effect on BTEX degradation in both processes. The degradation efficiency was reduced by 4.35–10.1% after 40 min in LFDUS/ $\text{O}_3$ . However, still the performance of the processes was on acceptable level.

Scavenging effect of  $\text{Cl}^-$  anions on BTEX degradation was more pronounced in HFDUS/ $\text{O}_3$  (Fig. 9b). Degradation rates of BTEXs were reduced by 22.89–24.95%, respectively, after 60 min of treatment. The inhibitory effect of  $\text{Cl}^-$  anions is commonly attributed to the scavenging of  $\text{HO}^\bullet$  radicals to form chlorine oxidizers (i.e.,  $\text{Cl}^\bullet$ ,  $\text{Cl}_2^\bullet$  and  $\text{HClO}^\bullet$ ) with lower oxidation potential (Eqs. (19)–(21)) (von Gunten, 2003; Asghar et al., 2022). However, the sequence of radical reactions initiated with Eq. (19) is pH-dependent and the steady-state concentration of  $\text{HOCl}^\bullet$  at neutral conditions is negligible as the reverse reaction with  $6.1 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$  prevails (Yu and Barker, 2003). Thus, the inhibitory effect of  $\text{Cl}^-$  anions can be referred to the direct competitive reaction with  $\text{O}_3$  to yield  $\text{OCl}^-$  (Eq. (22)), which is present in equilibrium with  $\text{HOCl}$  at neutral conditions and stable to  $\text{O}_3$  oxidation (Asghar et al., 2022).



As shown in Fig. 10a and b,  $\text{SO}_4^{2-}$  anions caused the reduction of BTEX degradation efficiency in both LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  processes.  $\text{SO}_4^{2-}$  anions are commonly considered as a scavenger of  $\text{HO}^\bullet$  radicals due to inevitable generation of  $\text{SO}_4^\bullet$  radicals (Eq. (24)) (Dehvari et al., 2020; Golshan et al., 2018). The degradation efficiency of BTEX in LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  was decreased as  $\text{SO}_4^{2-}$  anions partially

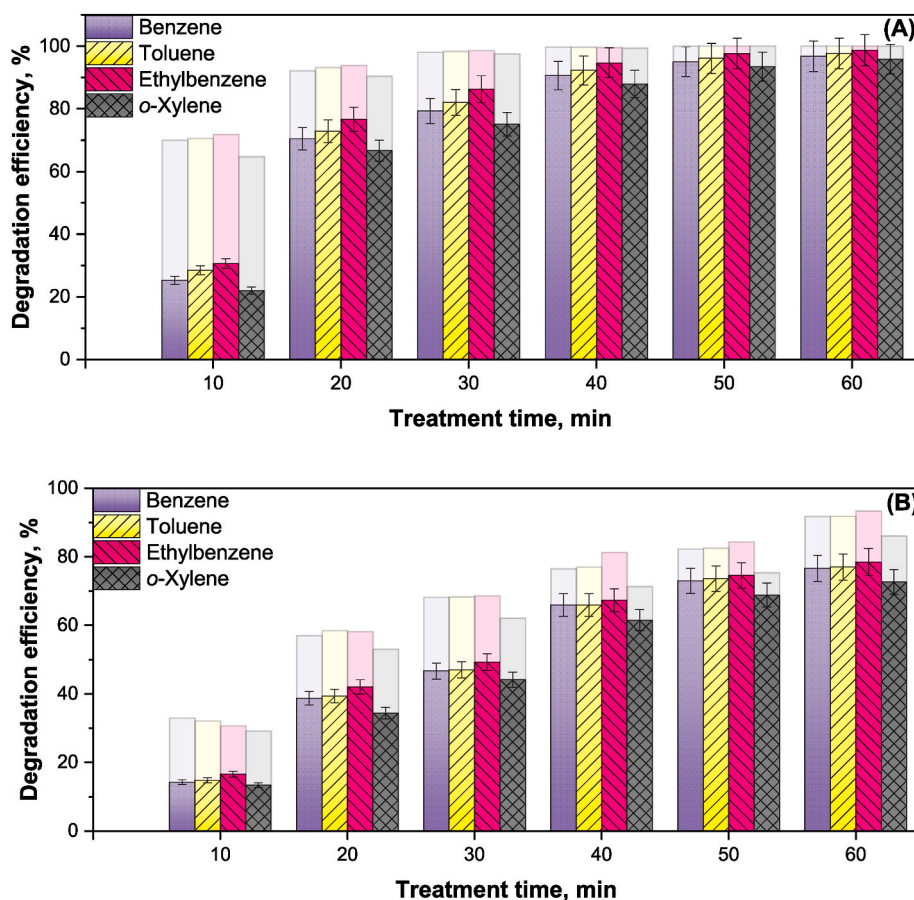


Fig. 11. The effect of  $\text{CO}_3^{2-}$  on BTEX degradation in (a) LFDUS/ $\text{O}_3$  and (b) HFDUS/ $\text{O}_3$ ;  $[\text{BTEX}]_0$ : 50 ppm (v/v),  $[\text{O}_3]$ :  $[\text{Na}_2\text{CO}_3] = 1:10$ , pH 10.5,  $T = 20 \pm 2.5$  °C,  $\text{O}_3$  flow rate  $0.5 \text{ L min}^{-1}$ , US: 600 W, 40/120 kHz (LFDUS) and 80/200 kHz (HFDUS). Shaded data - corresponding processes without additives.

Table 5

Pseudo-first-order kinetic model parameters of BTEX degradation in LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  systems in the presence of inorganic anions.

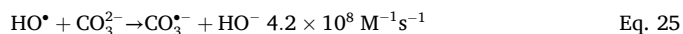
Anion	Process	Benzene	Toluene	Ethylbenzene	o-Xylene
		$k, \text{min}^{-1}$	$k, \text{min}^{-1}$	$k, \text{min}^{-1}$	$k, \text{min}^{-1}$
$\text{Cl}^-$	LFDUS/ $\text{O}_3$	0.0575	0.0649	0.0738	0.0560
	HFDUS/ $\text{O}_3$	0.0188	0.0190	0.0203	0.0160
$\text{SO}_4^{2-}$	LFDUS/ $\text{O}_3$	0.0231	0.0242	0.0265	0.0200
	HFDUS/ $\text{O}_3$	0.0106	0.0114	0.0125	0.0096
$\text{CO}_3^{2-}$	LFDUS/ $\text{O}_3$	0.0602	0.0656	0.0760	0.0555
	HFDUS/ $\text{O}_3$	0.0259	0.0262	0.0270	0.0231

consumed  $\text{HO}^\bullet$  radicals and formed  $\text{SO}_4^\bullet$  radicals possess relatively lower oxidation potential (2.5–3.1 V) and selectivity towards electron-rich substances (Tian et al., 2022). Particularly, the presence  $\text{SO}_4^{2-}$  anions in LFDUS/ $\text{O}_3$  suppressed the degradation efficiency of BTEXs by 43.1–48.7%, in 40 min of the treatment. In the case of HFDUS/ $\text{O}_3$ , the degradation efficiency of these compounds was correspondingly reduced by 40.7–43.04% after 60 min.



As shown in Fig. 11a and b, the addition of  $\text{CO}_3^{2-}$  anions demonstrated negligible inhibitory effect on BTEX degradation in both LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  processes. With the addition of  $\text{CO}_3^{2-}$  anions, the degradation efficiency was declined by 4.9–11.4% in LFDUS/ $\text{O}_3$ , respectively, in 40 min. The corresponding inhibitory effect of  $\text{CO}_3^{2-}$  anions in HFDUS/ $\text{O}_3$  after 60 min was a bit higher – a 13.4–15.1% decrease was observed. This effect is conditioned by the dual impact of

$\text{CO}_3^{2-}$  anions, which is comprised of two contrary factors. Firstly,  $\text{CO}_3^{2-}$  anions are strong scavengers of  $\text{HO}^\bullet$  radicals forming  $\text{CO}_3^\bullet$  radicals (Eq. (25)) with lower oxidation potential and selectivity towards certain contaminants (Gagol et al., 2020; Kasprzyk-Hordern et al., 2003; Rayaroth et al., 2023). Secondly, addition of  $\text{CO}_3^{2-}$  anions lead to the increase of pH. Strong alkaline condition (pH~11.0) facilitates  $\text{O}_3$  decomposition resulting in generation of  $\text{HO}^\bullet$  radicals (Gagol et al., 2018c). As was discussed in section 3.3, such conversion takes place in the bulk liquid phase, while the degradation of BTEX proceeds in the gaseous phase of cavitation bubbles. Hence, the base-catalyzed decomposition of  $\text{O}_3$  led to the accumulation of  $\text{HO}^\bullet$  radicals in bulk liquid thereby hindering the efficient utilization of  $\text{O}_3$  for BTEX degradation under cavitation.



The degradation rate constants of BTEX in LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  determined in the presence of co-existing anions are presented in Table 5. According to obtained results, the negative impact of inorganic anions showed the following order:  $\text{SO}_4^{2-} > \text{Cl}^- > \text{CO}_3^{2-}$  in both LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  processes. The inhibitory effect of inorganic anions on degradation of organic contaminants may be considerable when LFDUS/ $\text{O}_3$  and HFDUS/ $\text{O}_3$  processes are applied in the treatment of real wastewater effluents.

### 3.6. Identification of intermediates and possible degradation mechanism

Inefficient AOPs often lead to the incomplete mineralization of organic pollutants. Therefore, such processes are related with the formation of undesirable degradation intermediates. These intermediates may pose the toxicity risk greater than parent contaminants causing

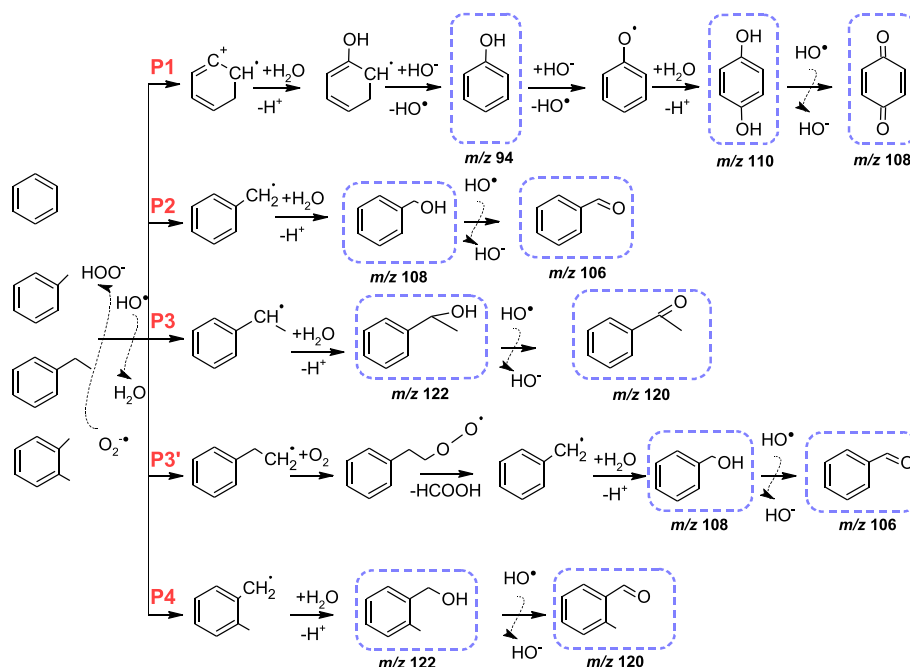


Fig. 12. The proposed degradation mechanism of BTEX in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub>.

secondary pollution. In order to reveal the intermediates of BTEX degradation in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> processes, treated samples of BTEX at certain time interval were analyzed by GC-MS. The intermediates were identified using SCAN mode based on the peak analysis performed by similarity search. The possible degradation mechanism of BTEX was proposed based on the identified intermediates. To elucidate the individual degradation product of each BTEX component, model solutions of benzene, toluene, ethylbenzene and *o*-xylene were separately treated by LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub>. These model solutions of benzene, toluene, ethylbenzene, *o*-xylene were prepared with the concentration of 800 ppm, 450 ppm, 300 ppm and 250 ppm, respectively, for better expression of intermediate peaks in GC-MS chromatogram to ease the detection.

Generally, oxidative degradation of organic contaminants during ozonation under US is conducted by ROSS, such as HO<sup>•</sup>, O<sub>2</sub><sup>•-</sup>, <sup>1</sup>O<sub>2</sub>. In this case, aromatic hydrocarbons react with ROSS via hydrogen abstraction (H-abstraction) from benzoic ring or methyl/ethyl groups of aromatic compounds. Oxidation intermediates may further undergo hydroxylation, dealkylation and consecutive mineralization. As shown in Table S1, several intermediates were detected during oxidative degradation of BTEX. Specifically, phenol, hydroquinone and *p*-benzoquinone were formed during benzene degradation. Toluene was accordingly converted to benzyl alcohol and benzaldehyde, while 1-phenylethanol, acetophenone, benzene alcohol, benzaldehyde, *o*-methylbenzyl alcohol and *o*-tolualdehyde were present in treated samples of ethylbenzene and *o*-xylene.

Based on the range of detected intermediates, it can be suggested that the oxidative degradation of benzene was processed via the radical route in both LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> processes. When benzene reacts with HO<sup>•</sup>/O<sub>2</sub><sup>•-</sup> radicals, the aromatic ring undergoes H-abstraction to form a cation radical. The cation radicals can react with H<sub>2</sub>O resulting to OH-group addition with further propagation of the radical adduct yielding phenol (m/z 94). Detection of hydroquinone (m/z 110) and *p*-benzoquinone (m/z 108) suggests the hydroxylation of phenol in *para*-position and subsequent re-arrangement of conjugated π-π system. H-abstraction of toluene, ethylbenzene and *o*-xylene proceeded from alkyl groups attached to the aromatic ring as C-H bond energy in alkyl groups is lower than in the aromatic ring. Initiated by H-abstraction, the radical route of oxidation involves several steps, possibly including

hydroxylation and dealkylation prior to ring-opening reactions. As illustrated in Fig. 12, the primary step of toluene degradation started with H-abstraction from methyl group by HO<sup>•</sup> or O<sub>2</sub><sup>•-</sup> radicals. The obtained radical adduct underwent hydroxylation in presence of water and readily oxidized by ROSS to form benzyl alcohol (m/z 108) and benzaldehyde (m/z 106). These intermediates were also detected in treated samples of ethylbenzene implying the dealkylation of ethyl group, which is possible with elimination of formic acid in presence of oxygen. Then, the obtained aromatic radical repeated the degradation pathway described for toluene. Additionally, non-selective attack of ROSS caused β-H-abstraction from ethylbenzene resulting in formation of 1-phenylethanol (m/z 122) and acetophenone (m/z 120). In case of *o*-xylene, H-abstraction can be conducted from one of the methyl groups. Identification of *o*-methylbenzyl alcohol (m/z 122) and *o*-tolualdehyde (m/z 106) in the treated solution reflects the consecutive hydroxylation and oxidation of one methyl group of *o*-xylene. These intermediates were not detected in final samples of studied processes (detection limits for such VOCs for used DLLME-GC-MS based method are below 5 ppb (Makoš et al., 2018)) for primary concentration of BTEXs 50 ppms confirming their further complete degradation.

#### 4. Conclusions

The oxidative degradation of BTEX in US/O<sub>3</sub> was significantly enhanced by the introduction of the second source of US. The combination of O<sub>3</sub> and dual-frequency US with operating frequencies of 40 and 120 kHz (LFDUS/O<sub>3</sub>) exhibited higher degradation capacity than 80/200 kHz US (HFDUS/O<sub>3</sub>). Both combined processes could effectively degrade BTEX at pH 6.5, O<sub>3</sub> containing gas flow rate 0.5 L min<sup>-1</sup>, US power input 600 W, frequencies: 40/120 kHz for LFDUS and 80/200 kHz for HFDUS, respectively. The synergistic indexes of 1.13 and 0.94 were obtained for BTEX degradation in LFDUS and HFDUS, respectively. The combination of LFDUS and HFDUS with O<sub>3</sub> resulted in significant increase of BTEX degradation efficiency with the synergistic indexes of 7.86 and 2.9, respectively. Synergistic effect for LFDUS is unusual and largely exceeds typically reported values of synergistic coefficient available in the literature (typically not higher than 4.0). The observed results confirmed the crucial role of dual-frequency US for specific and not obvious frequency values in acoustic cavitation, which contributes

to sonochemical generation of HO• radicals and O<sub>3</sub> decomposition. The presence of SO<sub>4</sub><sup>2-</sup> and Cl<sup>-</sup> anions noticeably inhibited the degradation efficiency of BTEX in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub>, whereas CO<sub>3</sub><sup>2-</sup> showed negligible inhibitory effect. Also in this aspect LFDUS revealed to be more effective and stable under simulated real conditions. Quenching experiments indicated that HO• radicals were the dominant reactive species responsible for BTEX degradation, singlet oxygen also importantly contributed in degradation, while O<sub>2</sub><sup>•-</sup> radicals had a minor contribution. Identification of degradation intermediates using GC-MS confirmed the radical route of BTEX oxidation in LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub>. The study contributes to the understanding of hybrid cavitation-based AOPs for the removal of water contaminants emphasizing the importance of process parameters and water constituents on the removal efficiency. As a part of ongoing trend towards environmental sustainability, future research can focus on scaling up LFDUS/O<sub>3</sub> and HFDUS/O<sub>3</sub> processes for the treatment of real wastewaters. In case of the developed process, increase of the treatment scale seems possible, as both ozonation and ultrasonic systems are already available for industrial scale processes.

### CRedit authorship contribution statement

**Kirill Fedorov:** Writing – original draft, Visualization, Methodology, Investigation, Conceptualization. **Lingshuai Kong:** Writing – review & editing, Validation. **Chongqing Wang:** Writing – review & editing, Validation. **Grzegorz Boczkaj:** Writing – review & editing, Writing – original draft, Validation, Supervision, Resources, Project administration, Methodology, Funding acquisition, Conceptualization.

### Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

### Data availability

No data was used for the research described in the article.

### Acknowledgements

The authors gratefully acknowledge financial support from the National Science Centre, Warsaw, Poland for project OPUS nr UMO-2017/25/B/ST8/01364.

### Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.jenvman.2024.121343>.

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